Recommended Practice 101

Control of the Hazards Associated with Reactive Chemicals

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RP-101 Control of the Hazards Associated with Reactive Chemicals

Abstract

Highly hazardous reactive chemicals pose a significant risk to chemical plant workers and the communities around them. These chemicals have the potential to create explosions, fires and releases of toxic materials. Unfortunately, the OSHA PSM regulation only covers a small fraction of these chemicals and in addition, the requirements of the regulation are not well understood by many companies. Recommended Practice – 101 is intended to fill this gap. It provides guidance on how to identify highly hazardous reactive chemicals and the recognized and generally accepted good engineering practices needed to control their hazards.

Preface

This recommended practice is dedicated to the people that were killed or seriously injured because Recognized and Generally Accepted Good Engineering Practices (RAGAGEP) were not followed in chemical process facilities, refineries, pulp and paper mills and related process industries. It is anticipated that this recommended practice will enlighten those personnel that are responsible for the design, operation, maintenance and management of process units and ultimately save lives.

Numerous RAGAGEP are referenced in this practice. Most of these practices are updated periodically and the most recent revision is the practice that should be used.

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Any suggestions for improving this recommended practice should be sent to the author.

Introduction

Reactive chemicals are materials capable of giving rise to a sudden uncontrolled chemical reaction (a runaway reaction) with a significant release of energy and/or toxic materials capable of causing injury to people, property, or the environment.

This recommended practice establishes the minimum requirements for employers that manufacture, process, use or handle Highly Hazardous Reactive Chemicals (HHRC). The objective of this recommended practice is to protect employees, the public and the environment from the fire, explosion and toxic hazards associated with the manufacture, processing, use or storage of reactive chemicals.

There are three ways in which reactive chemicals are used: Intentional Chemistry, Physical Processing and Storage. A Highly Hazardous Reactive Chemical (HHRC) Storage process is one where HHRC are in a container, and are never removed from the container except for sampling. Examples of possible storage processes are: Warehouses and storage facilities at a chemical production facility; Warehouses and storage facilities of a wholesaler; Warehouse and storage facilities at a freight terminal.

A HHRC Physical Processing process removes the HHRC from a vessel or container, process it in some way, and then either returns the material to the same vessel or container or to another vessel or container. Physical processing also includes operations where the material in a vessel or container is processed in the vessel container and no chemical reaction is intended. Examples of process that may include physical processing include: Repackaging; Mixing or blending of the HHRC; Addition of chemicals, additives, or other materials to the HHRC, which may or may not include mixing or blending; Screening, compaction, granulation, grinding or milling; Heating, cooling or drying; and Distillation, liquid-liquid extraction, adsorption, absorption, or filtering.

An Intentional Chemistry process is a process where chemicals are intentionally reacted to form a different chemical or chemicals. Intentional chemistry processes are found in the vast majority of chemical manufacturing and refining facilities.

Some of the recommended practices that follow are not applicable to storage processes. For storage processes, the sections pertaining to process safety information, the design and design basis of safety systems, and process hazards analysis may be the only sections that are applicable. Employers at storage facilities should however, review all of the sections to determine if there are other sections, or portions of other sections that are applicable to their situation.

Use of Good Engineering Practices: Employers shall use Recognized and Generally Accepted Good Engineering Practices (RAGAGEP) in the design, operation, maintenance and management of all chemical processes covered by this recommended practice.

RAGAGEP is defined in consensus codes, recommended practices, and guidelines. Some of those most applicable to chemical processes are the Guideline and Concept books prepared by the Center for Chemical Process Safety (CCPS) of the American Institute of Chemical Engineers (AIChE). These books in turn reference many of the applicable standards, recommended practices, and guidelines by other organizations such as ANSI (American National Standards Institute), API (American Petroleum Institute), ASME (American Society of Mechanical Engineers), ISA (the Instrumentation, Systems, and Automation Society), and NFPA (National Fire Protection Association). OSHA also has certain regulations that mandate good engineering practices. Documents which represent good engineering practices are referenced at applicable places within this recommended practice. Identification of these practices is not intended to indicate that they are the only RAGAGEP that apply.

The requirements listed in sections (c) through (o) of this recommended practice identify the elements of good engineering practices that must be met. The requirements listed for each element are not, and are not intended to be, comprehensive. They only provide a framework, and not the details required by the employer to establish that RAGAGEP has been used. The employer shall use appropriate consensus standards, recommended practices, and guidelines to ensure that the elements are addressed in a comprehensive manner.

When two or more consensus standards, recommended practices, or guidelines cover the same issue, the one, or the portions of the one that provides the highest level of safety, or hazard reduction, shall govern. Regulatory requirements must always be met regardless of whether they conflict with industry standards.

Application.

- a) This recommended practice applies if any of the following apply:
 - 1) A process which involves a chemical having the characteristics listed in Appendix A.
 - 2) A process which involves a flammable liquid, solid or gas on-site, in one location, in a quantity of 5,000 pounds, or more except for:
 - 3) Hydrocarbon fuels used solely for workplace consumption as a fuel (e.g., propane used for comfort heating, gasoline for vehicle refueling), if such fuels are not a part of a process containing another highly hazardous chemical covered by this recommended practice;
 - Any process that the employer determined to be not covered by this recommended practice that experiences a fire, explosion, or release of toxic material due to a reactive incident that results in, or had the potential to result in death, injury, or significant property damage on-site, or known off-site deaths, injuries, evacuations, sheltering in place, property damage, or environmental damage, shall be considered to be covered by this recommended practice after that incident. Similar processes operated by

the employer at other sites also become covered by this recommended practice.

- 5) This recommended practice does not apply to:
 - (i) Retail facilities;
 - (ii) Oil or gas well drilling or servicing operations; or,
 - (iii) Normally unoccupied remote facilities.

Definitions

Definitions applicable to this and referenced recommended practices include:

- 1) **Basic Process Control System (BPCS)** means a system that responds to input signals from the equipment under control and/or from an operator and generates output signals, causing the equipment under control to operate in the desired manner. Also referred to as process control system.
- Boiling Point means the boiling point of a liquid at a pressure of 14.7 pounds per square inch absolute (psia) (760 mm.). For the purposes of this recommended practice, where an accurate boiling point is unavailable for the material in question, or for mixtures which do not have a constant boiling point, the 10 percent point of a distillation performed in accordance with the Standard Method of Test for Distillation of Petroleum Products, ASTM D-86-62, may be used as the boiling point of the liquid.
- 3) **Calorimetry** means the use of specialized equipment and techniques to determine heats of reaction, onset temperatures, rates of pressure rise, rates of temperature rise, reaction rates and other thermal properties of chemicals or mixtures of chemicals.
- 4) **Catastrophic Release** means a major uncontrolled emission, fire, or explosion, involving one or more highly hazardous chemicals that present serious danger to employees in the workplace.
- 5) **Chemical Reactivity Hazard** means a situation with the potential for an uncontrolled chemical reaction that can result directly or indirectly in serious harm to people, property or the environment. The uncontrolled chemical reaction may result in a fire, explosion or release of toxic gas.
- 6) **Compatibility** means the ability of materials to exist in contact with each other without a reaction occurring.
- 7) **Contractor** means an entity that performs work for the employer for a fee.
- 8) **Decomposition** means the breakdown of a chemical into its constituents. Frequently results in the release of a gas, which may be toxic.
- 9) **Employer** means the entity that owns and or operates the facility.

- 10) **Endothermic** means a chemical reaction that absorbs heat from its surroundings.
- 11) **Exothermic** means a chemical reaction that is accompanied by the release heat. By convention, exothermic reactions have a negative heat of reaction. Runaway reactions are exothermic
- 12) **ERPG-2** means Emergency Response Planning Guide Level 2; the maximum airborne concentration below which it is believed that nearly all individuals could be exposed for up to 1 hour without experiencing or developing irreversible or other serious health effects or symptoms that could impair their ability to take protective action.
- **Facility** means the buildings, infrastructure and equipment which contain a process, or processes.
- 14) **Flammable** means a material that meets the NFPA definition² for a class 3, or 4 Flammability Hazard or a class 2 Flammability Hazard combustible liquid that is processed, used, or stored or has the potential to be processed, used, or stored, at 20 degrees F below its flashpoint, or higher.
- 15) **Functional Groups** are portions of chemical molecules. Chemicals that contain the same functional group often react in similar ways.
- 16) **Hazard** means a chemical or physical condition that has the potential to cause damage to people, property or the environment.
- 17) **Heat of Reaction** means the total quantity of thermal energy that is released (or absorbed) during a chemical reaction. Mathematically, it is equal to the heat of formation of the reaction products at reaction conditions minus the heats of formation of the reactants at the initial condition. Exothermic reactions have a negative heat of reaction.
- 18) **Highly Hazardous Chemical** means a substance possessing toxic, reactive, flammable, or explosive properties and specified by paragraph (a)(1) of this recommended practice.
- 19) **Hot Work** means work involving electric or gas welding, cutting, brazing, grinding, sand blasting or similar flame or spark-producing operations.
- 20) **Hypergolic** means mixtures of liquids that immediately react when the constituents are added together or mixed. This may result in spontaneous ignition or explosion.
- 21) Independent Layer of Protection (IPL) means a device, system or action that is capable of preventing a scenario from proceeding to its undesired consequence independent of the initiating event or the action of any other layer of protection or safeguard associated with the scenario. In order for a control to qualify as an independent layers of protection, it must be capable of being tested and must also be able to reduce the probability of failure of the layer of protection by a factor of 100. Any layer of protection that

- requires operator actions is not an independent layer of protection. Typical IPLs are high reliability instrumented systems and pressure relief devices.
- 22) **Inhibitor** means a chemical substance that is capable of stopping a reaction. Inhibitors are most applicable to storage of polymerizable or decomposing chemicals.
- 23) **Instability** means the degree of intrinsic susceptibility of a material to self-react such as polymerization, decomposition, or rearrangement.
- 24) **Layer of Protection** means a device, system or action that is used to reduce the probability that a deviation from intended operation will result in a hazardous condition such as a release of toxic material, fire or explosion.
- 25) **Near Miss** means an unplanned event that had the potential to cause harm if conditions had been different or had been allowed to progress. Examples include: opening of a pressure relief device, activation of a safety instrumented system (interlock), a release of flammable material that does not result in a fire or explosion and a release of toxic material that does not enter an area where personnel are located.
- Normally Unoccupied Remote Facility means a facility which is operated, maintained or serviced by employees who visit the facility only periodically to check its operation and to perform necessary operating or maintenance tasks. No employees are permanently stationed at the facility. Facilities meeting this definition are not contiguous with, and must be geographically remote from all other buildings, processes or persons.
- Occupied Building means a stationary or portable building that people enter more than one day per year. Typical examples include control rooms, maintenance shops, locker rooms, motor control centers, administrative buildings, laboratory buildings, trailers (including temporary trailers), work trailers, tool trailers and portable toilets.
- Onset Temperature means the temperature at which a chemical or mixture of chemicals starts to react at a measurable rate. The temperature at which the reaction causes a rate of temperature rise of 0.01 to 0.02°C/minute is often considered the onset temperature that would be expected in process equipment. The determination of the onset temperature is dependent on the sensitivity of the test equipment, the heat rate and the wait time. Estimation of the onset temperature in process equipment requires highly sensitive test equipment, a low heat rate, and long wait times.
- 29) **Peroxide** means a chemical that contains the peroxy (-O-O-) group. Most peroxides are very reactive.
- 30) **Polymerization** means a chemical reaction generally associated with the production of plastic. The individual chemicals (monomers) react with themselves to form compounds containing many multiples of the original chemicals linked together like a chain.

- 31) **Probability of Failure on Demand (PFD)** is a value that indicates the probability of a system failing to respond to a demand. Values range from 0 to 1.
- Process means any activity involving a highly hazardous chemical including any use, storage, manufacturing, handling, or the on-site movement of such chemicals, or combination of these activities. For purposes of this definition, any group of equipment which is interconnected and separate equipment which is located such that a highly hazardous chemical could be involved in a potential release shall be considered a single process. All utilities are also part of the process.
- 33) **Process Chemistry** means the manner in which chemicals are reacted to form products and byproducts, including undesirable reactions.
- 34) **Pyrophoric** means a chemical with an autoignition temperature in air at or below 130°F (54.4°C).
- 35) **Quenching** means abruptly stopping a reaction by severe cooling, usually by the addition of a cold solvent or other compatible material. Used as a safeguard against runaway reactions.
- 36) **Reaction** means any transformation of material or mixtures of materials that result in either the release or absorption of heat. Runaway reactions release heat.
- 37) **Reliability** means the probability that a system can perform a defined function under stated conditions over a given period of time.
- 38) **Remote Facility** means a process for which the worst case scenario, as defined in 40 CFR Part 68, would not result in off-site deaths, injuries, evacuations, sheltering in place, property damage, or environmental damage;
- 39) **Replacement In Kind** means a replacement which satisfies the design specification (equipment) or training requirements (personnel).
- 40) **Runaway Reaction** means a reaction that is out of control because the rate of heat generation by exothermic chemical reaction exceeds the rate of heat removal (cooling) available.
- 41) **Safety Instrumented System (SIS)** means a system composed of sensors (i.e. temperature transmitter), logic solvers (i.e. Programmable Logic Controller (PLC)), and final control elements (i.e. actuated valve) for the purpose of taking the process to a safe state when a predetermined condition is violated. An interlock is a SIS.
- 42) **Safety Integrity Level (SIL)** is a measure of the reliability of a safety instrumented system to function as designed. One of three possible discrete integrity levels (SIL 1, SIL 2, and SIL 3) of safety instrumented systems defined in terms of Probability of Failure on Demand (PFD). SIL 3 has the highest reliability, SIL1 the lowest.

- 43) **Self Accelerating Decomposition Temperature (SADT)** means the onset temperature for a decomposition reaction.
- 44) **Self Reactive** means a chemical capable of polymerization, decomposition or rearrangement. Initiation of the reaction can be spontaneous, by energy input such as thermal or mechanical energy, or by catalytic action.
- 45) **Shock Sensitive** means a relatively unstable compound that can energetically decompose with the addition of mechanical energy, such as impact.
- 46) **Spontaneously Combustible** means chemicals or mixtures of chemicals capable of igniting and burning in air without the presence of an ignition source. Includes pyrophoric materials. A common concern is when spontaneously combustible materials are heated due to their normally slow decomposition rate, faster than the heat is removed due to the insulating affect of containers or the material itself.
- 47) **Temperature of No Return** means the temperature at which the rate of heat generation due to a chemical reaction is equal to the rate of heat removal (cooling). Any temperature increase over this value results in a runaway reaction.
- 48) **Thermally Unstable** means a material that will undergo an exothermic, self substantiating or accelerating self-reaction when heated to a specified temperature.
- 49) **Toll Manufacturing** means manufacturing, blending, mixing, processing, or packaging chemicals for a fee. The contractor may be using equipment owned by either the contractor or the employer on property owned by either the employer or the contractor.
- 50) **Trade Secret** means any confidential formula, pattern, process, device, information or compilation of information that is used in an employer's business, and that gives the employer an opportunity to obtain an advantage over competitors who do not know or use it.
- 51) Water Reactive means a material that will react upon contact with water during ambient or process temperatures. Includes materials that react slowly, but can generate heat or gases that can result in elevated pressure if the material is contained.

Employee participation

- b) Employee Participation
 - 1) Employers shall develop a written plan of action regarding the implementation of the employee participation required by this recommended practice.
 - 2) Employers shall consult with employees and their representatives on the conduct and development of process hazards analyses and on the

- development of the other elements of process safety management in this recommended practice.
- 3) Employers shall provide to employees and their representatives access to process hazard analyses and to all other information required to be developed under this recommended practice.

Process Safety Information

- Process safety information. The employer shall complete a compilation of written process safety information³⁷ before conducting any process hazard analysis required by the recommended practice. The compilation of written process safety information is to enable the employer and the employees involved in operating the process to identify and understand the hazards posed by those processes involving highly hazardous chemicals. This process safety information shall include information pertaining to the hazards of the highly hazardous chemicals used or produced by the process, information pertaining to the technology of the process, and information pertaining to the equipment in the process.
 - 1) Information pertaining to the hazards of the highly hazardous chemicals in the process. This information shall consist of at least the following:
 - (i) Toxicity information;
 - (ii) Permissible exposure limits;
 - (iii) Physical data;
 - (iv) Corrosivity data;
 - (v) Reactivity, thermal and chemical instability data^{3, 4, 6} including:
 - (A) Self-Reacting:
 - (B) Polymerization, both catalyzed and uncatalyzed;
 - (C) Decomposition, both thermal and shock induced;
 - (D) Rearrangement of chemical structure such as isomerization and disproportionation;
 - (E) Reactivity with other chemicals:
 - (F) Reactivity with oxygen;
 - (G) Reactivity with water;
 - (H) Reactivity with metals, including the materials of construction of the equipment in the process;
 - (I) Potential to form peroxides;
 - (J) Reactivity with acids and bases;
 - (K) Reactivity with other chemicals present in the process;

- (L) Heats of reaction for the desired reactions as well as all other foreseeable reactions to the extent necessary to design heat transfer equipment, safety systems and pressure relief systems;
- (vi) Hazardous effects of inadvertent mixing of different materials that could foreseeably occur. This shall be documented by means of a reactivity matrix^{3, 5, 7, 30}. Refer to Table 15 for an example of a typical reactivity matrix. The maximum number of chemicals that could foreseeably be inadvertently mixed at any one time must be considered for each chemical.
 - (A) All reasonably foreseeable potential combinations must be considered, such as:
 - (1) All stored or handled chemicals, including raw materials, intermediates, products, by-products, solvents, inhibitors and catalysts;
 - (2) Potential residual chemicals in equipment, piping and hoses that are also used for other processes, or in other batches;
 - (3) All utilities (Steam, heat transfer fluids, refrigerants, nitrogen, etc.);
 - (4) Environmental substances (Air, humidity, water, dirt and dust, etc.);
 - (5) Process contaminants (Dirt, rust, lubricants, cleaning or passivation fluids, hydrotest fluids, etc.);
 - (6) Materials of construction, including gaskets and instrumentation (also consider potential substitutions and corrosion byproducts);
 - (7) Process materials (Adsorbents, absorbents, filter media, insulation);
 - (8) Excessive process conditions as defined in section (d)(2)(iv)(High or low temperature, high or low pressure);
 - (9) Potential sources of energy (Static electricity, adiabatic compression, heat, light);
 - (B) For example, a monomer storage tank could foreseeably contain oxygen (air), water, rust, monomer peroxide, monomer popcorn, polymer, and oligomers as well as the monomer. The hazards of such a mixture must be determined and documented.

- (C) When information about the hazards of chemicals used in the process, under similar conditions to those used in the process, can not be found in company databases, open literature or commercial databases, then it shall be developed^{6, 3, 7}
- 2) Information pertaining to the technology of the process. Information concerning the technology of the process^{1, 62} shall include at least the following:
 - (i) A block flow diagram or simplified process flow diagram;
 - (ii) Process chemistry;
 - (iii) Maximum intended inventory;
 - (iv) Safe upper and lower limits for such items as temperatures, pressures, flows or compositions; and,
 - (v) An evaluation of the consequences of deviations, including those affecting the safety and health of employees.
 - (vi) Where the original technical information no longer exists, such information must be developed in sufficient detail to support the requirements of this recommended practice.
- 3) Information pertaining to the equipment in the process.
 - (i) Information pertaining to the equipment in the process shall include:
 - (A) Materials of construction;
 - (B) Piping and instrument diagrams (P&ID's);
 - (C) Electrical classification^{8, 9, 10, 11}
 - (D) Relief system design and design basis ^{12, 26};
 - (1) All foreseeable overpressure scenarios and combinations of scenarios must be considered, including runaway reaction and fire induced runaway reaction;
 - (2) Relief systems on vessels containing reactive materials such as those showing the characteristics listed in Appendix A, and those systems that may have two-phase flow through the relief system, shall be evaluated using Design Institute for Emergency Relief Systems (DIERS) methodology ¹³;
 - (E) Ventilation system design ^{14, 15, 21};
 - (F) Design codes and standards employed;
 - (G) Material and energy balances and,

- (H) Safety systems^{3, 6, 28, 35} such as:
 - (1) Instrumentation and controls 16, 17 such as:
 - (a) Monitoring devices;
 - (b) Transmitters;
 - (c) Control systems;
 - (d) Control valves;
 - (e) Sensors;
 - (f) Alarms;
 - (g) Interlocks;
 - (h) Emergency shutdown systems;
 - (2) Inerting systems;
 - (3) Inhibitor concentrations and conditions necessary to maintain effective inhibitor levels;
 - (4) Runaway reaction mitigation systems^{3, 6, 28, 35}, such as:
 - (a) Quench systems;
 - (b) Depressurization systems;
 - (c) Catalyst poison addition systems;
 - (d) Dump systems;
 - (e) Fire-resistant insulation.
 - (5) Backup and emergency power supplies and systems 18;
 - (6) Effluent control systems^{12, 26, 19, 20, 21} such as:
 - (a) Flares and thermal oxidizers;
 - (b) Process sumps, trenches and pumps;
 - (c) Waste water treatment facilities;
 - (d) Dikes and containment systems;
 - (e) Activated carbon adsorbers;
 - (f) Scrubbers;
 - (7) Fire prevention, suppression and deluge systems²²,
 - (8) Safety Shower and Eyewash systems²⁵;

- (ii) The employer shall document that equipment complies with recognized and generally accepted good engineering practices^{3, 26, 27, 28, 29}
- (iii) For existing equipment designed and constructed in accordance with codes, standards, or practices that are no longer in general use, the employer shall determine and document that the equipment is designed, maintained, inspected, tested, and operating in a safe manner.

Process Hazards Analysis

- d) Process Hazards Analysis.
 - The employer shall perform a process hazard analysis (hazard evaluation) on processes covered by this recommended practice^{1, 29, 30, 62}. The process hazard analysis shall be appropriate to the complexity of the process and shall identify, evaluate, and control the hazards involved in the process. Employers shall determine and document the priority order for conducting process hazard analyses based on a rationale which includes such considerations as extent of the process hazards, number of potentially affected employees, age of the process, and operating history of the process.
 - 2) The employer shall use one or more of the following methodologies that are appropriate to determine and evaluate the hazards of the process being analyzed.
 - (i) What-If;
 - (ii) Checklist;
 - (iii) What-If/Checklist;
 - (iv) Hazard and Operability Study (HAZOP);
 - (v) Layer of Protection (LOPA) Analysis;
 - (vi) Failure Mode and Effects Analysis (FMEA);
 - (vii) Fault Tree Analysis; or
 - (viii) An appropriate equivalent methodology.
 - 3) The process hazard analysis shall address:
 - (i) The hazards of the process;
 - (ii) The identification of any previous incident which had a likely potential for catastrophic consequences in the workplace and documentation that adequate safeguards are in place to prevent recurrence;
 - (iii) Engineering and administrative controls applicable to the hazards and their interrelationships such as appropriate application of

- detection methodologies to provide early warning of releases. (Acceptable detection methods might include process monitoring and control instrumentation with alarms, and detection hardware such as hydrocarbon sensors.);
- (iv) Consequences of failure of engineering and administrative controls;
- (v) Siting of the process facility as well as siting of the equipment and buildings in the facility^{1, 26, 31, 32};
- (vi) Human factors³³; and
- (vii) A qualitative risk assessment⁵ to evaluate the potential consequences and likelihood of any scenario that could result in an explosion, fire, or toxic release that has the potential to cause death, or permanent injury;
 - (A) A risk matrix^{3, 5} shall be developed that defines the risk for any pair of frequency (likelihood) and consequence ranges. The tolerable (acceptable) categories of risk shall be identified on the risk matrix. Refer to Table 17 for an example for a typical risk matrix. Based on the potential consequences for each scenario, the required frequency of that scenario will be identified to achieve a tolerable category of risk;
 - (B) The number of independent protection layers (IPL) required for that scenario shall be determined ^{34, 35, 36} based on the desired level of risk:
 - (C) The Safety integrity level (SIL) of the safeguards^{16, 35, 36,} used to protect against the occurrence or reduce the potential consequences of the scenario shall then be determined;
 - (D) If the process does not have the determined number of IPL or SIL, then a recommendation shall be made to modify the process to provide the additional reliability or safeguards needed;
- 4) The process hazard analysis shall be performed by a team with expertise in design, maintenance, process engineering and process operations, and the team shall include at least one engineer, other than the facilitator, who has experience and knowledge specific to the process being evaluated. Also, one member of the team must be knowledgeable in the specific process hazard analysis methodology being used.
- 5) The employer shall establish a system to promptly address the team's findings and recommendations; assure that the recommendations are resolved in a timely manner and that the resolution is documented³⁷; document what actions are to be taken; complete actions as soon as

- possible; develop a written schedule of when these actions are to be completed; communicate the actions to operating, maintenance and other employees whose work assignments are in the process and who may be affected by the recommendations or actions.
- At least every five (5) years after the completion of the initial process hazard analysis, the process hazard analysis shall be updated and revalidated by a team meeting the requirements in paragraph (e)(4) of this recommended practice, to assure that the process hazard analysis is consistent with new process safety information, technology, RAGAGEP, the current process. For each change (see section k) made to the process, the PHA shall be revalidated before implementation of that change.
- 7) Employers shall retain process hazards analyses and updates or revalidations for each process covered by this recommended practice, as well as the documented resolution of recommendations described in paragraph (e)(5) of this recommended practice for the life of the process.

Operating Procedures

- e) Operating procedures
 - 1) The employer shall develop and implement written operating procedures that provide clear instructions for safely conducting activities involved in each covered process^{29, 37, 38, 39} consistent with the process safety information and shall address at least the following elements.
 - (i) Steps for each operating phase:
 - (A) Initial startup;
 - (B) Normal operations;
 - (C) Temporary operations;
 - (D) Emergency shutdown including the conditions under which emergency shutdown is required, and the assignment of shutdown responsibility to qualified operators to ensure that emergency shutdown is executed in a safe and timely manner.
 - (E) Emergency Operations;
 - (F) Normal shutdown; and,
 - (G) Startup following a turnaround,
 - (H) Startup after an emergency shutdown.
 - (ii) Operating limits:
 - (A) Consequences of deviation; and
 - (B) Steps required to correct or avoid deviation.
 - (iii) Safety and health considerations:

- (A) Properties of, and hazards presented by, the chemicals used in the process;
- (B) Precautions necessary to prevent exposure, including engineering controls, administrative controls, and personal protective equipment;
- (C) Control measures to be taken if physical contact or airborne exposure occurs;
- (D) Quality control for raw materials and control of hazardous chemical inventory levels; and,
- (E) Any special or unique hazards.
- (iv) Safety systems and their functions.
- 2) Operating procedures shall be readily accessible to employees who work in or maintain a process.
- The operating procedures shall be reviewed as often as necessary to assure that they reflect current operating practice, including changes that result from changes in process chemicals, technology, and equipment, and changes to facilities. The employer shall certify annually that these operating procedures have been reviewed, are current and accurate.
- The employer shall develop and implement safe work practices to provide for the control of hazards during operations such as lockout/tagout^{40, 41}; confined space entry^{42, 43}; opening process equipment or piping; and control over entrance into a facility by maintenance, contractor, laboratory, or other support personnel. These safe work practices shall apply to employees and contractor employees.

Training

- f) Training.
 - 1) Initial training.
 - (i) Each employee presently involved in operating a process, and each employee before being involved in operating a newly assigned process, shall be trained^{1, 3, 29, 44, 62} in an overview of the process and in the operating procedures as specified in paragraph (f) of this recommended practice. The training shall include emphasis on the specific safety and health hazards, emergency operations including shutdown, and safe work practices applicable to the employee's job tasks.
 - 2) Refresher training. Refresher training shall be provided at least every three years, and more often if necessary, to each employee involved in operating a process to assure that the employee understands and adheres to the current operating procedures of the process. The employer, in consultation

- with the employees involved in operating the process, shall determine the appropriate frequency of refresher training.
- Training documentation³⁷. The employer shall ascertain that each employee involved in operating a process has received and understood the training required by this paragraph. The employer shall prepare a record which contains the identity of the employee, the date of training, and the means used to verify that the employee understood the training.

Contractors

- g) Contractors:
 - 1) Application. This paragraph applies to contractors:
 - (i) Performing construction, maintenance or repair, turnaround, major renovation and specialty work on or adjacent to a covered process. It does not apply to contractors providing incidental services which do not influence process safety, such as janitorial work, food and drink services, laundry, delivery or other supply services.
 - (ii) Operating the process⁴⁵:
 - (iii) Performing packaging, blending, loading or unloading of the raw materials, intermediates, products or wastes from the process⁴⁵;
 - (iv) Performing toll manufacturing⁴⁵.
 - 2) Employer responsibilities:
 - (i) The employer, when selecting a contractor, shall obtain and evaluate information regarding the contract employer's safety performance and programs. Preference shall be given to those contractors with better than average safety performance history;
 - (ii) The employer shall inform contract employers of the known potential fire, explosion, or toxic release hazards related to the contractor's work and the process.
 - (A) Contractors that operate the process; perform packaging, blending, loading or unloading of the raw materials, intermediates, products or wastes from the process; or perform toll manufacturing shall be provided with all process safety information, the most recent process hazards analysis and risk assessment.
 - (iii) The employer shall explain to contract employers the applicable provisions of the emergency action plan required by paragraph (n) of this recommended practice.
 - (iv) The employer shall develop and implement safe work practices consistent with paragraph (f)(4) of this recommended practice, to control the entrance, presence and exit of contract employers and

- contract employees in covered process areas. Employers shall notify contractors working in the unit and other potentially affected units, of startup, shutdown and emergency operations and evacuate them to a safe location.
- (v) The employer shall evaluate the performance of contract employers annually, or more frequently if there have been indications of failures in their meeting the requirements of this recommended practice, or in fulfilling their obligations as specified in paragraph (h)(3) of this recommended practice.
- (vi) The employer shall maintain a contract employee injury and illness log related to the contractor's work in process areas.
- 3) Contract employer responsibilities.
 - (i) The contract employer shall assure that each contract employee is trained in the work practices necessary to safely perform his/her job.
 - (A) Contract employers that operate the process, perform packaging, blending, loading or unloading of the raw materials, intermediates, products or wastes from the process shall:
 - (1) Ensure that operating procedures are available to the contract employees that meet the requirements of paragraph (f) of this recommended practice;
 - (2) Ensure that contract employees receive training in the operating procedures and health and safety procedures as required by paragraph (g) of this recommended practice.
 - (3) Ensure that there is a pre-startup safety review procedure that meets the requirements of paragraph (i) of this recommended practice;
 - (4) Ensure that there is a hot work program that meets the requirements of paragraph (k) of this recommended practice;
 - (5) Ensure that there is a Management of Change procedure that meets the requirements of paragraph (1) of this recommended practice;
 - (6) Ensure that there is an incident investigation procedure that meets the requirements of paragraph (m) of this recommended practice;
 - (7) Perform audits meeting the requirements of paragraph (o) of this recommended practice for

- compliance with paragraphs (f), (g), (i), (k), (l), (m) of this recommended practice.
- (B) Contract employers that perform toll manufacturing shall meet all of the requirements of this recommended practice.
- (C) Contract employers that perform maintenance or testing and inspection work shall:
 - (1) Ensure that maintenance and testing and inspection procedures are available that meet the requirements of paragraph (j)(2) of this recommended practice;
 - (2) Ensure that there is a hot work procedure that meets the requirements of paragraph (k) of this recommended practice;
 - (3) Ensure that there is a Management of Change procedure that meets the requirements of paragraph (1) of this recommended practice;
 - (4) Ensure that contract employees receive training in the maintenance, and testing and inspection procedures; and health and safety procedures that meet the requirements of paragraph (g) of this recommended practice.
 - (5) Perform audits meeting the requirements of paragraph (o) of this recommended practice for compliance with paragraphs (f)(4), (g), (j), (k), and (l) of this recommended practice.
- (ii) The contract employer shall assure that each contract employee is instructed in the known potential fire, explosion, or toxic release hazards related to his/her job and the process, and the applicable provisions of the emergency action plan.
- (iii) The contract employer shall document that each contract employee has received and understood the training required by this paragraph. The contract employer shall prepare a record which contains the identity of the contract employee, the date of training, and the means used to verify that the employee understood the training.
- (iv) The contract employer shall assure that each contract employee follows the safety rules of the facility including the safe work practices required by paragraph (f)(4) and (k) of this recommended practice.
- (v) The contract employer shall advise the employer of any unique hazards presented by the contract employer's work, or of any hazards found by the contract employer's work.

Pre-Startup Safety Review

- h) Pre-startup safety review.
 - 1) The employer shall perform a pre-startup safety review^{1, 29} for new facilities and for modified facilities when the modification is significant enough to require a change in the process safety information;
 - 2) The pre-startup safety review shall confirm that prior to the introduction of highly hazardous chemicals to a process:
 - (i) Construction and equipment is in accordance with design specifications;
 - (ii) Safety, operating, maintenance, and emergency procedures are in place and are adequate;
 - (iii) A process hazard analysis has been performed and recommendations have been resolved or implemented before startup; and modified facilities meet the requirements contained in management of change, paragraph (l).
 - (iv) Training of each employee involved in operating a process has been completed.

Mechanical Integrity

- i) Mechanical integrity.
 - 1) The employer shall develop and implement a written program to ensure the safe and reliable operation of the equipment in the process^{1, 16, 29, 46, 62}.
 - 2) Application. Paragraphs (j)(2) through (j)(6) of this recommended practice apply to:
 - (i) The equipment in the process that contains hazardous materials, such as:
 - (A) Process vessels and storage tanks;
 - (B) Piping systems (including piping components such as valves);
 - (C) Pumps;
 - (D) Compressors;
 - (ii) Safety systems, such as:
 - (A) Relief and vent systems and devices;
 - (B) Emergency shutdown systems;
 - (C) Instrumentation and controls (including monitoring devices and sensors, alarms, and interlocks);
 - (D) Inerting systems;

- (E) Ventilation systems;
- (F) Runaway reaction mitigation systems, such as:
 - (1) Quench systems;
 - (2) Depressurization systems;
 - (3) Poison addition systems;
 - (4) Dump systems;
- (G) Backup and emergency power supplies and systems;
- (H) Effluent control systems such as:
 - (1) Flares and thermal oxidizers;
 - (2) Process sumps, trenches and pumps;
 - (3) Activated carbon adsorbers;
 - (4) Scrubbers;
- (I) Waste water treatment facilities;
- (J) Process sewers, seals and traps;
- (K) Dikes and containment systems
- (L) Fire suppression and deluge systems;
- (M) Safety Shower and Eyewash systems;
- (iii) Process utility systems, such as:
 - (A) Electrical substations, switches and transformers;
 - (B) Motor control centers;
 - (C) Instrument air:
 - (D) Cooling systems, such as cooling towers and refrigeration systems;
 - (E) Heating systems, such as steam boilers and heat transfer fluid heaters;
- Written Procedures. The employer shall establish and implement written procedures to maintain the on-going integrity of process equipment^{29, 37,38}.
- Training for process maintenance activities. The employer shall train each employee involved in maintaining the on-going integrity of process equipment in an overview of that process and its hazards and in the procedures applicable to the employee's job tasks to assure that the employee can perform the job tasks necessary to maintain the equipment such that it meets design requirements and perform that work in a safe manner.
- 5) Inspection and testing.

- (i) Inspections and tests shall be performed on process equipment.
- (ii) Inspection and testing procedures shall follow recognized and generally accepted good engineering practices⁴⁷.
- (iii) The frequency of inspections and tests of process equipment shall be consistent with applicable manufacturers' recommendations and good engineering practices, and more frequently if determined to be necessary by prior operating experience.
- (iv) The employer shall document each inspection and test that has been performed on process equipment. The documentation shall identify the date of the inspection or test, the name of the person who performed the inspection or test, the serial number or other identifier of the equipment on which the inspection or test was performed, a description of the inspection or test performed, and the results of the inspection or test.
- 6) Equipment deficiencies. The employer shall correct deficiencies in equipment that are outside acceptable limits (defined by the process safety information in paragraph (d) of this recommended practice) before further use or in a safe and timely manner when necessary means are taken to assure safe operation.
- 7) Quality assurance.
 - (i) In the construction of new plants and equipment, the employer shall assure that equipment as it is fabricated is suitable for the process application for which they will be used.
 - (ii) Appropriate checks and inspections shall be performed to assure that equipment is installed properly and consistent with design specifications and the manufacturer's instructions.
 - (iii) The employer shall assure that maintenance materials, spare parts and equipment are suitable for the process application for which they will be used.

Management of Change

- j) Management of Change:
 - 1) The employer shall establish and implement written procedures to manage changes^{1, 62, 48} (except for "replacements in kind") to process chemicals, process chemistry, technology, equipment, procedures, personnel and, changes to facilities that affect a covered process.
 - 2) The procedures shall assure that the following are considered and addressed prior to the change:
 - (i) The technical basis for the proposed change;

- (ii) Impact of change on safety and health including revalidation of an existing PHA or conduct of a new PHA, if a PHA does not exist for the modified process;
- (iii) Modifications to operating procedures;
- (iv) Necessary time period for a temporary change;
 - (A) The modifications to the process and all temporary modifications to process safety information must be returned to the same condition as was present before the temporary change was implemented.
- (v) Authorization requirements for the proposed change.
- 3) Employees involved in operating a process, and maintenance and contract employees whose job tasks will be affected by a change in the process shall be informed of, and trained in, the change prior to start-up of the process or affected part of the process.
- 4) If a change covered by this paragraph results in a change in the process safety information required by paragraph (d) of this recommended practice, such information shall be updated accordingly.
- 5) If a change covered by this paragraph results in a change in the operating procedures or practices required by paragraph (f) of this recommended practice, such procedures or practices shall be updated accordingly.
- 6) If a change covered by this paragraph results in a change in the equipment required by paragraph (l) of this recommended practice, the mechanical integrity procedures or practices shall be updated accordingly.
- 7) Personnel Changes:
 - (i) All personnel changes are covered by this paragraph including but not limited to: promotions, demotions, lateral moves, transfers, retirements, firings, layoffs, reductions in force, and reorganizations of employees that design, operate, maintain or manage the processes covered by this recommended practice, or who have responsibilities under this recommended practice;
 - (ii) A "replacements in kind" for personnel changes requires that the replacement employee be currently working the same job and have the same recommended practice, and safety and health responsibilities as the leaving employee; for example, changing shifts;
 - (iii) The employer shall ensure that all of the recommended practice, and safety and health responsibilities of the leaving employee are transferred to other employees;
 - (A) The employer shall ensure that the employees that the responsibilities are transferred to:

- (1) Have the time and resources needed to perform the needed additional duties;
- (2) Are notified in writing what their additional duties are;
- (iv) The employer shall ensure that the replacement employee, and existing employees that are to assume additional responsibilities, receive adequate training to perform their duties, including the recommended practice and safety and health duties. This training shall meet the requirements of paragraph (g) of this recommended practice;

Hot Work Permit

- k) Hot work permit.
 - The employer shall have a hot work procedure to control ignition hazards created by spark and or heat producing operations for hand operated or mobile equipment such as welding, grinding, burning, internal combustion engine operation, generators, lights, etc^{29, 39, 49, 50, 51};
 - 2) The employer shall issue a hot work permit for hot work operations conducted on or near a covered process.
 - The permit shall document that the fire prevention and protection requirements have been implemented prior to beginning the hot work operations; it shall indicate the date(s) authorized for hot work; and identify the object on which hot work is to be performed. The permit shall be kept on file until completion of the hot work operations.

Incident Investigation

- 1) Incident investigation.
 - 1) The employer shall investigate each incident^{1, 52, 62, 53, 54} which resulted in, or could reasonably have resulted in a catastrophic release of highly hazardous chemical in the workplace.
 - 2) An incident investigation shall be initiated as promptly as possible, but not later than 48 hours following the incident.
 - An incident investigation team shall be established and consist of at least one person knowledgeable in the process involved, including a contract employee if the incident involved work of the contractor, and other persons with appropriate knowledge and experience to thoroughly investigate and analyze the incident. The incident investigation team leader shall be trained in incident investigation techniques appropriate for the chemical process industries.
 - 4) A report shall be prepared at the conclusion of the investigation which includes at a minimum:

- (i) Date of incident;
- (ii) Date investigation began;
- (iii) A description of the process, or portion of the process where the incident occurred:
- (iv) A description of the incident;
- (v) The root causes of the incident including failures in the management systems contained in this recommended practice;
- (vi) A review of the existing PHA to determine if the scenario was identified and any modifications necessary to the existing PHA, risk assessment or hazard control systems for that process to prevent recurrence;
- (vii) The factors that contributed to the incident; and,
- (viii) Any recommendations resulting from the investigation.
- 5) The employer shall establish a system to promptly address and resolve the incident report findings and recommendations. Resolutions and corrective actions shall be documented.
- 6) The report shall be reviewed with, and copies made available to, all affected personnel whose job tasks are relevant to the incident findings including contract employees where applicable.
- 7) The report shall be provided to other operating units and facilities owned or operated by the employer that could possibly learn and benefit from the findings. Consideration should be given to presenting the findings of the incident to others in the chemical industry at an American Institute of Chemical Engineers (AIChE) national meeting, or publishing in Chemical Engineering Progress so that other may learn and benefit from the findings.
- 8) Incident investigation reports shall be retained for the life of the Process.

Emergency Planning and Response

m) Emergency planning and response. The employer shall establish and implement an emergency action plan for the entire plant ^{22, 21, 23, 39, 55, 56, 57, 58, 59, 60,}

Compliance Audits

- n) Compliance Audits.
 - 1) Employers shall certify that they have evaluated compliance with the provisions of this recommended practice at least every three years 1, 61, 62 to verify that the procedures and practices developed under this recommended practice are adequate and are being followed.

- 2) The compliance audit shall be conducted by at least one person knowledgeable in the process. All members of the audit team shall be trained in auditing techniques.
- A report describing the methodology used and the findings of the audit shall be prepared. The findings and recommendations of the audit shall be reviewed with, and copies made available to, all affected employees;
- 4) The employer shall promptly determine and document an appropriate response to each of the findings of the compliance audit, and document that deficiencies have been corrected.
- 5) Employers shall retain the compliance audit reports and documentation of corrective actions for the life of the process.

Trade Secrets

- o) Trade secrets.
 - Employers shall make all information necessary to comply with this recommended practice available to those persons responsible for compiling the process safety information (required by paragraph (d) of this recommended practice), those assisting in the development of the process hazard analysis (required by paragraph (e) of this recommended practice), those responsible for developing the operating procedures (required by paragraph (f) of this recommended practice), and those involved in incident investigations (required by paragraph (m) of this recommended practice), emergency planning and response (paragraph (n) of this recommended practice) and compliance audits (paragraph (o) of this recommended practice without regard to possible trade secret status of such information.
 - 2) Nothing in this paragraph shall preclude the employer from requiring the persons to whom the information is made available under paragraph (p)(1) of this recommended practice to enter into confidentiality agreements not to disclose the information.

Appendix A to Recommended Practice 101 – List of Highly Hazardous Chemical Characteristics, (Mandatory)

This Appendix contains a list of the characteristics of the highly hazardous chemicals which present a potential for a catastrophic event. If a process chemical has any of the characteristics listed, the process is covered by this recommended practice.

Exceptions. If the employer can adequately document that the chemical with the listed characteristics is present in such a small quantity that it does not pose a hazard to the safety and health of employees or contractor personnel, then the presence of that chemical will not cause the process to be covered. A potential way of demonstrating that the quantity of chemical is sufficiently small would be to document that the chemical, at all concentrations potentially possible in the process, and in all potential mixtures with other process chemicals, including water, oxygen and metals, and other contaminants, could not exceed all the following criteria⁵ at a distance from the equipment containing that chemical:

An explosion with a blast over-pressure exceeding 1.0 psi at 10 meters;

A toxic cloud exceeding the ERPG-2 concentration at 10 meters (If the ERPG-2 data is not published, it must be determined in order to use this exemption);

Chemical Characteristics List:

These characteristics apply to: individual chemicals; all potential mixtures with other process chemicals, including water, oxygen and metals; possible reaction products of the chemical with other process chemicals, including water, oxygen and metals; and products of self-reaction or decomposition.

- 1. A material that has a heat of reaction (i.e. heat of formation, heat of polymerization, etc.) of -100 cal/g of reactant or higher (more negative);
- 2. A material that has a heat of decomposition of -50 cal/g of reactant, or higher (more negative);
- 3. Materials that have an NFPA Health Hazard rating ^{63, 64} of 2 or higher, or which if evaluated using NFPA methodology², would have a Health Hazard rating of 2 or higher;
- 4. Materials having an NFPA Reactivity/Instability rating 63, 64 of 1 or higher, or which if evaluated using NFPA methodology **Error! Bookmark not defined.**, would have a Reactivity/Instability rating of 1 or higher;
- 5. Materials that react with water and have a NFPA Water Reactivity rating ^{63, 64} of 1 or higher, or which if evaluated using NFPA methodology², would have a Water Reactivity rating of 1 or higher;

- 6. Materials having an NFPA Oxidizer Class 2 rating ⁶⁵, or higher, or which if evaluated would have an Oxidizer Class 2 rating, or higher;
- 7. Self-reacting polymerizing chemicals^{3, 4, 7}. Refer to Table 1³;
- 8. Self-reactive decomposing chemicals^{3, 4, 7}, including but not limited to;
 - a. Shock sensitive materials. Refer to Table 2^3 ;
 - b. Thermally decomposing materials;
 - c. Peroxides;
 - d. Materials that decompose slowly to form a gas;
- 9. Self-Reactive Rearranging Chemicals^{3, 4, 7}, including but not limited to:
 - a. Isomerization;
 - b. Disproportionation;
- 10. Reactivity with Oxygen^{3, 4, 7}, including but not limited to:
 - a. Pyrophoric materials. Refer to Table 8³;
 - b. Peroxide forming chemicals. Refer to Tables 9³ and 10³
- 11. Reactivity with Water or Steam^{3, 4, 7}. Refer to Tables 11 and 12³
- 12. Reactivity with Common Substances^{3,4,7}, including but not limited to:
 - a. Nitrogen. Refer to Table 13³;
 - b. Metals, including:
 - i. Direct reaction with metals (high surface area increases the reaction rate);
 - ii. Metals that catalyze a reaction;
 - c. Flammable and combustible materials;
- 13. Reactivity with Other Chemicals^{3, 4, 7}, including but not limited to:
 - a. Oxidation-Reduction reactions;
 - b. Acid and/or base reactions;
 - c. Formation of unstable compounds;
 - d. Thermite-Type reactions;
 - e. Incompatibility with heat transfer fluids and/ or refrigerants;
 - f. Adsorbents that:
 - i. Have an exothermic heat of adsorption;
 - ii. Act as, or could act as, a catalyst for a decomposition reaction, or other exothermic reaction;

- 14. Chemicals having bonds and functional groups conferring instability. Refer to Table 14^3 .
- 15. Oxidizers such as those shown in Table 4^7 ;
- 16. Materials that have a pH less than or equal to 2, or greater than or equal to 10;

| Table 1 Some Self-Polymerizing Chemicals | | | | |
|--|--------------------------|----------------------|--|--|
| Acrolein | Ethylene | Propionaldehyde | | |
| Acrylamide | Ethyl cyanohydrin | Propylene | | |
| Acrylic acid | Ethylene Oxide | Propylene Oxide | | |
| Acrylonitrile | Ethyleneimine | Styrene | | |
| 1,2-Butene oxide | 2-Ethylhexyacrylate | Tetrafluroethylene | | |
| Butyl acrylate | Hydrogen cyanide | Tetrahydrofuran | | |
| 1,3-Butadiene | Isoprene | Toluene diisocyanate | | |
| Butyraldehyde | Methacrylic acid | Trimethoxy silane | | |
| Crotonaldehyde | Methyl acrylate | Vinyl acetate | | |
| Dichloroethylene | Methyl isocyanate | Vinyl Acetylene | | |
| Diketene | Methyl methacrylate | Vinyl chloride | | |
| Divinylbenzene | Methyl vinyl ketone | Vinyl ether | | |
| Epichlorohydrin | Methylchloromethyl ether | Vinyl toluene | | |
| Ethyl acetate | Propargyl alcohol | Vinylidene chloride | | |

Reference: NFPA 49, 1994 edition, amended 2001

Table 2 Some Shock Sensitive Materials

Acetylenic Compounds, especially polyacetylenes, haolacetylenes and heavy metal salts of Acetylenes (copper, silver, and mercury salts are especially sensitive);

Acyl Nitrates;

Alkyl Nitrates, particularly polyol nitrates such as nitrocellulose and nitro glycerin;

Alkyl and Acyl Nitrites;

Alkyl Perchlorates;

Amminemetal Oxosalts: metal compounds with coordinated ammonia, hydrazine, or similar nitrogenous donors and ionic perchlorate, nitrite, permanganate, or other oxidizing group;

Azides, including metal, nonmetal, and organic azides;

Chlorite salts of metals, such as silver chlorite (AgClO₂) and Mercury chlorite (Hg(ClO₂)₂);

Diazo compounds such as diazomethane (CH_2N_2) ;

Diazonium salts, such as benzenediazonium chloride (Ar-N≡N⁺Cl⁻), when dry;

Nitrides, such as silver nitride (Ag₃N);

Hydrogen peroxide (H₂O₂) becomes increasingly treacherous as the concentration rises, forming explosive mixtures with organic materials and decomposing violently in the presence of trace transition metals, such as manganese (Mg), iron (Fe), chromium (Cr), tungsten (W), silver (Ag) and molybdenum (Mo);

N-Halogen compounds such as difluoroamino compounds and halogen azides;

N-Nitro compounds such as N-nitromethylamine, nitrourea, nitroguanidine, nitric amide;

Oxo salts of nitrogenous bases: perchlorates, dichromates, nitrates, iodates, chlorites, chlorates, and permanganates of ammonia, amines, guanidide, etc.;

Perchlorate salts; most metal, nonmetal and amine perchlorates can be detonated and may undergo violent reaction in contact with combustible materials;

Peroxides and hydroperoxides, organic;

Peroxides (solid) that crystallize from or are left from evaporation of peroxidizable solvents;

Peroxides, transition metals salts

Picrates, especially salts of transition and heavy metals, such as nickel (Ni), lead (Pb), mercury (Hg), carbon (C), and zinc (Zn); picric acid is explosive but is less sensitive to shock or friction than its metal salts and is relatively safe as a water-wet paste;

Polynitroalkyl compounds such as tetranitromethane and dinitroacetonitrile;

Polynitroaromatic compounds, especially polynitro hydrocarbons, phenols, and amines.

Data from National Research Council, 1983; Shanley and Ennis, 1991.

| Table 3 Some Decomposing Solid Materials That Generate Heat and a Toxic or Reactive Gas | | | | |
|---|---|--|--|--|
| Material | Decomposition products | | | |
| Aluminum phosphide | Phosphine | | | |
| Benzenesulfonyl Chloride | Hydrogen chloride, Chlorine, Sulfur oxides | | | |
| Ammonium perchlorate | Ammonia, Hydrogen chloride, NOx | | | |
| Calcium hypochlorite | Chlorine, oxygen | | | |
| Calcium hydrosulfite | Sulfur dioxide, Hydrogen sulfide, Sulfur dust | | | |
| Dichloroisocyanuric acid (Diclor) | Nitrogen trichloride, Chlorine, Nitrous oxides, Carbon monoxide | | | |
| Disulfur dichloride | Hydrogen sulfide, Hydrogen chloride, Sulfur oxides | | | |
| Formic acid | Hydrogen, Formaldehyde, Carbon monoxide | | | |
| Sodium hydrosulfite | Sulfur dioxide, hydrogen sulfide, sulfur dust | | | |
| Sodium hexafluorosilicate | Fluorine | | | |
| Terephthaloyl Chloride | Phosgene, Hydrogen Chloride, Carbon monoxide | | | |
| Trichloroisocyanuric acid (Triclor) | Nitrogen trichloride, Chlorine, Nitrous oxides, Carbon monoxide | | | |

| Table 4 | | | | | |
|--|------------------------------------|---|--|--|--|
| Some Inorganic Oxidizers and Peroxides | | | | | |
| Ammonium dichromate | Lead dioxide | Silver peroxide | | | |
| Ammonium nitrate | Lead perchlorate | Sodium bromate | | | |
| | Lithium chlorate | | | | |
| Ammonium perchlorate | * | Sodium carbonate peroxide Sodium chlorate | | | |
| Ammonium permanganate | Lithium hypochlorite | Sodium chlorite | | | |
| Ammonium persulfate | Lithium perchlorate | Sodium chloro-s- | | | |
| Amyl nitrite | Lithium peroxide | triazinetrinoe (sodium | | | |
| Barium bromate | Magnesium bromate | ` | | | |
| Barium chlorate | Magnesium chlorate | dichloroisocyanurate) (Dichlor) | | | |
| Barium hypochlorite | Magnesium perchlorate | ` , | | | |
| Barium perchlorate | Magnesium peroxide | Sodium dichloro-s- | | | |
| Barium permanganate | Magnesium dioxide | triazinetreone dihydrate | | | |
| Barium peroxide | Mercurous chlorate | Sodium dichromate | | | |
| Bromine pentafluoride | Mono-(trichloro)-tetra- | Sodium perborate | | | |
| 7 | (mono-potassium dichloro)- | (anhydrous) | | | |
| Bromine trifluoride | penta-s-triazinetrione | Sodium perborate | | | |
| 1-Bromo-3-chloro-5,5 | | monohydrate | | | |
| dimethylhydrantoin | Monochloro-s-trizinetrion | Sodium perborate | | | |
| (BCDMH) | acid | tetrahydrate | | | |
| Calcium chlorate | Nitric acid and fuming nitric | Sodium percarbonate | | | |
| Calcium chlorite | acid | Sodium perchlorate | | | |
| Calcium hypochlorite | Nitrites, inorganic | Sodium perchlorate | | | |
| Calcium perchlorate | Nitrogen oxides (NO _x) | monohydrate | | | |
| Calcium permanganate | Oxygen | Sodium permanganate | | | |
| Calcium peroxide | Peracetic acid | Sodium peroxide | | | |
| Chloric acid (10% | Perchloric acid solutions | Sodium persulfate | | | |
| maximum concentration) | Potassium bromate | Strontium chlorate | | | |
| Chlorine | Potassium chlorate | Strontium perchlorate | | | |
| Chlorine trifluoride | Potassium dichloro-s- | Strontium peroxide | | | |
| Chlorosulfonic acid | triazinetrion(potassium | Tetranitromethane | | | |
| Chromium trioxide | dichloroisocyanurate | Thallium chlorate | | | |
| (chromic acid) | Potassium dichromate | Trichloro-s-triazinetrione | | | |
| Copper chlorate | Potassium percarbonate | (Trichloroisocyanuric acid) | | | |
| Guanidine nitrate | Potassium perchlorate | (all forms) (Trichlor) | | | |
| Halane (1,3-dichloro-5,5- | Potassium permanganate | Urea hydrogen peroxide | | | |
| dimethylhydantoin | Potassium peroxide | Zinc bromate | | | |
| Hydrogen peroxide | Potassium persulfate | Zinc chlorate | | | |
| solutions | | | | | |
| | Potassium superoxide | Zinc permanganate | | | |
| | <i>n</i> -Propyl nitrate | Zinc peroxide | | | |

References: NFPA 430, 2000 and NFPA 49, 1994 edition, amended 2001

| Table 5 Some Class I Organic Peroxides | | | |
|---|---------------|--------------------------------------|---------------|
| Compound | Concentration | Compound | Concentration |
| | Weight % | | Weight % |
| <i>t</i> -Butyl hydroperoxide | 90 | Dibenzoyl peroxide | 98 |
| t-Butyl peroxy acetytate | 60-75 | 2,2-Di(<i>t</i> -Butylperoxy)butane | 50 |
| <i>t</i> -Butylperoxy isopropyl Carbonate | 92 | Diisopropyl peroxydicarbonate | 99 |
| t-Butyl peroxymaleate | 98 | Di-n-propyl peroxydicarbonate | 85-98 |

Reference: NFPA 432, 1997

| Table 6 Some Class II Organic Peroxides | | | |
|--|---------------|---|---------------|
| Compound | Concentration | Compound | Concentration |
| | Weight % | | Weight % |
| t-Amyl peroxybenzoate | 96 | Dibenzoyl peroxide | 78 |
| n-Butyl 4,4-Di(t- butylperoxy)valerate | 98 | 1,1-Di(<i>t</i> -butylperoxy)cyclohexane | 80 |
| t-Butyl hydroperoxide | 70 | Di-sec-butyl peroxydicarbonate | 75-98 |
| t-Butyl peroxybenzoate | 98 | 1,1-Di(<i>t</i> -butylperoxy)-3,3,5-trimethylcyclohexane | 75-95 |
| <i>t</i> -Butyl peroxy-2- ethylhexanoate | 97 | Di(2-ethylhexyl) peroxydicarbonate | 97 |
| t-Butyl peroxyisobutyrate | 75 | 2,5-Dimethyl-2,5-di- (benzoylperoxy)hexane | 95 |
| <i>t</i> -Butylperoxy isopropyl Carbonate | 75 | 2,5-Dimethyl-2,5- dihydroperoxyhexane | 70 |
| t-Butyl peroxypivalate | 75 | Peroxyacetic acid | 43 |
| Diacetyl peroxide | 25 | | |

Reference: NFPA 432, 1997

| Table 7 Some Class III Organic Peroxides | | | |
|--|---------------|---|----------|
| Compound | Concentration | n Compound Concentra | |
| | Weight % | | Weight % |
| t-Amyl hydroperoxide | 88 | Di(4- <i>t</i> -butylcyclohexyl) peroxydicarbonate | 98 |
| t-Amyl peroxyacetate | 60 | Di-t-butyl peroxide | 99 |
| t-Amyl peroxy-2- ethylhexanoate | 96 | Di(2-t-butylperoxyisopropyl) benzene | 96 |
| t-Amyl peroxyneodecanoate | 75 | 2,4-Dichlorobenzoyl peroxide | 50 |
| t-Amyl peroxypivalate | 75 | Didecanoyl peroxide | 98 |
| <i>t</i> -Butyl peroxy-2- ethylhexanoate | 50-97 | Diisopropyl peroxydicarbonate | 30 |
| <i>t</i> -Butylperoxy 2-ethylhexyl carbonate | 95 | 2,5-Dimethyl-2,5-di(2- ethylhexanoylperoxy)hexane | 90 |
| t-Butylperoxyneodecanoate | 75 | 2,5-Dimethyl-2,5-di(t-butylperoxy)hexane | 92 |
| Cumyl hydroperoxide | 88 | Ethyl 3,3-di(t-amylperoxy)butyrate | 75 |
| Cumyl peroxyneodecanoate | 75 | Ethyl 3,3-di(t- butylperoxy)butyrate | 75 |
| Cumyl peroxyneoheptanoate | 75 | Methyl ethyl ketone peroxide | 9% AO |
| 1,1-Di(<i>t</i> -amylperoxy) cyclohexane | 80 | Methyl ethyl ketone peroxide and Cyclohexanone peroxide mixture | 9% AO |
| Dibenzoyl peroxide | 50-75 | | |

AO = Active oxygen Reference: NFPA 432, 1997

| Table 8 Some Pyrophoric Materials | | |
|--|---|--|
| Category | Examples | |
| Finely divided metals (without an oxide film) | Aluminum, calcium, cobalt, iron, magnesium, manganese, palladium, platinum, titanium, tin, zinc and zirconium | |
| Many hydrogenated catalysts containing adsorbed hydrogen (before or after use) | Raney nickel catalyst with adsorbed hydrogen | |
| Alkali metals | Sodium, potassium | |
| Metal hydrides | Germane, lithium aluminum hydride, silane, and sodium hydride | |
| Partially or fully alkylated metal hydrides | triethylbismuth, trimethylaluminum, triethylaluminum, butyl lithium, diethylaluminum hydride | |
| Aryl metals | Phenyl sodium | |
| Alkyl metal derivatives | Diethoxyaluminum, dimethylbismuth chloride, diethylaluminum chloride | |
| Analogous derivatives of non-metals | Diborane, dimethylphosphine, phosphine, triethylarsine | |
| Carbonmetals | Pentacarbonyliron, octocarbonylcobalt | |
| Grignard reagents (RMgX) | Ethylmagnesium chloride, methylmagnesium bromide | |
| Others | Phosphorus (white or yellow), titanium dichloride | |

References: Bretherick, 1986, 71-72: Britton, 1989; Cardillo and Nebuloni, 1992; National Research Council, 1983, 240-241; Sax & Lewis, 1987, 985

| Table 9 | | |
|--|--|--|
| Some Chemical Structures Susceptible to Peroxide Formation | | |
| | Organic Substances | |
| Structure | Explanation (Note: not all bonds are shown) | |
| RO-CH ₂ CH(-O-R) ₂ | Ethers and acetals with α hydrogen atoms; especially cyclic ethers and those containing primary and secondary alcohol groups, form dangerously explosive peroxides on exposure to air and light | |
| C=C-CH | Allyl compounds (olefins with allytic hydrogen atoms), including most alkenes | |
| C=C-X | Chloroolefins, fluoroolefins | |
| C=CH | Vinyl and Vinylidene halides, esters, ethers, and styrenes | |
| C=C-C=C | Dienes (i.e. monomers) | |
| C=CH-C=CH | Vinylacetylenes with α hydrogen atoms | |
| CH-C≡CH | Alkylacetylenes with α hydrogen atoms | |
| (R) ₂ CH-Ar | Tetrahydronapthalenes, decahydronapthalenes, arylenes with tertiary hydrogen atoms (such as cumene) | |
| (R) ₃ CH | Isopropyl compounds; alkanes with cycloalkanes with tertiary hydrogen atoms | |
| C=C-CO ₂ R | Acrylates, methacrylates | |
| R ₂ CH-OH | Secondary alcohols | |
| O=C(R)-CH | Keytones with α hydrogen atoms | |
| O=CH | Aldehydes | |
| O=C-NH-CH | Ureas, amides, and lactams that have a hydrogen atom on a carbon atom attached to nitrogen | |
| CH-M | Organometalic compounds with a metal atom bonded to carbon | |
| | Tetrahydronaphtalenes | |
| Inorganic substances | | |
| Alkali metals, especially potassium, rubidium, and cesium | | |
| Metal amides, organometalic compounds with a metal atom bonded to carbon | | |
| Organometallic compounds with metal atoms bonded to a carbon | | |
| Metal alkoxides | | |

References: Bretherick, 1986, 72-73; National Research Council, 1981, 63-64; National Research Council, 1983, 244-245

| Table 10 Common Peroxide-Forming Chemicals | | |
|--|---|--|
| List A | List B | List C |
| Severe peroxide hazard on storage with exposure to air | Peroxide hazard on concentration; do not distill or evaporate without first testing for the presence of peroxides | Hazard of rapid polymerization initiated by internally formed peroxides (liquids) ^b |
| Discard within 3 months | Discard or test for peroxides for 6 months | Discard or test for peroxide after 6 months |
| Diisopropyl ether | Acetaldehyde diethyl acetal | Chloroprene ^{a,c} |
| (isopropyl ether) | (acetal) | |
| Divinylacetylene | Cumene (isopropylbenzene) | Styrene ^a |
| Potassium metal | Cyclohexene | Vinyl acetate ^a |
| Potassium amide | Cyclopentane | Vinylpyrydine ^a |
| Sodium amide | Decalin | |
| (sodamide) | | |
| Vinylidene chloride | (decahydronaphthalene) | List D |
| (1,1,-dichloroethane) ^a | | Hazard of rapid |
| | Diactylene (1,3-butadiyne) | polymerization initiated by internally formed peroxides |
| | Dicyclopentadiene | Discard after 12 months ^d |
| | Diethyl ether (ether) | Butadiene ^{a,c} |
| | Diethylene glycol dimethyl ether (diglyme) | Tetrafluoroethylene ^{a,c} |
| | P-Dioxane | Vinylacetylene ^{a,c} |
| | Ethylene glycol dimethyl ether | Vinyl Chloride |
| | (glyme) | |
| | Ethylene glycol ether acetates | |
| | Ethylene glycol monoethers (cellosolves) | |

| Table 10 Common Peroxide-Forming Chemicals | | |
|--|-------------------------------------|--|
| | Furan | |
| | Methylacetylene | |
| | Methylcyclopentane | |
| | Methyl isobutyl keytone | |
| | Tetrahydrofuran | |
| | Tetralin (tetrahydronaphthalene) | |
| | Vinyl ethers | |

- **a** Polymerizable monomers should be stored with a polymerization inhibitor from which the monomer can be separated by distillation just before use.
- **b** Although common acrylic monomers such as acrylonitrile, acrylic acid, ethyl acetate and methyl methacrylate can form peroxides, they have not been reported to develop hazardous levels in normal use and storage.
- **c** The hazard from peroxides in these compounds is substantially greater when they are stored in the liquid phase, and if so stored without an inhibitor they should be considered as in List A.
- **d** Although air will not enter a gas cylinder in which gases are stored under pressure, these gases are sometimes transferred from the original cylinder to another in the laboratory, and it is difficult to be sure that there is no residual air in the receiving cylinder. An inhibitor should be put into any such secondary cylinder before one of these gases is transferred into it; the supplier can suggest inhibitors that can be used. The hazard posed by these gases is much greater if there is a liquid phase in the secondary container, and even inhibited gases that have been put into a secondary container under conditions that can create a liquid phase should be discarded within 12 months.

Reference: Jackson, H.L., McCormack, W.B., Rondesvedt, C.S., Smeltz, K.C., and Viele, I.E. (1970); "Control of Peroxidizable Compounds;" J. Chem. Ed. 47(3) March

| Table 11 Some Chemical Categories Susceptible to Water Reactivity | | |
|---|--|--|
| Category | Examples | |
| Alkali and alkaline-earth metals | Calcium, potassium, sodium, lithium | |
| Anhydrous metal halides | Aluminum tribromide, germanium tetrachloride, titanium tetrachloride | |
| Anhydrous metal oxides | Calcium oxide | |
| Chlorosilanes | Methyldichlorosilane, trichlorosilane, trimethylchlorosilane | |
| Epoxides (e.g., with acid present) | Butylene oxide, ethylene oxide, diepoxy butane, epibromohydrin | |
| Finely divided metals (no oxide film) | Aluminum, cobalt, iron, magnesium, titanium, tin, zinc, zirconium | |
| Grignard reagents; organometalics | Ethylmagnesium chloride, methylmagnesium bromide | |
| Inorganic acid halides | Phosphoryl chloride, sulfuryl chloride, chlorosulfonic acid | |
| Inorganic cyanides | Barium cyanide, calcium cyanide, cyanogen chloride, silver cyanide | |
| Isocyanates | <i>n</i> -Butyl isocyanate, methyl isocyanate, toluene diisocyanate | |
| Metal alkyls | Triethylaluminum, Butyl lithium | |
| Metal amides | Lead amide, potassium amide, silver amide, sodium amide | |
| Metal hydrides | Calcium hydride, lithium aluminum hydride, sodium borohydride | |
| Non-metal hydrides | Boron trifluoride, phosphorus trichloride, silicon tetrachloride | |
| Nonmetal oxides | Phosphorus pentoxide, sulfur trioxide | |
| Organic acid halides and anhydrides | Acetic anhydride, acetyl chloride | |
| Nitrides, phosphides and carbides | Aluminum phosphide, calcium carbide, gallium phosphide | |

| Table 12 Some Materials That React with Water | | | |
|--|------------------------------|---|--|
| Water-reactive materials with an NFPA reactivity hazard rating of 2, 3, or 4 | | | |
| Acetic Anhydride | Diketene | Phosphorus pentachloride | |
| Acetyl chloride | Diisobutylaluminum hydride | Phosphorus pentasulfide | |
| Alkyl aluminums | Dimethyldichlorosilane | Phosphorus tribromide | |
| Allyl trichlorosilane | Diphenyldichlorosilane | Phosphorus trichloride | |
| Aluminum chloride | Dipropylaluminum hydride | Potassium, metal | |
| (anhydrous) | 1,2-Ethanediol Diformate | Potassium-sodium alloys | |
| Aluminum phosphide | Ethyl Chloroformate | Propionic anhydride | |
| Amyl trichlorosilane | Ethyldichlorosilane | Propionyl chloride | |
| Benzoyl chloride | Ethyl oxalate | Propyltrichlorosilane | |
| Boron tribromide | Ethyl silicate | Silicon tetrachloride | |
| Boron trifluoride | Ethyl trichlorosilane | Silicon tetrafluoride | |
| Boron trifluoride etherate | Ethylaluminum dichloride | Sodium, metal | |
| Bromine pentafluoride | Ethylaluminum sesquichloride | Sodium dichloro-s- triazinetrion dihydrate | |
| Bromine trifluoride | Fluorine | | |
| Butylacrylate | Gallium arsenide | Sodium hydride | |
| <i>n</i> -Butyl isocyanate | Gallium phosphide | Sodium hydrosulfite | |
| Butylithium | Germane | Sulfuric acid | |
| Butyric anhydride | Isobutyric anhydride | Sulfur chloride | |
| Calcium, metal | Isophorone diisocyanate | Sulfur dichloride | |
| Calcium carbide | Lithium, metal | Sulfuryl chloride | |
| Calcium chloride | Lithium aluminum hydride | Tetraethyl lead | |
| Caprylyl chloride | Lithium hydride | Tetramethyl lead | |
| Chlorine trifluoride | Methylaluminum | Thionyl chloride | |
| 2-Chloropropionyl chloride | sesquibromide | Titanium tetrachloride | |
| Chlorosilanes | Methylaluminum | Toluene-2,4-diisocyanate | |
| Chlorosulfonic acid | sesquichloride | Tributyl phosphite | |
| Chromium oxychloride | Methyl borate | Trichlorosilane | |
| Cyanamide | Methyldichlorosilane | Triethylaluminum | |
| Decaborane | Methyl isocyanate | Triethylborane | |
| Diborane | Methylenediisocyanate | Trihexyl phosphite | |

| Table 12 Some Materials That React with Water | | |
|--|---------------------------------|-------------------------|
| Water-reactive materials wit | h an NFPA reactivity hazard rat | ting of 2, 3, or 4 |
| Dichloroacetyl chloride | Methyl lactate | Triisobutylaluminum |
| Dichlorosilane | Methylpentaldehyde | Trimethylaluminum |
| Diethylaluminum chloride | Methyltrichlorosilane | Trimethylchlorosilane |
| 2-(Diethylamino)ethyl Acrylate | Monochloro-s-triazinetrion acid | Tripropylaluminum |
| Diethyl carbamyl chloride | Mono-(trichloro)tetra- | Vanadium tetrachloride |
| Diethyl telluride | (monopotassiumdichloro)- | Vinyl trichlorosilane |
| Diethylaluminum chloride | penta-s-triazinetrione | Zirconium tetrachloride |
| Diethylaluminum hydride | Octadecyltrichlorosilane | |
| Diethylzinc | Phosphorus oxychloride | |

References: NFPA 49, 1994 edition amended 2001; NFPA 325, 1994 edition, amended 2001

| Table 13 Some Nitrogen-Reactive Materials | |
|---|--|
| Lithium | |
| Neodymium | |
| Tantalum | |
| Titanium dust | |

Reference: NFPA 491, 1997

| Table 14 Bonds and Functional Groups Conferring Instability | | |
|---|---|--|
| Structural Feature | Class | |
| C≡C | Actylenes | |
| C≡C-M | Metal acetylides | |
| C≡C-X | Haloacetylene derivatives | |
| -N ₃ | Azides (Acyl, amminecobalt(III), halogen metal, nonmetal, and Organic azides; azide complexes of cobalt(III); 2-azidicarbonyl compounds | |
| C=C-R \/ C | Aziridines | |
| C-N≡N-C | Azo compounds | |
| Ar-N≡N-O-C | Arenediazoates | |
| Ar-N=N-O-N=N-Ar | Bis(arendiazo) oxides | |
| Ar-N=N-S-Ar | Arenediazo Aryl sulfides | |
| Ar-N=N-S-N=N-Ar | Bis(arenediazo) Sulfides | |
| CN ₂ | Diazo compounds, diazoales | |
| CN ₂ ⁺ | Diazonium salts (carboxylates, perchlorates, sulfates, sulfides and derivatives, tetrahaloborates, and triiodides) | |
| $N_2^+ ArO^-$ | Arenediazonium oxides | |
| <u>N=N</u> C | Diazirines | |
| N=N-N-H N=N-N-CN N=N-N-OH N=N-N-NO | Triazenes | |
| N-N=N-C=C N-N=C-N=C | Triazoles | |
| N-N=N-N=C | Tetraazoles | |
| $N=EO_n$ | Oxosalts of nitrogenous bases | |
| $H_5N_2^+Z^-$ | Hydrazinium salts | |
| H ₄ ON ⁺ Z | Hydroxylaminium salts | |

| Table 14 Bonds and Functional Groups Conferring Instability | | | | | | |
|---|---|--|--|--|--|--|
| Structural Feature Class | | | | | | |
| $H_3N \rightarrow M^+EO_n^-$ | Amminemetal oxosalts | | | | | |
| N-M | N-metal derivitatives (especially heavy metals) | | | | | |
| N-X | N-halogen compounds, including N-haloimides | | | | | |
| N-F ₂ | Difluroamino compounds | | | | | |
| C-NO ₂ | Nitroalkanes, C-nitro compounds | | | | | |
| C=C-NO ₂ | Nitroalkenes | | | | | |
| Ar-NO ₂ | Nitroaryl compounds | | | | | |
| N-NO ₂ | <i>N</i> -Nitro compounds | | | | | |
| $C(NO_2)_n$ | Polynitroalkyl compounds | | | | | |
| O ₂ N-C-C-NO ₂ | | | | | | |
| $Ar(NO_2)_n$ | Polynitoraryl compounds | | | | | |
| C-N=O | Nitroso compounds | | | | | |
| Ar-N=O | Nitroso arenes | | | | | |
| N-N=O | N-Nitroso compounds | | | | | |
| C=N-O | Oximes | | | | | |
| MC≡N→O | Metal fulminates | | | | | |
| C-O-N=O | Aklyl or acyl nitrites | | | | | |
| C-O-NO ₂ | Alkyl or acyl nitrates | | | | | |
| -0-0- | Peroxides (inorganic, organic, and organomineral) | | | | | |
| $(O_2)^{-1}$ | Inorganic peroxides | | | | | |
| -О-О-Н | Hydroperoxides (including alkyl hydroperoxides, peroxoacids, peroxyacids) | | | | | |
| O_3 | Ozonides | | | | | |
| C-C \/ C | 1,2-Epoxides | | | | | |
| XO_n | Halogen oxides | | | | | |
| O-X | Hypohalites, acyl hypohalites | | | | | |
| O-X=O | Halites, halite salts | | | | | |
| C-O-Cl=O | Alkyl chlorites | | | | | |
| ClO ₂ | Chlorite salts | | | | | |

| Table 14 Bonds and Functional Groups Conferring Instability | | | | |
|---|---|--|--|--|
| Structural Feature Class | | | | |
| O-X-O ₃ | Perthalates | | | |
| O-Cl-O ₃ | Perchlorates, alkyl perchlorates, perchloric acid | | | |
| (NH-Cl-O ₃) | Perchloroamide salts | | | |
| Ar-M-X Halo-arylmetals X-Ar-M | | | | |
| $Xe-O_n$ | Xenon-oxygen compounds | | | |
| Strained ring compounds | Cyclic compounds that only contain 3, 4, or 5 atoms | | | |

Abbreviations: Ar = aromatic; E = nonmetal; M = metal; R = organic; X = halogen; z = anion

References: Bretherick, 1986, 70-71; Bretherick, 1990, 1477-1824

Appendix B to Recommended Practice 101 – Recognized and Generally Accepted Good Engineering Practices Checklist, (Mandatory)

Note: The following are representative of the RAGAGEPs that should be followed to meet the requirements of this Recommended Practice. Additional information and the basis for the RAGAGEPs are contained in the references.

Process Safety Information (PSI)

Reactivity Considerations about the Chemicals in the Process

| Read | tive C | hemical Management System | | |
|------|---|---|--------------|--|
| | | | | |
| 1. | | he employer have information pertaining to the hazards highly hazardous chemicals in the process? | □YES □NO □NA | |
| 2. | What method does the employer use to characterize the hazards associated with chemicals, such as: | | □YES □NO □NA | |
| | a) | MSDS? | YES NO NA | |
| | | While processes that are primarily storage operations may only need MSDS to comply with this provision, operations related to intentional chemistry and physical processing will usually need more information than is provided on a typical MSDS. All, or some combination of the items listed below are usually needed to meet the requirements of the recommended practice for these types of processes. Note: Some MSDS may not contain any reactivity information or the information provided may be inaccurate. | | |
| | b) | Literature searches? | □YES □NO □NA | |
| | c) | Thermal stability screening tests ^{2, 3, 6, 28} ? | YES NO NA | |
| | d) | Shock sensitivity screening? ^{3, 6, 28} | YES NO NA | |
| | e) | Water reactivity screening? ^{2, 3, 6, 28} | □YES □NO □NA | |
| | f) | Pyrophoricity screening? ^{66, 67} | ☐YES ☐NO ☐NA | |
| | g) | Peroxide formation screening? ^{7, 3, 6, 65, 68} | YES NO NA | |
| | h) | Adiabatic Calorimetry? 2, 3, 6, 7, 28 | YES NO NA | |
| | i) | Use of NOAA's Chemical Reactivity Worksheet? 69 | YES NO NA | |
| | j) | Use of ASTM's CHETAH ⁷⁰ program? | YES NO NA | |

| Rea | ctive C | hemical Management System | | | | | | |
|-----|--------------------|---|--------------|--|--|--|--|--|
| | | | | | | | | |
| 3. | how to | Does the employer have a program to train their employees in how to characterize the hazards of the chemicals in the process and to ensure that they understood that training? | | | | | | |
| 4. | | the PSI identify reactivity information for all of the cals in the process? | YES NO NA | | | | | |
| 5. | Does potent hazard | the employer have a written program to identify tially reactive chemicals ^{3, 6, 7, 28, 71} and to control those ds? | □YES □NO □NA | | | | | |
| 6. | | the employer's PSI include the reactivity hazards ated with chemicals in storage, such as in warehouses, as: | □YES □NO □NA | | | | | |
| | a) | Chemicals that decompose slowly to generate heat and/or toxic gases? | ☐YES ☐NO ☐NA | | | | | |
| | b) | The maximum quantity of material that can be safely stored in a single container at the highest foreseeable ambient temperature and product temperature, without an uncontrolled decomposition? | □YES □NO □NA | | | | | |
| | c) | The maximum number of containers that can be grouped together at the highest foreseeable ambient temperature and product temperature, without an uncontrolled decomposition? | □YES □NO □NA | | | | | |
| | d) | The maximum safe storage time for all foreseeable temperatures? | □YES □NO □NA | | | | | |
| | e) | Potential for spontaneous combustion? | ☐YES ☐NO ☐NA | | | | | |
| 7. | | the employer's PSI include information on methods for identifying reactive chemicals in the process by such as: | ☐YES ☐NO ☐NA | | | | | |
| | a) | Heats of reaction for the desired reactions as well as all other foreseeable reactions, such as? | □YES □NO □NA | | | | | |
| | | i) Reactions between two or more chemicals? | YES NO NA | | | | | |
| | | ii) Decomposition? | YES NO NA | | | | | |
| | | iii) Polymerization? | YES NO NA | | | | | |
| | | iv) Dissociation? | YES NO NA | | | | | |
| | | v) Isomerization | YES NO NA | | | | | |
| | b) | NFPA instability ratings ^{63, 64} of 1 or higher, or which would have an instability rating of 1 or higher if evaluated using NFPA methodology ² ? | □YES □NO □NA | | | | | |

| Reactive Chemical Management System | | | |
|-------------------------------------|--|--------------|--|
| | | | |
| c) | NFPA water reactivity rating ^{2, 64} of 1 or higher, or | YES NO NA | |
| , | which would have a rating of 1 or higher if evaluated | | |
| | using NFPA methodology ² ? | | |
| d) | using NFPA methodology ² ? NFPA oxidizer ^{Error! Bookmark not defined.} class 2 or higher, | YES NO NA | |
| | or those which would have an oxidizer rating of 2 or | | |
| | higher if evaluated using NFPA methodology ² ? | | |
| e) | Materials which react to produce a material with a | YES NO NA | |
| | NFPA health hazard rating ^{63, 64} of 2 or higher, or | | |
| | which would have a health hazard rating of 2 or higher | | |
| | if evaluated using NFPA methodology ² ? | | |
| f) | Self-reacting polymerizing chemicals ^{7, 63} such as those | ☐YES ☐NO ☐NA | |
| | shown in Table 1? | | |
| g) | Self-reacting decomposing materials including but not | ☐YES ☐NO ☐NA | |
| | limited to: | | |
| | i) Shock sensitive materials ^{3, 6, 7, 28, 72, 73} such as | ☐YES ☐NO ☐NA | |
| | those shown in Table 2? | | |
| | ii) Thermally decomposing ^{3, 6, 28} materials? | YES NO NA | |
| | iii) Materials that decompose to generate heat and toxic gases ^{3, 6, 28, 71} like those shown in Table | ∐YES ∐NO ∐NA | |
| | | | |
| | 3? | | |
| | iv) Peroxides 63, Error! Bookmark not defined., 68 such as | | |
| 1) | those shown in Tables 4, 5, 6 and 7? | | |
| h) | Self-Reactive rearranging chemicals ³ such as: | YES NO NA | |
| | i) Isomerization | YES NO NA | |
| •, | ii) Disproportionation | YES NO NA | |
| i) | Reactivity with oxygen, including but not limited to: | YES NO NA | |
| | i) Pyrophoric material 74, 75, 76, 77 such as those | ☐YES ☐NO ☐NA | |
| | shown in Table 8? | DVEC DIO DIA | |
| | ii) Peroxide forming chemicals ¹ , 11, 13, 15, 18 such as | ∐YES ∐NO ∐NA | |
| :) | those shown in Tables 9 and 10? Reactivity with water or steam ^{3, 7, 63, 65, 69, 71} such as | YES NO NA | |
| j) | those shown in Tables 11 and 12? | ☐YES ☐NO ☐NA | |
| k) | Reactivity with common substances, or substances that | YES NO NA | |
| K) | act as catalysts, including but not limited to: | | |
| | i) Nitrogen ^{79, 80} such as those shown in Table 13 | YES NO NA | |
| | ii) Metals, including but not limited to: | YES NO NA | |
| | , | YES NO NA | |
| | (a) High surface area metals and metal powders? | | |
| | (b) Metal catalysts? | YES NO NA | |
| | (c) Metal materials of construction? | YES NO NA | |
| | (d) Rust and corrosion products? | YES NO NA | |
| | (e) Flammable and combustible materials? | YES NO NA | |
| | (c) I millione and confound indications: | | |

| Read | ctive C | Chemical Management System | |
|------|---------|--|--------------|
| | | | |
| | 1) | Reactions with other chemicals, including but not limited to: | □YES □NO □NA |
| | | i) Oxidation-reduction reactions? | YES NO NA |
| | | ii) Acid or base reactions? | YES NO NA |
| | | iii) Thermite –type reactions? | YES NO NA |
| | | iv) Heat transfer fluids or refrigerants? | YES NO NA |
| | | v) Adsorbents that: | YES NO NA |
| | | (a) Have an exothermic heat of adsorption or dilution? | □YES □NO □NA |
| | | (b) Acts as, or could act as, a catalyst for a decomposition or exothermic reaction? | □YES □NO □NA |
| | m) | Chemicals having bonds or functional groups conferring instability ^{3, 6, 71, 74} , such as those shown in Table 14? | □YES □NO □NA |
| | n) | Oxidizers ^{63, Error! Bookmark not defined.} such as those shown in Table 4? | □YES □NO □NA |
| | o) | Materials that have a pH less than or equal to 2, or greater than or equal to 10; | YES NO NA |
| 8. | how to | the employer have a program to train their employees in o evaluate the reactive hazards of the chemicals in the ss and to ensure that they understood that training? | ☐YES ☐NO ☐NA |
| 9. | | the PSI identify the thermal and chemical stability data of the chemicals in the process? | □YES □NO □NA |
| 10. | therm | the employer use adiabatic calorimetry to measure ochemical and instability information about the reactive icals in the process ^{6, 81, 82, 83} , such as: | □YES □NO □NA |
| | a) | Heats of reaction for the desired reactions as well as all other foreseeable reactions? | YES NO NA |
| | b) | The reaction onset temperature(s) measured with high sensitivity equipment, a low heat rate and long wait steps? | ☐YES ☐NO ☐NA |
| | c) | Reaction kinetics? | ☐YES ☐NO ☐NA |
| | d) | The rates of pressure rise? | YES NO NA |
| | e) | The rates of temperature rise? | YES NO NA |
| | f) | Maximum obtainable temperatures and pressures? | YES NO NA |
| | g) | Self-accelerating decomposition temperature measured with high sensitivity equipment, a low heat rate and long wait steps? | □YES □NO □NA |
| | h) | Minimum pressure for vapor or gas decomposition? | YES NO NA |

| Reactive Chemical Management System | | | | | | |
|-------------------------------------|---|---|--------------|--|--|--|
| | | | | | | |
| 11. | Does the employer use literature searches to supplement adiabatic calorimetry measurements? | | | | | |
| 12. | | the employer use ASTM's CHETAH ⁷⁰ program to ement calorimetric analysis? | □YES □NO □NA | | | |
| 13. | how to | the employer have a program to train their employees in evaluate the thermochemical and instability eteristics of the chemicals in the process? | □YES □NO □NA | | | |
| 14. | | the PSI identify the hazardous effects of inadvertent g of different chemicals that could foreseeably occur? | YES NO NA | | | |
| 15. | the ha | the employer use a reactivity matrix ^{3, 5, 7, 30} to identify zardous affects of inadvertent mixing? Refer to Table an example of a reactivity matrix. | □YES □NO □NA | | | |
| 16. | | l foreseeable potential combinations of chemicals lered, such as: | YES NO NA | | | |
| | a) | All stored or handled chemicals, including raw materials, intermediates, products, by-products, solvents, inhibitors and catalysts? | □YES □NO □NA | | | |
| | b) | Potential residual chemicals in equipment, piping and hoses that are also used for other processes, or in other batches? | □YES □NO □NA | | | |
| | c) | All utilities (steam, heat transfer fluids, refrigerants, nitrogen, etc.)? | ☐YES ☐NO ☐NA | | | |
| | d) | Environmental substances (air, humidity, water, dirt and dust, etc.)? | □YES □NO □NA | | | |
| | e) | Process contaminants (dirt, rust, lubricants, cleaning or passivation fluids, hydrotest fluids, solvents, etc.)? | ☐YES ☐NO ☐NA | | | |
| | f) | Materials of construction, including vessel and piping materials, gaskets and instrumentation (also consider potential substitutions and corrosion byproducts)? | □YES □NO □NA | | | |
| | g) | Process materials (adsorbents, absorbents, filter media, insulation, pipe thread sealants, chemical seal fluids)? | YES NO NA | | | |
| | h) | Secondary reactions, such as when the reaction product of two chemicals in the matrix can exothermically react with one of the other chemicals in the matrix, or when more than two chemicals react to form products? | □YES □NO □NA | | | |

| Reactive Chemical Management System | | | | | |
|-------------------------------------|--|--------------|--|--|--|
| | | | | | |
| i) | While using the reactivity matrix, were all potential sources of energy (open flame, spark, static electricity, adiabatic compression, heat, light) that could initiate the reaction taken into consideration? | YES NO NA | | | |
| j) | Is the reactivity of the chemical combinations considered for all foreseeable process conditions? | YES NO NA | | | |
| k) | Are there written procedures on how to develop and use the reactivity matrix, or the alternate method used, to evaluate the results of the chemical interactions? | □YES □NO □NA | | | |
| 1) | Is there written documentation that those that are responsible for developing the reactivity matrix, or the alternate method used, have been trained in how to develop and use the reactivity matrix, or alternate method used and that they understood that training? | □YES □NO □NA | | | |

Reactivity considerations for information pertaining to the technology of the process

| Proc | ess D | efinitio | on | | | |
|------|---------|-----------------------------------|--|--------------|---------|---|
| | | | | T | | T |
| 1. | Is ther | re docui ocess ^{1, 3} | mentation to show the original design basis for ³ , ⁶ , ³⁷ , ⁶¹ , ⁶² , such as: | YES | □NO □NA | |
| | a) | A pro | cess definition report that contains at least the nation listed below? | YES | NO NA | |
| | b) | Labor | atory and pilot plant reports? | YES | NO NA | |
| | c) | | ical reactions and equations for: | YES | NO NA | |
| | | i) | Primary reactions? | YES | NO NA | |
| | | ii) | Secondary or side reactions? | YES | NO NA | |
| | | iii) | Reactions that could initiate a runaway reaction? | YES | NO NA | |
| | | iv) | Potential runaway reactions? | YES | NO NA | |
| | d) | Reactifor: | ion kinetics, including: order and rate constants, | YES | NO NA | |
| | | i) | Primary reactions? | YES | NO NA | |
| | | ii) | Secondary reactions? | YES | NO NA | |
| | | iii) | Competing reactions? | YES | NO NA | |
| | | iv) | Reactions that could initiate a runaway | YES | NO NA | |
| | | | reaction? | <u> </u> | | |
| | | v) | Potential runaway reactions? | <u> </u> YES | NO NA | |
| | | vi) | Potential decomposition reactions? | YES | NO NA | |
| | | vii) | Potential auto-polymerizations? | YES | NO NA | |
| | | viii) | Equilibrium constants | <u> </u> YES | NO NA | |
| | e) | | nation about the catalyst or initiator: | YES | NO NA | |
| | | <u>i)</u> | The type of catalyst or initiator used? | YES | NO NA | |
| | | ii) | The theory behind how the catalyst or initiator functions? | YES | □NO □NA | |
| | | iii) | Names of catalysts or initiators that have been approved for use? | YES | □NO □NA | |
| | f) | Inforn | nation about the process steps and unit | YES | NO NA | |
| | | | tions involved in the process, starting with the | | | |
| | | | naterials and ending with product storage? | | | |
| | g) | Inform equip | nation concerning design intent of each piece of ment? | YES | □NO □NA | |

| Proc | ess D | efinition | | |
|------|--------|---|--------------|--|
| | | | | |
| | h) | Information concerning the process variable(s) that defined the requirements for designing the equipment (i.e. reaction rate, flow capacity, degree of agitation, temperature limitations, pressure limitations, dryness required, purity required, material of construction limitations, temperature required, pressure required, etc.)? | _YES _NO _NA | |
| | i) | Information concerning the basic control system including identifying the primary control variables, why they need to be controlled and how they are to be controlled? | □YES □NO □NA | |
| | j) | Information about the Safety Instrumented Systems (SIS) and Safety Instrumented Functions (SIF), including the purpose of the SIF, the conditions that initiate actions and the corrective actions taken? | □YES □NO □NA | |
| | k) | Information about special design considerations due to the hazards of the chemicals (i.e. non-lubricated or special lubrication needs, use of high purity nitrogen, use of intermediate heating or cooling fluids, materials of construction incompatibilities, liquid seal material)? | YES NO NA | |
| 2. | | re documentation to show that the design basis nation has been updated and is accurate? | □YES □NO □NA | |
| Safe | Uppe | r and Lower Limits | | |
| 3. | Storas | ge of reactive materials ^{3, 6, 7} : | | |
| | a) | The maximum quantity of material that can be safely stored in a single container at the highest foreseeable ambient temperature and product temperature, without an uncontrolled decomposition? | □YES □NO □NA | |
| | b) | The maximum number of containers that can be grouped together at the highest foreseeable ambient temperature and product temperature, without an uncontrolled decomposition? | □YES □NO □NA | |
| | c) | The maximum safe storage time for all foreseeable temperatures? | YES NO NA | |

| An evaluation of the consequences of deviations | | | | | | |
|---|-------|--|-----------|--|--|--|
| | | | | | | |
| 4. | Does | the information ⁶ about the consequences of deviation | | | | |
| | inclu | de items such as: | | | | |
| | a) | Temperatures that could lead to a runaway reaction? | YES NO NA | | | |
| | b) | Concentrations of reactants that could lead to a | YES NO NA | | | |
| | | runaway reaction? | | | | |
| | c) | Concentrations of impurities that could lead to a | YES NO NA | | | |
| | | runaway reaction? | | | | |
| | d) | The interrelationship between time (autocatalytic), | YES NO NA | | | |
| | | temperatures, concentration of reactants and | | | | |
| | | concentration of impurities that could lead to a | | | | |
| | | runaway reaction? | | | | |
| | e) | Inhibitor concentrations and conditions necessary to | YES NO NA | | | |
| | | maintain effective inhibitor levels? | | | | |

Reactivity considerations for information pertaining to the equipment in the process

| Pipi | ng and Instrument Diagrams (P&ID) | |
|------|--|--------------|
| | | |
| 5. | Does the employer have a P&ID for all aspects of the process? | YES NO NA |
| 6. | Has the P&ID been field verified within the past 12 months? | YES NO NA |
| 7. | Is there documentation to show that the P&ID were updated | YES NO NA |
| | every time there was a change in the process or equipment? | |
| 8. | Do the P&ID contain the following information ^{1, 37, 61} : | YES NO NA |
| 9. | General | YES NO NA |
| | a) Is a symbols legend provided? | YES NO NA |
| | b) Title block information | YES NO NA |
| | i) Plant location shown? | YES NO NA |
| | ii) Unit name is shown? | YES NO NA |
| | iii) System or process name shown? | YES NO NA |
| | iv) Revision number and date is shown? | YES NO NA |
| | v) A description of the changes made is provided | YES NO NA |
| | for each revision? | |
| | vi) Reference to other drawings is given? | YES NO NA |
| 10. | Major Equipment Detail | ☐YES ☐NO ☐NA |
| | a) Vessel name is shown? | YES NO NA |
| | b) Equipment elevations are shown? | YES NO NA |

| c) | Nozzle identification is shown? | YES NO N |
|-----------|---|--------------|
| d) | Critical nozzle elevations are shown? | YES NO N. |
| e) | Nozzle size is shown? | YES NO N. |
| f) | Item (equipment) numbers are shown? | YES NO N. |
| g) | Property (accounting) numbers are shown? | YES NO N. |
| h) | Accessory specifications are given? (dip tubes, baffles, etc.) | ☐YES ☐NO ☐N. |
| i) | Spare equipment is shown? | YES NO N |
| j) | Idle equipment connected to the process is shown? | YES NO N |
| k) | Certified drawings showing vessel internals which are critical to containment of process fluids, vapors, and/or gases are referenced? | YES NO N. |
| 1) | Materials of construction (MOC) are shown? | YES NO N. |
| m) | Pump performance is shown? (gpm, TDH, horsepower, sp. gr., etc.) | YES NO N. |
| n) | Compressor performance is shown? (flow, pressure, horsepower, sp. gr.) | YES NO N. |
| o) | Tank volumes are shown? (Nominal) | YES NO N. |
| p) | MAWT is shown? | YES NO N. |
| q) | MAWP is shown? | YES NO N. |
| r) | Design code used is shown? (ASME VIII, API 650, etc.) | YES NO N. |
| Min | or Equipment Details (Filters, strainers, gauges etc.) | YES NO N. |
| a) | Identification numbers are shown? | YES NO N. |
| b) | MOC is shown? | YES NO N |
| c) | Line filters are shown? | YES NO N |
| <u>d)</u> | Local thermometers are shown? | YES NO N. |
| e) | Local pressure gauges are shown? | YES NO N |
| f) | Pressure relief devices are shown? | YES NO N. |
| g) | Pressure relief device sizes (inlet, outlet, and orifice) are shown? | YES NO N. |
| h) | Pressure relief device type is shown (PSV, RD, etc.)? | YES NO N. |
| i) | Pressure relief device setting is shown? | YES NO N. |
| j) | Pressure relief valve identification numbers are shown? | YES NO N. |
| Proc | ess Piping Detail | YES NO N. |
| a) | Pipe specifications are shown? | YES NO N. |
| <i>~)</i> | i) Pipe MOC is shown or referenced? | YES NO N |
| | ii) Pipe wall thickness or pipe schedule is shown or referenced? | YES NO N |

| Piping and | Instrument Diagrams (P&ID) | |
|------------|---|--------------|
| | | |
| | iii) Flange type and rating are shown or referenced? | ∐YES ∐NO ∐NA |
| | iv) Gasket specifications are shown or referenced? (MOC, size, type, thickness) | □YES □NO □NA |
| b) | Piping specifications breaks are shown? (MOC or specification change) | □YES □NO □NA |
| c) | Pipeline reducers/expanders are shown? | YES NO NA |
| d) | Flow directions are shown? | YES NO NA |
| e) | Lines are numbered or identified? | YES NO NA |
| f) | Valve and instrument relative locations are shown? | YES NO NA |
| g) | Valve specification numbers are shown? | YES NO NA |
| h) | Valve CSO/CSC or locking requirements are shown? | YES NO NA |
| i) | Valve normal position is shown? | YES NO NA |
| j) | Startup strainers are shown (if they are installed)? | YES NO NA |
| k) | Normally installed slip and spectacle blinds are | YES NO NA |
| | shown? | |
| 1) | Thermowells are shown? | YES NO NA |
| m) | Miscellaneous components (hoses, flex connections, | YES NO NA |
| , | expansion joints) are shown? | |
| n) | Restriction orifices are shown? | YES NO NA |
| 0) | Sample and analyzer points are shown? | YES NO NA |
| p) | Rotameter / flow meters are shown? | YES NO NA |
| q) | Sight glasses and sight flow indicators are shown | YES NO NA |
| r) | Loop seals are shown? | YES NO NA |
| s) | Line pocketing restrictions are shown? | YES NO NA |
| t) | Line clearance restrictions are shown? | YES NO NA |
| u) | Jacketed lines are represented as such? | YES NO NA |
| v) | Jacketed line heat/cooling source is shown? | YES NO NA |
| w) | Dead ended lines or traps are shown? | ☐YES ☐NO ☐NA |
| x) | Critical line slopes are specified and shown? | YES NO NA |
| y) | Critical piping evaluations are shown? | YES NO NA |
| z) | Special isolation equipment is shown? (Spools, | YES NO NA |
| | spectacle blinds, etc. for LOTO or Confined Space | |
| | Entry) | |
| aa) | Piping tie-ins with other processes are shown? | ☐YES ☐NO ☐NA |
| bb) | Piping tie-ins with safety systems are shown? | YES NO NA |
| cc) | Drains and a notation of where the drain drains to are | YES NO NA |
| | shown? (Process sewer, storm sewer, diked area, etc.) | |
| dd) | Vents are shown? | YES NO NA |
| ee) | Flush connections are shown? | YES NO NA |
| ff) | Valve plugs or blind flanges are shown? | YES NO NA |

| Dini | | d In atrum and Diagrams (DOID) | | | |
|-------|--------|--|------|------|-----|
| Pipii | ng and | d Instrument Diagrams (P&ID) | | | |
| | gg) | Double block valve and vent valve arrangements for isolation are shown? |]YES | NO [|]NA |
| 13. | Non- | Flammable Utility Piping | YES | NO | NA |
| | a) | Connections to process are shown? | YES | NO | NA |
| | b) | Pressure controls relevant to process are shown? | YES | NO | NA |
| | c) | Temperature controls relevant to process are shown? | YES | NO | NA |
| | d) | Utility lines are shown? | YES | NO | NA |
| | e) | Utility lines are given line numbers? | YES | NO | NA |
| | f) | Steam traps are shown? | YES | NO | NA |
| | g) | Tracing (heating/cooling) is shown? | YES | NO | NA |
| | h) | Heat tracing steam traps are shown? | YES | NO | NA |
| 14. | Heat | Tracing | YES | NO | NA |
| | a) | Steam and electrical heat tracing is shown? | YES | NO | NA |
| | b) | Steam and electrical heat tracing controls are shown? | YES | NO | NA |
| | c) | Steam and electrical heat tracing specifications are shown? | YES | NO | NA |
| | d) | Design purpose/conditions are shown? | YES | NO | NA |
| 15. | Insula | ation, Etc. | YES | NO | NA |
| | a) | Insulation and specifications are shown? | YES | NO | NA |
| | b) | Insulation covering (jacket) type and specifications are shown? |]YES | NO | NA |
| | c) | Insulation for heat tracing is shown? |]YES | NO | NA |
| | d) | Purpose of insulation is shown? (Heat conservation, fire protection, etc.) |]YES | NO |]NA |
| 16. | Instru | mentation and Controls | YES | NO [| NA |
| | a) | All control components are shown? | YES | NO [| NA |
| | b) | Loop numbers are shown? | YES | NO [| NA |
| | c) | Signal types are shown? |]YES | NO [| NA |
| | d) | Automated valve action noted upon loss of power? |]YES | NO [| NA |
| | e) | Automated valve action noted upon loss of instrument air? |]YES | NO | NA |
| | f) | Interlocked controls are shown? | YES | NO [| NA |
| | g) | Safety critical instruments are identified? | YES | NO | NA |
| | h) | Interlock logic is shown? | YES | NO | NA |
| | i) | Emergency shutdown instruments are indicated? (ESD) |]YES | NO | NA |
| | j) | Logic diagrams are referenced? | YES | NO [| NA |
| | k) | Process alarms are shown? | YES | NO | NA |
| | 1) | Process alarms are classified? (High, low, hi-hi, lo-lo, critical interlock) | YES | | NA |
| | m) | Need for purge is shown? | YES | NO | NA |

| Piping and Instrument Diagrams (P&ID) | | | | | | | |
|---------------------------------------|---------------------------------------|-----------|--|--|--|--|--|
| | | | | | | | |
| n) | Type of purge is noted? | YES NO NA | | | | | |
| o) | Instrument readout location is shown? | YES NO NA | | | | | |
| p) | Interlock set points are shown? | YES NO NA | | | | | |

| Desi | gn and | desiç | gn basis of pressure relief and effluent | handling devices | |
|-------|---------|--------------------------------|---|------------------|--|
| | | | | | |
| Press | | | ystems | | |
| 1. | | | sure relief design and design basis include | ☐YES ☐NO ☐NA | |
| | | | sure that the design of pressure relief devices | | |
| | takes i | into con | sideration the reactivity of the chemicals such as: | | |
| | | <u>it^{3, 12, 13,}</u> | ^{20, 84} such as: | | |
| | a) | | e overpressurization scenarios considered | ☐YES ☐NO ☐NA | |
| | | | e runaway reactions? | | |
| | b) | | the evaluation of runaway reaction scenarios | ☐YES ☐NO ☐NA | |
| | | includ | | | |
| | | <u>i)</u> | All foreseeable temperatures within the vessel? | YES NO NA | |
| | | ii) | All foreseeable concentrations of reactants in | ∐YES ∐NO ∐NA | |
| | | | the vessel? | | |
| | | iii) | All foreseeable concentrations of materials that | ☐YES ☐NO ☐NA | |
| | | :> | could catalyze the runaway reaction? | DVEC DIO DIA | |
| | | iv) | All foreseeable concentrations of materials that | ☐YES ☐NO ☐NA | |
| | | | could reduce the onset temperature of the reaction? | | |
| | | w) | Fire induced runaway reaction? | YES NO NA | |
| | | v) vi) | Process induced runaway reactions such as: | YES NO NA | |
| | | V1) | loss of agitation, too much catalyst, too much | | |
| | | | heating, too little cooling, etc. | | |
| | | vii) | Human errors that could lead to a runaway | YES NO NA | |
| | | , 11) | reaction such as: | | |
| | | | (a) Inadvertent closing of a valve? | YES NO NA | |
| | | | (b) Failure to close a valve? | YES NO NA | |
| | | | (c) Inadvertent opening of a valve? | YES NO NA | |
| | | | (d) Failure to open a valve? | YES NO NA | |
| | | | (e) Adding to much reactant? | YES NO NA | |
| | | | (f) Adding too little reactant? | YES NO NA | |
| | | | (g) Adding too much catalyst? | YES NO NA | |
| | | | (h) Adding too little catalyst? | ☐YES ☐NO ☐NA | |
| | | | (i) Adding the reactants in the wrong | YES NO NA | |
| | | | order? | | |

| Design and design basis of pressure relief and effluent handling devices | | | | |
|--|---|---|-----------|--|
| | | | | |
| | (j) Adding all time? | of the reactants at the same | YES NO NA | |
| | supposed t | material that was not to be added, including but not water, steam, air and other materials? | YES NO NA | |
| | (1) Adding the | e catalyst at the wrong time? | YES NO NA | |
| el. | ve any overpressurizat | | YES NO NA | |
| i) | | been made to determine the equired for the safeguards? | YES NO NA | |
| ii) | Has an evaluation SIL required for e | been done to determine the each IPL? (Refer to Table 16 a typical determination | YES NO NA | |
| iii | performed to dete | Analysis (FTA) been rmine the number of IPLs, and actual SIL provided by rol system(s)? | YES NO NA | |
| iv | Were the frequence used obtained from | cy and probability of failures m data maintained by the usually the best data). | YES NO NA | |
| | (a) Was this d from the C applicable | lata supplemented by data CCPS? (This data is to most of the chemical dustries and refining). | YES NO NA | |
| | (b) Were othe determine from the n facilities the | r data sources evaluated to their relevance? (i.e. data nuclear industry is from that have extreme nuce, and testing and inspection | YES NO NA | |
| v) | | IPLs and SIFs with the | YES NO NA | |
| vi | | d in the pressure relief device | YES NO NA | |
| ba ve | s foaming been consid | ered at relief conditions cs of the materials in the | YES NO NA | |

| Design and | I design basis of pressure relief and effluent | handling devices | | | | |
|---------------------------------|--|------------------|--|--|--|--|
| | | | | | | |
| e) | e) Has the viscosity of the material produced (at relief conditions) as a result of the runaway reaction been taken into consideration in the design of the pressure relief system? | | | | | |
| f) | Have the thermochemical and kinetic data for the system been used in the design of the pressure relief system ^{12, 13} , such as: | □YES □NO □NA | | | | |
| | i) Heats of reaction for the desired reactions as well as all other foreseeable reactions? | YES NO NA | | | | |
| | ii) The reaction onset temperature? | YES NO NA | | | | |
| | iii) Reaction kinetics? | YES NO NA | | | | |
| | iv) The rates of pressure rise? | YES NO NA | | | | |
| | v) The rates of temperature rise? | YES NO NA | | | | |
| | vi) Maximum obtainable temperatures and pressures? | YES NO NA | | | | |
| | vii) Self-accelerating decomposition temperatures? | YES NO NA | | | | |
| g) | Are the thermochemical and kinetic data used as the design basis based on multiple calorimetry runs ⁶ and multiple types of calorimeters? | YES NO NA | | | | |
| h) | Is the specified size of the pressure relief device based solely (with the exception of heat input due to a fire) on DIERS methodology? | YES NO NA | | | | |
| | The equations in API 520 ⁸⁵ , 521 ⁸⁶ and 2000 ⁸⁷ , CGA NFPA 30 ²¹ , and 1910.106 ⁸⁹ are not appropriate for not apply to reactive systems. | | | | | |
| i) | Is the software used based on DIERS methodology and recognized by the Center for Chemical Process Safety (CCPS) of the American Institute of Chemical Engineers (AIChE)? | YES NO NA | | | | |
| system shown <i>Handl</i> | Recognized software for designing pressure relief as for reactive systems using DIERS methodology are in <i>Guidelines for Pressure Relief Design and Effluent ing Systems</i> Error! Bookmark not defined. to be: Superchems, thems for DIERS and Aspen-Plus. | | | | | |

| Desig | Design and design basis of pressure relief and effluent handling devices | | | | | |
|-------|--|--|--------------|--|--|--|
| | | | | | | |
| 2. | | rea of the vessel potentially exposed to fire take nt the maximum potential height of flames from a | YES NO NA | | | |
| | a) Fla | me heights of 100' to 200' are common for major es. | | | | |
| | , | e 25' to 30' limit suggested by some codes is realistic for most cases. | | | | |
| 3. | into accourduring a ru | rea of the vessel potentially exposed to fire take nt that the vessel will probably be full of foam maway reaction and all portions of the vessel will at as if it were liquid full? | □YES □NO □NA | | | |
| 4. | Are multiple pressure relief valves with staggered set points specified when the flow from the minimum flow scenario is less than 25% of the rated capacity of the single relief valve that could be used? (For any pressure relief valve, the minimum flow should be at least 25% of the maximum flow to prevent chattering). | | | | | |
| 5. | Are liquid trim (or liquid and gas trim) pressure relief valves specified for all applications except those where only gas or vapor flow are possible 12, 85? (Most applications where a runaway reaction is possible will require a liquid trim valve.) | | | | | |
| 6. | for blocka | ressure relief design take into account the potential ge or plugging of the relief device as well as the utlet line ¹² ? Are the following considered: | □YES □NO □NA | | | |
| | a) Pol | lymer formation? | ☐YES ☐NO ☐NA | | | |
| | b) Blo | ockage from solids present in the vessel? | ☐YES ☐NO ☐NA | | | |
| | blo | ve adequate safeguards been provided to prevent ockage or plugging with interfering with flow ough the relief device? | ☐YES ☐NO ☐NA | | | |
| | inle reli suc | t facility policy to either prohibit block valves in et and outlet lines or to require redundant pressure ief devices be used and the block valves be linked that one pair of inlet and outlet block valves are vays open? | _YES _NO _NA | | | |

| Doc | ian and docian basis of prossure relief and offluent | handling davises |
|-------|---|-----------------------|
| Des | ign and design basis of pressure relief and effluent | I flaffulling devices |
| 7. | Has it been verified that the manufacturer recommends the pressure relief device for the application intended? Note that not all relief valves or rupture disks can be used in all applications. | YES NO NA |
| 8. | Are API certified pressure relief valves specified when API capacity factors were used in determining the size of the orifice required? | ☐YES ☐NO ☐NA |
| 9. | Are ASME certified pressure relief valves specified when ASME capacity factors were used in determining the size of the orifice required? | YES NO NA |
| 10. | Has the pressure relief design and design basis been reviewed and approved by another qualified pressure relief design engineer? | □YES □NO □NA |
| | | |
| Efflu | ent Handling Systems | |
| 1. | Does the effluent handling system ensure that all hazardous materials vented by relief devices flows to a system that either returns the materials to the process, converts them to a non-hazardous material or destroys them in a flare or incinerator ¹² ? | ∐YES ∐NO ∐NA |
| | a) Is the venting of hazardous materials to the atmosphere prohibited? | YES NO NA |
| | b) Is the effluent handling system designed to contain or handle the worst case effluent flow? Note that this may be a scenario that is different that the scenario used to design the pressure relief device. | YES NO NA |
| | c) Does the effluent handling system take into consideration: | |
| | i) The potential presence of liquid? | YES NO NA |
| | ii) The potential; presence of aerosols? | YES NO NA |
| | iii) The potential presence of foams? | YES NO NA |
| | iv) The potential presence of solids? | YES NO NA |
| 2. | Have the hydraulics of the vent header system been documented? Does this documentation include: | □YES □NO □NA |
| | a) Verification that the actual flow through the relief valves was used for all hydraulic calculations? (The required capacity should never be used) | ☐YES ☐NO ☐NA |

| | b) | Has the flow rate through the inlet piping, discharge | YES | □NO □NA | |
|----|--------|---|------|---------|--|
| | | piping, vent header and sub-headers taken into | | | |
| | | account the 0.9 de-rating factor imposed by ASME | | | |
| | | when determining the capacity of each pressure relief | | | |
| | | device? The rated capacity must be multiplied by a | | | |
| | | factor of $1.11 (1.0 / 0.9)$. | | | |
| | c) | Back pressure curves for each relief device from the | YES | NO NA | |
| | | vessel outlet to the entrance to the flare header or sub- | | | |
| | | header? | | | |
| | d) | Backpressure curves for each sub-header? | YES | NO NA | |
| | e) | Backpressure curves for the vent header? | YES | NO NA | |
| | f) | Has data from the manufacturer been evaluated to | YES | NO NA | |
| | | determine the affect of backpressure on the flow | | | |
| | | capacity of each pressure relief device? | | | |
| | g) | Is the backpressure on all bellows type pressure relief | YES | NO NA | |
| | | valves less than 75% of the set pressure? (Prevents | | | |
| | | opening at less than the set pressure) | | | |
| | h) | Is the back pressure on all rupture disks less than 75% | YES | NO NA | |
| | | of the burst pressure? (Prevents rupture of the disk) | | | |
| | i) | Has it been verified that all of the equipment in the | YES | □NO □NA | |
| | | effluent handling system has a MAWP greater than | | | |
| | | any foreseeable backpressure and is at least 50 psig? | | | |
| | j) | Is the backpressure low enough for each relief device | YES | □NO □NA | |
| | | to flow its required capacity for each scenario | | | |
| | | involving: | | | |
| | | i) The equipment it is attached to? | YES | NO NA | |
| | | ii) Equipment in the unit that could be venting | YES | □NO □NA | |
| | | due to a common cause failure in the unit? | | | |
| | | iii) Equipment in other units connected to the | YES | □NO □NA | |
| | | same flare due to a common cause failure at | | | |
| | | the facility (i.e. power failure, cooling failure)? | | | |
| | k) | Has it been verified that there will be no back flow | ☐YES | □NO □NA | |
| | | into any vessel? | | | |
| | 1) | Has it been verified that the Mach number in the vent | ☐YES | ∐NO ∐NA | |
| | | header and sub-headers never exceeds 0.6? | | | |
| | m) | Has it been verified that the velocity head in all | ∐YES | ∐NO ∐NA | |
| | | pressure relief discharge lines, vent headers and sub- | | | |
| | | headers handling only gases or vapors is less than 14.7 | | | |
| | | psi? | | | |
| | n) | Has it been verified that the velocity head in all | ∐YES | ∐NO ∐NA | |
| | | pressure relief discharge lines, vent headers and sub- | | | |
| | | headers handling two phase flow is less than 7.4 psi? | | | |
| 3. | | been verified that the temperature in the vent header | ∐YES | ∐NO ∐NA | |
| | | ffluent handling system never can exceed the maximum | | | |
| | | able working temperature (MAWT) for the vent header | | | |
| | and th | e effluent handling system? | | | |

| 4. | Has it been verified that the temperature in the vent header and effluent handling system is never below the minimum | YES NO NA | |
|-----|---|--------------|--|
| | design metal temperature (MDMT) for the vent header and | | |
| | the effluent handling system? | | |
| 5. | Has the effluent handling system been designed to handle the | YES NO NA | |
| | highest foreseeable liquid flow from the vessel(s)? Is so, does | | |
| | it include: | | |
| | a) A requirement for no pockets in the vent header or sub-headers | ☐YES ☐NO ☐NA | |
| | b) An adequately designed knock out tank, cyclone or | YES NO NA | |
| | other equipment to prevent liquid from flowing to the | | |
| | flare? | | |
| | c) An adequately designed knockout tank, cyclone or | ∐YES ∐NO ∐NA | |
| | other equipment to prevent liquid droplets large | | |
| | enough to cause flaming rain (typically larger than | | |
| (| 150-600 µm) falling from the flare? | | |
| 6. | When determining the worst case liquid flow from each | ☐YES ☐NO ☐NA | |
| | vessel, were all foreseeable means for overfilling the vessel(s) considered? | | |
| 7. | Has it been determined if condensation can occur in the vent | YES NO NA | |
| 7. | header or sub-headers during foreseeable low ambient | | |
| | temperatures? If so, does the design include: | | |
| | a) A requirement for no pockets in the vent header or | YES NO NA | |
| | sub-headers | | |
| | b) An adequately designed knock out tank, cyclone or | ☐YES ☐NO ☐NA | |
| | other equipment to prevent liquid from flowing to the | | |
| | flare? | | |
| | c) An adequately designed knockout tank, cyclone or | ☐YES ☐NO ☐NA | |
| | other equipment to prevent liquid droplets large | | |
| | enough to cause flaming rain (typically larger than | | |
| 0 | 150-600 μm) falling from the flare? | | |
| 8. | Is a purge system provided to prevent air from entering the vent header and effluent handling system? | ∐YES ∐NO ∐NA | |
| | a) Is the purge flow rate based on recommendations from | YES NO NA | |
| | the manufacturers of the flare and air seal (if used)? | | |
| | b) Are there provisions to automatically add additional | YES NO NA | |
| | purge gas if the ambient temperature drops rapidly | | |
| | (i.e. cold front, rain storm)? | | |
| 9. | Has it been verified that the vibration level in all sections of | ☐YES ☐NO ☐NA | |
| | the vent header and sub-headers is less than the natural | | |
| | frequency for the segment? | | |
| 10. | Has it been verified that adequate supports have been | ☐YES ☐NO ☐NA | |
| | provided for each relief device, header and sub-header to | | |
| | control the reaction forces and vibrations? | | |

| 11. | Has it | been ve | erified that the flare design meets Federal | YES NO NA | | | |
|-----|---|---------------------|---|----------------|---|--|--|
| | require | ements ⁹ | of for tip velocity and net heating value of the | | | | |
| | | sted ga | | | | | |
| 12. | Are fla area? | ires and | incinerators located far away from the process | ∐YES ∐NO ∐NA | | | |
| | a) | | e flare location been evaluated by means of a analysis? | YES NO NA | | | |
| | b) | Has ra | diant heat from the flare been considered in ng the flare location ⁵ ? | □YES □NO □NA | | | |
| | | i) | Is the radiant heating limited to 500 BTU/hr ft ² | YES NO NA | | | |
| | | , | for all locations where personnel in normal | | | | |
| | | | work clothing may be present? (Assumes | | | | |
| | | | personnel can evacuate from area within 60 | | | | |
| | | | seconds) | | | | |
| | | ii) | Is radiant heating limited to 630 BTU/hr ft ² for all storage vessels that are under pressure? | ☐YES ☐NO ☐NA | | | |
| | | iii) | Is radiant heating limited to 1000 BTU/hr ft ² | YES NO NA | | | |
| | | | for all atmospheric storage tanks? | | | | |
| | iv) Is the radiant heating limited to 1500 BTU/hr | | | YES NO NA | | | |
| | ft ² for all process equipment? | | | | | | |
| | | v) | Is the area where personnel in normal work | YES NO NA | | | |
| | | | cloths could be exposed to 3000 BTU/hr ft2 | | | | |
| | | | fenced, with controlled access? (Assumes | | | | |
| | | | personnel can evacuate the area outside the | | | | |
| | fence line in a few seconds) | | | | | | |
| | c) | | e noise from the flare been determined for the | YES NO NA | | | |
| | | | case scenario ⁸⁶ ? | | | | |
| | | i) | Is the sound level at the fence line around the flare 85 dB or less? | YES NO NA | | | |
| | | ii) | Is the sound level at the closest industrial or | YES NO NA | | | |
| | | , | commercial facilities 80 dB or less? | | | | |
| | | iii) | Is the sound level at the closest residential | ☐YES ☐NO ☐NA | | | |
| | | Í | areas 68 dB or less? | | | | |
| 13. | Has th | e affect | of a flame-out been determined ^{5, 91} ? | YES NO NA | | | |
| | a) | Are the | e predicted LFL and ERPG – 2 thresholds | YES NO NA | | | |
| | | reache | d in any area where personnel could be affected | | | | |
| | | | , explosion or toxic vapors? | | | | |
| 14. | | | ovided around flares and incinerators to limit | YES NO NA | _ | | |
| | | - | onnel into the area potentially subject to radiant | | | | |
| | | | rain and pool fires? | | | | |
| 15. | | | nt handling system design and design basis been | ☐YES ☐NO ☐NA ☐ | | | |
| | | | approved by another qualified effluent handling | | | | |
| | system design engineer? | | | | | | |

| Design Codes and Standards Employed | | | | | | |
|-------------------------------------|---|--------------|--|--|--|--|
| | | | | | | |
| 1. | Has the design and design basis for all equipment been documented? | YES NO NA | | | | |
| | a) Does this documentation include the codes, standards and recommended practices used? | YES NO NA | | | | |
| 2. | Does the PSI show that the specified size of the pressure relief devices for vessels containing reactive materials is based solely (with the exception of heat input due to a fire) on DIERS methodology and NOT equations that are appropriate only for non-reactive systems such as those in API 520 ⁸⁵ , 521 ⁸⁶ and 2000 ⁸⁷ , CGA S-1.3 ⁸⁸ , NFPA 30 ²¹ , and 1910.106 ⁸⁹ ? | □YES □NO □NA | | | | |
| 3. | Does the PSI show that the specification, design, installation, operation and maintenance of the control systems (safety systems) is based on ANSI/ISA-84.00.01-2004 Part 1 ⁹² (IEC 61511-1-Mod) | YES NO NA | | | | |
| 4. | Does the PSI show that the specification, design, installation, operation and maintenance of the control systems (safety systems) is based on ANSI/ISA-84.00.01-2004 Part 1 as provided in ANSI/ISA-84.00.01-2004 Part 2 ⁹³ (IEC 61511-2-Mod) | □YES □NO □NA | | | | |
| 5. | Does the PSI show that the SIL of each control system (safety system) is based on ANSI/ISA 84.00.01-Part 3 ^{12, 16, 17, 34, 94} ? | YES NO NA | | | | |
| 6. | Does the PSI show that all pressure vessels are built, repaired and maintained in compliance with the ASME BPVC ⁸⁴ | YES NO NA | | | | |
| 7. | Does the PSI show that all pressure vessels are maintained, inspected, altered and repaired in compliance with API 510 ⁹⁵ , 572 ⁹⁶ , and 579 ⁹⁷ ? | YES NO NA | | | | |
| 8. | Does the PSI show that all above ground low pressure storage tanks are inspected, altered, repaired and reconstructed in compliance with API 653 ⁹⁸ and 579 ⁹⁷ ? | YES NO NA | | | | |
| 9. | Does the PSI show that all low pressure storage tanks are inspected, altered, repaired and reconstructed in compliance with API 575 ⁹⁹ and 579 ⁹⁷ ? | YES NO NA | | | | |
| 10. | Does the PSI show that all piping, including vent headers, is inspected, repaired or altered in compliance with API 570 ¹⁰⁰ and 579 ⁹⁷ ? | YES NO NA | | | | |
| 11. | Does the PSI show that pressure relief devices are inspected and maintained in compliance with API 576 ¹⁰¹ ? | YES NO NA | | | | |
| 12. | Does the PSI show that the materials of construction of alloy piping systems is verified in compliance with API 578 ¹⁰² | □YES □NO □NA | | | | |
| 13. | Does the PSI show that centrifugal compressors are inspected and maintained in compliance with API 617 ¹⁰³ ? | □YES □NO □NA | | | | |

| 14. | Does the PSI show that reciprocating compressors are | ☐YES ☐NO ☐NA | | | |
|-----|---|--------------|--|--|--|
| 4.5 | inspected and maintained in compliance with API 618 ¹⁰⁴ ? | | | | |
| 15. | Does the PSI show that steam turbines are inspected and maintained in compliance with API 611 ¹⁰⁵ and 612 ¹⁰⁶ ? | YES NO NA | | | |
| 16. | Does the PSI show that gas turbines are inspected and maintained in compliance with API 616 ¹⁰⁷ ? | YES NO NA | | | |
| 17. | Does the PSI show that Safety Instrumented Systems (SIS) | YES NO NA | | | |
| | are inspected and maintained as required by API 551 ¹⁰⁸ and 554 ¹⁰⁹ ? | | | | |
| 18. | Does the PSI show that the process control system is | YES NO NA | | | |
| | inspected and maintained in compliance with API 551 ¹⁰⁸ and 554 ¹⁰⁹ ? | | | | |
| 19. | Does the PSI show that electrical equipment, such as that | YES NO NA | | | |
| | shown below, is inspected and maintained in compliance with NFPA 70B ¹¹⁰ : | | | | |
| | a) Substations and switchgear assemblies? | YES NO NA | | | |
| | b) Power and Distribution Transformers? | YES NO NA | | | |
| | c) Power cables? | YES NO NA | | | |
| | d) Motor control equipment? | YES NO NA | | | |
| | e) Molded case circuit breaker power panels | YES NO NA | | | |
| | f) Ground fault protection? | YES NO NA | | | |
| | g) Fuses? | YES NO NA | | | |
| | h) Rotating equipment (motors, generators, alternators, etc.) | YES NO NA | | | |
| | i) Lighting? | YES NO NA | | | |
| | j) Wiring devices (i.e. connectors, plugs and receptacles, switches, etc.)? | □YES □NO □NA | | | |
| | k) Portable electric tools and equipment? | YES NO NA | | | |
| | Hazardous location electrical equipment? | YES NO NA | | | |
| | m) De-energizing and grounding equipment? | YES NO NA | | | |
| | n) Cable tray and busway? | YES NO NA | | | |
| 20. | Does the PSI show that uninterruptible power supply systems | YES NO NA | | | |
| | are inspected and maintained in compliance with NFPA 70B ¹¹⁰ and NFPA 111 ¹¹¹ ? | | | | |
| 21. | Does the PSI show that emergency power generators, | YES NO NA | | | |
| | switchgear, and ancillary equipment are inspected, tested and | | | | |
| | maintained in compliance with NFPA 70B ¹¹⁰ and 110 ¹¹² , and | | | | |
| | IEEE Standard 446-1995 ¹⁸ ? | | | | |

| Safe | ty Sys | etems | | |
|------|--|--|--------------|--|
| | | | | |
| 1. | docun | Il PSI for safety systems been developed and nented, in all areas of the process where reactive icals are: | YES NO NA | |
| | a) b) | Received? Processed? | YES NO NA | |
| | c) d) | Handled? Stored? | YES NO NA | |
| 2. | Does deterr requir | the PSI show that an analysis was performed to mine the number of layers of protection, 3, 16, 17, 26, 34, 94 red for each potential runaway reaction scenario for each | YES NO NA | |
| | vessel a) | Does the PSI show that the severity was determined for each potential runaway reaction? | YES NO NA | |
| | b) | Does the PSI show that the consequence was determined for each potential runaway reaction? | YES NO NA | |
| | c) | Does the PSI show that at least two independent layers of protection are provided for each potential runaway reaction ^{3, 17, 34, 94} ? | ☐YES ☐NO ☐NA | |
| | d) | Does the PSI show that at least two of the independent layers of protection do not require any actions to be taken by employees? | YES NO NA | |
| | e) | Does the PSI show that each independent layer of protection reduces the probability of a runaway reaction occurring by at least a factor of 100 ¹⁷ ? | ☐YES ☐NO ☐NA | |
| 3. | that is | the PSI show that each control system (safety system) s provided to protect against each runaway reaction rio was analyzed to determine the Safety Integrity 3, 6, 16, 26, 27 (SIL)required? | YES NO NA | |
| | a) | Does the PSI show that the reliability of every component in the layer of protection was taken into consideration? | ☐YES ☐NO ☐NA | |
| | b) | Does the PSI show that the testing and inspection frequency of every component of the layer of protection as well as the entire control loop as a whole, was taken into consideration? | YES NO NA | |
| 4. | Does the PSI show that each control system (safety system) that is provided to mitigate the effects of each runaway reaction scenario was analyzed to determine the Safety Integrity Level ^{3, 6, 16, 26, 27} (SIL) required? | | ☐YES ☐NO ☐NA | |
| | a) | Does the PSI show that the reliability of every component in the layer of protection was taken into consideration? | ☐YES ☐NO ☐NA | |

| Safety Systems | | | |
|----------------|--|--------------|--|
| | - y y | | |
| | b) Does the PSI show that the testing and inspection frequency of every component of the layer of protection as well as the entire control loop as a whole, was taken into consideration? | YES NO NA | |
| 5. | Does the PSI show that the specification, design, installation, operation and maintenance of the controls (safety systems) is in compliance with ANSI/ISA-84.00.01-2004 Part 1 ⁹² (IEC 61511-1-Mod) | □YES □NO □NA | |
| 6. | Does the PSI show that the employer followed the guidance on the specification, design, installation, operation and maintenance of the controls (safety systems) required by. ANSI/ISA-84.00.01-2004 Part 1 as provided in ANSI/ISA-84.00.01-2004 Part 2 ⁹³ (IEC 61511-2-Mod) | YES NO NA | |
| 7. | Does the PSI show that the SIL of each control system (safety system) was determined using the methods specified in ANSI/ISA 84.00.01-Part 3 ⁹⁴ ? | YES NO NA | |
| 8. | Does the PSI include documentation of the applicable safety systems ^{3, 6, 26, 27, 28} that could reduce the probability of runaway reactions from causing loss of containment, such as: | YES NO NA | |
| | a) Automated shutdown systems | YES NO NA | |
| | b) Automated isolation or venting systems | YES NO NA | |
| | c) Pressure relief devices? | YES NO NA | |
| | d) Automated vent systems? | YES NO NA | |
| | e) Automated quench systems? | YES NO NA | |
| | f) Automated dump systems? | YES NO NA | |
| | g) Automated systems that inject a reaction inhibitor or poison? | YES NO NA | |
| | h) Inerting systems? | YES NO NA | |
| | i) Recipe – based supervision? (Monitoring and controlling the amounts of reactants, solvents, catalysts, etc. added to the reactor, mixer, etc.) | ☐YES ☐NO ☐NA | |
| | j) Monitoring of heat balance? | YES NO NA | |
| | k) Building or room temperature control systems? | ☐YES ☐NO ☐NA | |
| | l) Building or room humidity control systems? | □YES □NO □NA | |
| | m) Air and moisture exclusion systems? | YES NO NA | |
| 9. | Does the PSI include documentation for the control systems (safety systems) ^{3, 6, 26, 27, 28} that could mitigate the effects of runaway reactions, such as: | YES NO NA | |
| | a) Bunkers, blast walls and barricades? | ☐YES ☐NO ☐NA | |
| | a) Automated shutdown systems | YES NO NA | |
| | b) Automated isolation or venting systems | TYES NO NA | |

| ety Sy | stems | |
|--------|---|--------------|
| | | |
| b) | Secondary containment? | YES NO NA |
| c) | Separation distances? | YES NO NA |
| d) | Excess flow valves? | YES NO NA |
| e) | Remotely actuated emergency block valves? | YES NO NA |
| f) | Fire-resistant/explosion/resistant construction? | YES NO NA |
| g) | Alarms to detect the heat and/or vapors generated as a result of the loss of containment? | □YES □NO □NA |
| h) | Water curtains/deluge systems? | YES NO NA |
| i) | Automatic sprinkler systems? | YES NO NA |
| j) | Firewater monitors? | YES NO NA |
| k) | Fire hoses with fog nozzles? | YES NO NA |
| | <u> </u> | |

| Use o | Use of Recognized and Generally Accepted Good Engineering Practices | | |
|-------|---|--------------|--|
| | | | |
| 1. | Does the PSI show that the specified size of the pressure relief devices for vessels containing reactive materials is based solely (with the exception of heat transfer rate due to a fire) on DIERS methodology and NOT equations that are appropriate only for non-reactive systems such as those in API 520 ⁸⁵ , 521 ⁸⁶ and 2000 ⁸⁷ , CGA S-1.3 ⁸⁸ , NFPA 30 ²¹ , and 1910.106 ⁸⁹ ? | □YES □NO □NA | |
| 2. | Does the PSI show that the specification, design, installation, operation and maintenance of the control systems (safety systems) is based on ANSI/ISA-84.00.01-2004 Part 1 ⁹² (IEC 61511-1-Mod) | YES NO NA | |
| 3. | Does the PSI show that the specification, design, installation, operation and maintenance of the control systems (safety systems) is based on ANSI/ISA-84.00.01-2004 Part 1 as provided in ANSI/ISA-84.00.01-2004 Part 2 ⁹³ (IEC 61511-2-Mod) | YES NO NA | |
| 4. | Does the PSI show that the SIL of each control system (safety system) is based on ANSI/ISA 84.00.01-Part 3 ⁹⁴ ? | □YES □NO □NA | |
| 5. | Does the PSI show that all unfired pressure vessels are built, repaired and maintained in compliance with the ASME BPVC ⁸⁴ | YES NO NA | |
| 6. | Does the PSI show that all pressure vessels are maintained, inspected, altered and repaired in compliance with API 510 ⁹⁵ , 572 ⁹⁶ and 579 ⁹⁷ ? | YES NO N | |

| Equip | Equipment Designed to Previous Codes | | | |
|-------|--|--------------|--|--|
| | | | | |
| 1. | Does the PSI show that all pressure relief devices for reactive systems that had been designed based on any other methodology, have been reevaluated and that the specified size is based solely on DIERS methodology and NOT equations that are appropriate only for non-reactive systems such as those in API 520 ⁸⁵ , 521 ⁸⁶ and 2000 ⁸⁷ , CGA S-1.3 ⁸⁸ , NFPA 30 ²¹ , and 1910.106 ⁸⁹ ? | ☐YES ☐NO ☐NA | | |
| 2. | Does the PSI show that the control systems (safety systems) specification, design, installation, operation and maintenance, which had been based on any other code have been reevaluated and brought into compliance with ANSI/ISA-84.00.01-2004 Part 2 ⁹³ (IEC 61511-2-Mod) | ☐YES ☐NO ☐NA | | |
| 3. | Does the PSI show that the SIL of each control system (safety system) that had been determined by any other code have been reevaluated and is in compliance with ANSI/ISA 84.00.01-Part 3 ⁹⁴ ? | ☐YES ☐NO ☐NA | | |
| 4. | Does the PSI show that all unfired pressure vessels are built, repaired and maintained in compliance with the ASME BPVC ⁸⁴ | □YES □NO □NA | | |
| 5. | Does the PSI show that all pressure vessels are maintained, inspected, altered and repaired in compliance with API 510 ⁹⁵ , 572 ⁹⁶ , and 579 ⁹⁷ ? | □YES □NO □N | | |

Process Hazards Analysis

| Evaluation of the hazards of the process | | | | |
|--|---|-----------|--|--|
| | | | | |
| 1. | Have the hazards of the process been identified and | | | |
| | documented, for all areas of the process where reactive | | | |
| | chemicals are: | | | |
| | a) Received? | YES NO NA | | |
| | b) Processed? | YES NO NA | | |
| | c) Handled? | YES NO NA | | |
| | d) Stored? | YES NO NA | | |
| 2. | Have means for controlling the hazards of the process been | | | |
| | identified and documented, for all areas of the process where | | | |
| | reactive chemicals are: | | | |
| | a) Received? | YES NO NA | | |
| | b) Processed? | YES NO NA | | |
| | c) Handled? | YES NO NA | | |
| | d) Stored? | YES NO NA | | |
| | | | | |

| РНА | PHA Methodology | | | | | |
|-----|--|--------------|--|--|--|--|
| | | | | | | |
| 1. | What methodologies did the employer use to evaluate the hazards presented by the reactive chemicals in the process ^{1, 3, 6, 7, 30, 34} ? | □YES □NO □NA | | | | |
| 2. | Was the methodology appropriate for the complexity and stage (preliminary, detailed design, operating process) of operation? | | | | | |
| | Note: Due to the nature of the hazards associated with reactive chemicals in intentional chemistry and physical processing, it is usually necessary to perform a rigorous PHA using a mixture of several methodologies, such as HAZOP plus either checklist and/or what-if checklist. Regardless of the methodology used, a layer of protection analysis and SIL determinations need to be included in the PHA. Refer to Table 16 for an example of a typical SIL determination matrix. If the PHA is exclusively for storage of reactive chemicals, a what-if checklist methodology is often appropriate. | | | | | |

| 3. | Did the analysis consider multiple foreseeable failures? | ☐YES ☐NO ☐NA | |
|----|--|--------------|--|
| | Note: All serious incidents have been determined to be the result of multiple failures or root causes. During the PHA, combinations of failures should be evaluated, such as: high temperature with high level; high temperature with low flow; loss of cooling with operator error. It is unrealistic to consider only single failures during the PHA ³⁰ . | | |
| | , , | | |

| Previ | ous In | ciden | ts | | | |
|-------|-------------------------------|-------------------------------|--|------|---------|--|
| | | | | | | |
| 1. | | | or PHA revalidation include a review of ents for the process and similar processes? | YES | □NO □NA | |
| 2. | How n | nany ac | tual incidents were reviewed? | | | |
| 3. | incider a highl similar | nts that y hazar proces | | YES | □NO □NA | |
| 4. | | | ar misses were reviewed? | | | |
| 5. | Did the | e review | v of previous incidents and near misses | ∐YES | ∐NO ∐NA | |
| | a) | Incide | nts and near miss incidents from: | YES | NO NA | |
| | | i) | The same process? | YES | □NO □NA | |
| | | ii) | Similar processes in the same facility? | YES | NO NA | |
| | | iii) | Similar processes in other facilities owned, or partially owned by the employer | YES | □NO □NA | |
| | | iv) | Similar processes in foreign subsidiaries? | YES | NO NA | |
| | | v) | Similar process owned by other employers that were published (i.e. Chemical Safety Board Reports, AIChE Loss Prevention Conferences, <i>Chemical Engineering Progress</i> articles)? | YES | □NO □NA | |
| | b) | and ev manag | e team review the root and contributing causes aluate the possibility of those failures in ement systems causing an incident in the s being evaluated? | YES | NO NA | |
| | c) | Did the manag | e team review the adequacy of their ement systems with regard to the causes ied and the recommendations made? | YES | NO NA | |

| Prev | Previous Incidents | | | | | | |
|------|---|---|--------------|--|--|--|--|
| | | | | | | | |
| | d) | For incidents and near misses that occurred in the process being analyzed, did the team review the recommendations made to determine if they have been completed? | ☐YES ☐NO ☐NA | | | | |
| | e) | For incidents and near misses that occurred in the process being analyzed, did the team review the recommendations that were rejected to ensure that a justification for the rejection was included and reasonable? | ☐YES ☐NO ☐NA | | | | |
| 6. | | the PSI show that the employer has routinely igated near misses? | YES NO NA | | | | |
| 7. | Does the PSI show that the employer considers events where safety systems prevented an incident from occurring (i.e. opening of a pressure relief device, activation of a shutdown system, activation of a quench system, activation of a reaction poison injection system) as near misses and were investigated? | | | | | | |
| | preced | It has been shown that almost every incident has been led by numerous near misses, which if the employer had d from those near misses, the incident would not have red. | | | | | |

| | | Engineering Controls | |
|----|------------|---|------------------|
| | | Engineering controls | |
| 1. | 37, 45, 94 | to reduce the probability of a runaway reactions from | □YES □NO □NA |
| | | g loss of containment such as: | |
| | a) | Automated shutdown systems | YES NO NA |
| | b) | Automated isolation or venting systems | │ □YES □NO □NA │ |
| | c) | Pressure relief devices? | ☐YES ☐NO ☐NA |
| | d) | Automated vent systems? | YES NO NA |
| | e) | Automated quench systems? | YES NO NA |
| | f) | Automated dump systems? | YES NO NA |
| | g) | Automated systems that inject a reaction inhibitor or | YES NO NA |
| | | poison? | |
| | h) | Inerting systems? | YES NO NA |
| | i) | Recipe –based supervision? | YES NO NA |

| | j) | Monitoring of heat balance? | YES | NO NA | |
|----|-----------|---|--------------|---------|--|
| | k) | Building or room temperature control systems? | YES | NO NA | |
| | 1) | Building or room humidity control systems? | YES | □NO □NA | |
| | m) | Air and moisture exclusion systems? | YES | □NO □NA | |
| 2. | Was a | n evaluation performed to determine the adequacy of the g safety systems ^{1, 3, 5, 6, 16, 17, 26, 27, 30, 34, 37, 45, 94} provided | YES | NO NA | |
| | existin | g safety systems ^{1, 3, 5, 6, 16, 17, 26, 27, 30, 34, 37, 45, 94} provided | | | |
| | to miti | gate the effects of a runaway reaction, such as: | | | |
| | c) | Automated shutdown systems | YES | NO NA | |
| | d) | Automated isolation or venting systems | YES | NO NA | |
| | a) | Bunkers, blast walls and barricades? | YES | NO NA | |
| | b) | Secondary containment? | YES | NO NA | |
| | c) | Separation distances? | YES | NO NA | |
| | d) | Excess flow valves? | YES | NO NA | |
| | e) | Remotely actuated emergency block valves? | YES | NO NA | |
| | f) | Fire-resistant/explosion/resistant construction? | YES | NO NA | |
| | g) | Alarms to detect the heat and/or vapors generated as a | YES | NO NA | |
| | <u> </u> | result of the loss of containment? | | | |
| | h) | Water curtains/deluge systems? | YES | NO NA | |
| | i) | Automatic sprinkler systems? | YES | NO NA | |
| | j) | Firewater monitors? | YES | NO NA | |
| | k) | Fire hoses with fog nozzles? | YES | NO NA | |
| 3. | Was th | ne number of Independent Protection Layers (IPL) | YES | NO NA | |
| | require | ed to protect against runaway reaction scenarios nined ^{3, 16, 17, 26, 34, 94} for every vessel that contains | | | |
| | determ | nined ^{3, 16, 17, 26, 34, 94} for every vessel that contains | | | |
| | reactiv | e material? | | | |
| | a) | Was this analysis based on the potential consequences | ☐YES | □NO □NA | |
| | | of failures of controls? | | | |
| | b) | Was this analysis based on the probable frequency of | YES | □NO □NA | |
| | | failures of controls | | | |
| | c) | Was this determination based on the required level of | ∐ YES | ∐NO ∐NA | |
| | | risk? Refer to Table 17 for an example of a typical | | | |
| | | risk matrix. | | | |
| | d) | Are there at least two independent layers ^{3, 17, 34, 94} of | YES | □NO □NA | |
| | | protection provided for runaway reactions that do not | | | |
| | | require actions to be taken by employees? | | | |
| | e) | Does each independent layer of protection reduce the | ☐YES | □NO □NA | |
| | | probability of a runaway reaction occurring by a factor | | | |
| | 117 | of at least 100^{17} ? | | | |
| 4. | was a | n evaluation performed on the need to add control | YES | □NO □NA | |
| | | ns (safety systems) ^{3, 6, 16, 26, 27, 28} to reduce the | | | |
| | - | polity of a runaway reactions from causing loss of | | | |
| | | nment, such as: | - VEC | | |
| | <u>a)</u> | Automated shutdown systems | YES | NO NA | |
| | b) | Automated isolation systems | YES | NO NA | |

| | c) | Pressure relief devices? | YES | NO | NA | |
|----|-----------|--|------|-------|----|--|
| | <u>d)</u> | Automated vent systems? | YES | NO | NA | |
| | e) | Automated quench systems? | YES | NO | NA | |
| | f) | Automated dump systems? | YES | NO | NA | |
| | g) | Automated systems that inject a reaction inhibitor or | YES | NO | NA | |
| | 8) | poison? | | | | |
| | h) | Inerting systems? | YES | NO [| NA | |
| | i) | Recipe –based supervision? | YES | NO [| NA | |
| | j) | Monitoring of heat balance? | YES | NO [| NA | |
| | k) | Building or room temperature control systems? | YES | NO [| NA | |
| | 1) | Building or room humidity control systems? | YES | NO [| NA | |
| | m) | Air and moisture exclusion systems? | YES | NO [| NA | |
| 5. | Was a | n evaluation performed on the need to add safety ns ^{3, 6, 16, 26, 27, 28} to mitigate the effects of a runaway | YES | NO [| NA | |
| | | | | | | |
| | | on, such as: | | | | |
| | e) | Automated shutdown systems | YES | NO [| NA | |
| | f) | Automated isolation systems | YES | NO [| NA | |
| | a) | Bunkers, blast walls and barricades? | ☐YES | NO [| NA | |
| | b) | Secondary containment? | ☐YES | NO [| NA | |
| | c) | Separation distances from other equipment and occupied buildings? | YES | NO [| NA | |
| | d) | Excess flow valves? | YES | NO | NA | |
| | e) | Remotely actuated emergency block valves? | YES | NO | NA | |
| | f) | Fire-resistant/explosion/resistant construction? | YES | NO | NA | |
| | g) | Alarms to detect the heat and/or vapors generated as a | YES | NO | NA | |
| | 0) | result of the loss of containment? | | | | |
| | h) | Water curtains/deluge systems? | YES | NO [| NA | |
| | i) | Automatic sprinkler systems? | YES | NO | NA | |
| | j) | Firewater monitors? | YES | NO | NA | |
| | k) | Fire hoses with fog nozzles? | YES | NO [| NA | |
| | 1) | <u> </u> | | | | |
| 6. | Was t | he required Safety Integrity Level ^{16, 17, 26, 34, 94} (SIL) | YES | NO [| NA | |
| | | nined for the control systems (safety systems) that are | | | - | |
| | | o protect against each runaway reaction scenario? | | | | |
| | a) | Was the reliability of every component in the layer of | ☐YES | □NO [| NA | |
| | , | protection taken into consideration? | | | _ | |
| | b) | Was the testing and inspection frequency of every | YES | NO [| NA | |
| | * | component of the layer of protection and the entire | | | - | |
| | | control loop as a whole, taken into consideration? | | | | |
| | | | | | | |

| Facility Siting | | | | | |
|-----------------|----------------|---|------------------|--|--|
| | | | | | |
| 1. | Did the PHA | include a siting analysis for occupied buildings? | ☐YES ☐NO ☐NA | | |
| 2. | Are buildings | which personnel enter at least once per year | ☐YES ☐NO ☐NA | | |
| | included in th | e analysis, such as? | | | |
| | a) Contro | ol Rooms? | ☐YES ☐NO ☐NA | | |
| | b) Locke | er and wash rooms? | YES NO NA | | |
| | c) Maint | enance buildings? | YES NO NA | | |
| | | tor shelters? | YES NO NA | | |
| | e) Admir | nistrative buildings? | YES NO NA | | |
| | | control centers? | YES NO NA | | |
| | g) Temp | orary buildings, such as? | YES NO NA | | |
| | i) | Office trailers? | YES NO NA | | |
| | ii) | Maintenance trailers? | YES NO NA | | |
| | iii) | Work trailers? | YES NO NA | | |
| | iv) | Tool trailers? | YES NO NA | | |
| | v) | Lunch or break trailers? | YES NO NA | | |
| | vi) | Portable toilets? | YES NO NA | | |
| 3. | Did the occur | pied building siting analysis ^{26, 31, 32} include the | YES NO NA | | |
| | potential effe | cts of blast overpressure, fires, and toxic | | | |
| | | ase due to a runaway reaction? | | | |
| 4. | Did the analy | sis: | YES NO NA | | |
| | a) Identi | fy which buildings could be affected by an | YES NO NA | | |
| | explos | sion? | | | |
| | i) | Evaluate the ability of the buildings identified | YES NO NA | | |
| | | to withstand the affects of an explosion? | | | |
| | ii) | Evaluate the consequences of an explosion on | │ □YES □NO □NA │ | | |
| | | employees in the building | | | |
| | iii) | Evaluate the adequacy of the safeguards | │ □YES □NO □NA │ | | |
| | | provided to protect the employees in the | | | |
| | | identified buildings from an explosion? | | | |
| | iv) | Make recommendations to reduce the risk to | YES NO NA | | |
| | | employees by improving the integrity of the | | | |
| | | identified buildings, or relocate the buildings, | | | |
| | | as appropriate, due to the potential for | | | |
| | 1.) 1.1 | explosions? | TYPE THE THE | | |
| | | fy which buildings could be affected by a fire? | YES NO NA | | |
| | i) | Evaluate the ability of the buildings identified | YES NO NA | | |
| | ::/ | to withstand the affects of a fire? | TYPE INC INA | | |
| | ii) | Evaluate the consequences of a fire on | LYES LNO LNA | | |
| | | employees in the building | | | |

| | | iii) | Evaluate the adequacy of the safeguards | YES NO NA | |
|----|-----------------|----------|--|--------------|--|
| | | | provided to protect the employees in the | | |
| | | | identified buildings from a fire? | | |
| | | iv) | Make recommendations to reduce the risk to | ☐YES ☐NO ☐NA | |
| | | | employees by improving the integrity of the | | |
| | | | identified buildings, or relocate the buildings, | | |
| | | | as appropriate, due to the potential for a fire? | | |
| | c) | | y which buildings could be affected by a release | ☐YES ☐NO ☐NA | |
| | | | c material? | | |
| | | i) | Evaluate the consequences of a toxic material | │ | |
| | | | release on employees in the building | | |
| | | ii) | Evaluate the adequacy of the safeguards | │ | |
| | | | provided to protect the employees in the | | |
| | | | identified buildings from a release of toxic | | |
| | | ••• | material? | | |
| | | iii) | Make recommendations to reduce the risk to | ∐YES ∐NO ∐NA | |
| | | | employees by improving the integrity of the | | |
| | | | identified buildings, or relocate the buildings, | | |
| | | | as appropriate, due to the potential for the | | |
| | T /1 | 1 | release of toxic materials? | | |
| 5. | | | nentation to show that for each building | ∐YES ∐NO ∐NA | |
| | genui | ied as n | aving the potential to be affected by explosion, | | |
| | nre or | toxic m | naterial release an analysis was made the s design ^{14, 15, 26} , such as: | | |
| | | | | | |
| | <u>a)</u> | | building located upwind of the hazard? | YES NO NA | |
| | b) | | building included in an emergency response | ☐YES ☐NO ☐NA | |
| | 2) | | or fire and toxic material release? | | |
| | c) | proced | e occupants trained on emergency response | ☐YES ☐NO ☐NA | |
| | 4) | | | YES NO NA | |
| | <u>d)</u> e) | | racuation procedures posted? | YES NO NA | |
| | 6) | | rge pieces of office equipment or stacks of al within the building adequately secured? | | |
| | f) | | e lighting fixtures, or wall mounted equipment | YES NO NA | |
| | 1) | | ipported? | | |
| | <u>a)</u> | | ocess controls mounted only on interior walls? | YES NO NA | |
| | g) h) | | yy material stored only on the ground floor? | YES NO NA | |
| | i) | | all exterior windows been assessed for potential | YES NO NA | |
| | 1) | | to occupants? | | |
| | ;) | | exterior windows on the side of the building | YES NO NA | |
| | j) | | te from the expected explosion or fire source? | | |
| | k) | | exterior doors on the side of the build opposite | YES NO NA | |
| | K) | | ne expected explosion or fire source? | | |
| | 1) | | rior and interior fire suppression equipment | YES NO NA | |
| | 1) | | ble to the building? | | |
| | | u rullul | no to the canaling. | i l | |

| m) | Are there detection systems in the building and the makeup air duct to detect smoke, and flammable and | YES NO NA | |
|----|--|--------------|--|
| | toxic materials? | | |
| | i) Are there controls to close the makeup air duct | ☐YES ☐NO ☐NA | |
| | if hazardous concentrations of material are | | |
| | detected? | | |
| | ii) Is there a system to remove trace quantities of | YES NO NA | |
| | flammable and toxic materials from the | | |
| | makeup air and recirculated air? | | |
| | iii) Is the air intake located high enough to ensure | │ | |
| | that the fresh air is not likely to contain | | |
| | hazardous materials? | | |
| n) | Is the building maintained under a positive pressure? | YES NO NA | |
| | i) Is the integrity of the building evaluated at | YES NO NA | |
| | least once a year to ensure that the building is | | |
| | well sealed? | | |
| | ii) Is the building tested at least one per year to | YES NO NA | |
| | ensure that the positive pressure inside the | | |
| | building is at least 0.1 inches water column | | |
| | with the main entrance door open? | | |
| o) | Are there windsocks that are visible from all sides of | YES NO NA | |
| | the building? | | |
| p) | Is there an alarm system that can be easily heard and | YES NO NA | |
| | seen to warn employees in the building of an | | |
| | emergency situation? | | |
| q) | Is there sufficient bottled air, SCBA and supplied air | YES NO NA | |
| | respirators to support the foreseeable number of | | |
| | employees that can not immediately evacuate the | | |
| | building? | | |
| r) | Are all sewers connected to the building properly | ∐YES ∐NO ∐NA | |
| | sealed to prevent ingress of flammable or toxic | | |
| | vapors? | | |
| s) | Are only the employees that are essential to the | ☐YES ☐NO ☐NA | |
| | operation of the process housed in the building? | | |
| t) | Does the ventilation system have an emergency power | ☐YES ☐NO ☐NA | |
| | supply? | | |

| Hun | nan Fact | ors | | | | | | |
|-----|-----------|-------------------------------|---|---|------|-------|----|--|
| 1. | control s | system condit not defin | evaluate the hazards, consequences, frequency, as and management systems needed to protect ions that could cause human errors ^{1, 30, 33, Error!} that could lead to a runaway reaction, | | YES | □NO [| NA | |
| | | | nmental conditions: | Г | YES | NO | NA | |
| | | i) | Excessive background noise? | ┢ | YES | NO | NA | |
| | | i) | Excessive background vibration? | ┢ | YES | NO | NA | |
| | | iii) | Insufficient lighting? | ┢ | YES | NO | NA | |
| | | v) | Excessive heat or cold? | ┢ | YES | NO | NA | |
| | | v) | Noxious smells? | ┢ | YES | NO | NA | |
| | | | or/Process interface: | F | YES | NO | NA | |
| | |) | Identification of displays, and controls? | ┢ | YES | NO | NA | |
| | | i) | Layout of the instruments and controls? | F | YES | NO | NA | |
| | | iii) | Adequacy of the number of display screens? | | YES | NO | NA | |
| | | (v) | First-out alarm indication? | | YES | NO | NA | |
| | | v) | Nuisance alarms management system? | | YES | NO | NA | |
| | | vi) | Good accessibility of controls, valves and other equipment that needs to be operated periodically? | | YES | □NO [| NA | |
| | 7 | vii) | Good equipment layout? | | YES | NO | NA | |
| | | viii) | Adequate tools provided to perform the required tasks? | | YES | NO | NA | |
| | i | ix) | Good housekeeping? | | YES | □NO [| NA | |
| | Σ | x) | Loss of attention due to extended, uneventful vigilance? | |]YES | □NO [| NA | |
| | y | xi) | Provision of non-compatible fittings on hoses that transfer different materials? | |]YES | □NO [| NA | |
| | > | xii) | Conventional color schemes (i.e. red should mean stop, or off; green should mean start or on)? | |]YES | □NO [| NA | |
| | Σ | xiii) | Guarded critical controls that could be activated or deactivated unintentionally? | | YES | □NO [| NA | |
| | c) I | Physic | al activities: | | YES | NO | NA | |
| | i | i) | Excessive strength/endurance requirements? | | YES | NO | NA | |
| | i | ii) | Excessive repetition? | | YES | NO | NA | |
| | i | iii) | Chairs, stools, etc. that cause fatigue or poor posture? | | YES | NO | NA | |
| | i | iv) | Excessive work hours or overtime? | | YES | □NO [| NA | |
| | | - | (a) Are work hours limited to 12 hours per day? | | YES | NO | NA | |

| Human Fa | ctors | | |
|----------|-------|---|--------------|
| | | | |
| | | (b) Are work periods limited to no more than 7 consecutive work days? | ☐YES ☐NO ☐NA |
| d) | Manag | gement practices: | TYES TNO TNA |
| <u> </u> | i) | Procedures to ensure that management provides comprehensive, clear written instructions (i.e. supervisor's logbook entries)? | YES NO NA |
| | ii) | Procedures to ensure that operators provide comprehensive, clear written accounts of the events of the work period (i.e. operator's logbook entries)? | □YES □NO □NA |
| | iii) | Procedures to ensure that operators provide a comprehensive verbal accounting of the status of the process and any maintenance activities to the relieving operator? | □YES □NO □NA |
| | iv) | Procedures to ensure that shift foremen provide a comprehensive verbal accounting of the status of the process and any maintenance activities to the relieving shift foreman? | □YES □NO □NA |
| | v) | Clear written guidance prohibiting employees to take unnecessary risks, such as placing production requirements above safety requirements? | □YES □NO □NA |
| | | (a) Actions by management that demonstrate their commitment to this policy, such as shutting down the process under hazardous conditions and delaying startup until all maintenance and check-outs have been completed? | □YES □NO □NA |
| | vi) | Procedures to ensure that procedures and safe work practices are always followed? | □YES □NO □NA |

| Evalu | | of the range of possible safety and health af | fects due to failures | of |
|-------|--------|--|-----------------------|----|
| | | | | _ |
| 3. | Has a | qualitative evaluation (some employers call this a risk ment) ^{1, 3, 5, 7, 17, 26, 27, 30, 34, 94} been performed to evaluate | YES NO NA | |
| | the po | tential safety and health effects of all runaway reaction | | |
| | scenar | ios that could result, due to failures of controls, in an | | |
| | explos | sion, fire, or toxic release that has the potential to cause | | |
| | death, | or serious injury? | | |
| 4. | Was a | risk matrix 17, 27, 34, 94 developed that defines the risk for | YES NO NA | |
| | every | pair of frequency (likelihood) and consequence ranges? | | |
| | Refer | to Table 17 for an example of a typical risk matrix. | | |
| | a) | Are the tolerable (acceptable) categories of risk identified? | YES NO NA | |
| | b) | Based on the potential consequences for each runaway reaction, was the required frequency of that | YES NO NA | |
| | | occurrence identified to achieve a tolerable category of | | |
| | | risk? Refer to Table 17 for an example of a typical | | |
| | | risk matrix | | |

Operating Procedures

| Operating Limits | | | | |
|------------------|--|------------------|--|--|
| | | | | |
| 1. | Are there operating procedures ^{1, 3, 28, 29, 33, 37, 38, 45, 61, 62} for all | YES NO NA | | |
| , | phases of operation for each HHRC process? | | | |
| 2. | Do the operating procedures define the safe operating | │ □YES □NO □NA │ | | |
| | envelope (limits) for applicable process variables for each | | | |
| | piece of equipment, such as | | | |
| | a) Temperature? | YES NO NA | | |
| | b) Pressure? | YES NO NA | | |
| | c) Level? | YES NO NA | | |
| | d) Flow rates? | YES NO NA | | |
| | e) Quantities? | YES NO NA | | |
| | f) Concentrations of process chemicals? | YES NO NA | | |
| | g) Concentrations of impurities? | YES NO NA | | |
| | h) Concentrations of catalysts | YES NO NA | | |
| | i) Concentrations of inhibitors? | YES NO NA | | |
| 3. | Do the operating procedures address the normal operating | YES NO NA | | |
| | range (i.e. the values in between the hi and lo alarm set | | | |
| | points) for each piece of equipment for applicable process | | | |
| | variables such as: | | | |
| | a) Temperature? | YES NO NA | | |
| | b) Pressure? | YES NO NA | | |
| | c) Level? | YES NO NA | | |
| | d) Flow rates? | YES NO NA | | |
| | e) Quantities? | ☐YES ☐NO ☐NA | | |
| | f) Concentrations of process chemicals? | YES NO NA | | |
| | g) Concentrations of impurities? | YES NO NA | | |
| | h) Concentrations of catalysts | YES NO NA | | |
| | i) Concentrations of inhibitors? | YES NO NA | | |
| 4. | Do the operating procedures address the value of applicable | ☐YES ☐NO ☐NA | | |
| | process variables for each piece of equipment where operator | | | |
| | actions are required (i.e. the high and low alarm set points) | | | |
| | for process variables, such as: | | | |
| | a) Temperature? | YES NO NA | | |
| | b) Pressure? | YES NO NA | | |
| | c) Level? | YES NO NA | | |
| | d) Flow rates? | YES NO NA | | |
| | e) Quantities? | YES NO NA | | |
| | f) Concentrations of process chemicals? | ☐YES ☐NO ☐NA | | |
| | g) Concentrations of impurities? | │ □YES □NO □NA │ | | |

| Эре | erating | Limits | | | | |
|------------|-----------|--|-------------|---|---------|--|
| | 1. | | | C | | |
| | <u>h)</u> | Concentrations of catalysts | YE | | NO NA | |
| | <u>i)</u> | Concentrations of inhibitors? | YE | | NO NA | |
| 5. | | he operating procedures address the value of applicable | ☐YE | S | □NO □NA | |
| | | ess variables for each piece of equipment where actions | | | | |
| | | utomatically taken by the control system (safety system) | | | | |
| | | hi-hi and lo-lo alarm set points that activate a safety | | | | |
| | | umented function (interlock), such as: | | C | | |
| | <u>a)</u> | Temperature? Pressure? | YE | | NO NA | |
| | <u>b)</u> | | YE | | | |
| | <u>c)</u> | Level? | YE | | NO NA | |
| | <u>d)</u> | Flow rates? | YE | | NO NA | |
| | <u>e)</u> | Quantities? | YE | | NO NA | |
| | <u>f)</u> | Concentrations of process chemicals? | YE VE | | NO NA | |
| | <u>g)</u> | Concentrations of impurities? | YE | | NO NA | |
| | <u>h)</u> | Concentrations of catalysts | YE | | NO NA | |
| | <u>i)</u> | Concentrations of inhibitors? | YE | | NO NA | |
| | | he operating procedures address the consequences of | ☐YE | S | □NO □NA | |
| | | ation for each piece of equipment for applicable process | | | | |
| | varia | ibles, such as: | | | | |
| | a) | Temperature? | ☐YE | S | NO NA | |
| | b) | Pressure? | YE | S | NO NA | |
| | c) | Level? | YE | S | NO NA | |
| | d) | Flow rates? | YE | S | NO NA | |
| | e) | Quantities? | YE | S | NO NA | |
| | f) | Concentrations of process chemicals? | YE | S | NO NA | |
| | g) | Concentrations of impurities? | YE | S | NO NA | |
| | h) | Concentrations of catalysts | YE | S | NO NA | |
| | i) | Concentrations of inhibitors? | YE | S | NO NA | |
| <u>'</u> . | Do t | he operating procedures address the steps needed to be | YE | | NO NA | |
| | | n to avoid and to correct an applicable process variable | | , | | |
| | | ation for each piece of equipment, such as: | | | | |
| | a) | Temperature? | Т ҮЕ | S | □NO □NA | |
| | b) | Pressure? | ☐YE | S | □NO □NA | |
| | c) | Level? | ☐YE | S | NO NA | |
| | d) | Flow rates? | YE | S | NO NA | |
| | e) | Quantities? | YE | S | NO NA | |
| | f) | Concentrations of process chemicals? | YE | S | NO NA | |
| | g) | Concentrations of impurities? | YE | | NO NA | |
| | h) | Concentrations of catalysts | YE | | NO NA | |
| | i) | Concentrations of inhibitors? | YE | | NO NA | |

| Properties and hazards presented by the chemicals in the process | | | | | |
|--|-----------|---|-----------------|--|--|
| 1. | and ha | e operating procedures adequately discuss the properties tzards presented by the reactive chemicals in the as, such as: | YES NO NA | | |
| | a) | Temperatures that could lead to a runaway reaction? | YES NO NA | | |
| | b) | Concentrations of reactants that could lead to a | YES NO NA | | |
| | 0) | runaway reaction? | | | |
| | c) | Concentrations of impurities that could lead to a | YES NO NA | | |
| | •) | runaway reaction? | | | |
| | d) | The relationship between temperature and time to | YES NO NA | | |
| | / | runaway reaction? | | | |
| | e) | The interrelationship between temperatures, | YES NO NA | | |
| | , | concentration of reactants and concentration of | | | |
| | | impurities that could lead to a runaway reaction? | | | |
| | f) | Inhibitor concentrations and conditions necessary to | YES NO NA | | |
| | | maintain effective inhibitor levels? | | | |
| 2. | | e operating procedures adequately discuss the | YES NO NA | | |
| | precau | tions necessary to prevent exposure, such as: | | | |
| | a) | Engineering controls identified and listed as | YES NO NA | | |
| | | safeguards in the PHA? | | | |
| | b) | Administrative controls identified and listed as | ☐YES ☐NO ☐NA | | |
| | | safeguards in the PHA? | | | |
| | <u>c)</u> | PPE identified and listed as safeguards in the PHA? | YES NO NA | | |
| 3. | | e operating procedures include quality control | YES NO NA | | |
| | | lures for raw materials, catalysts, solvents, and other | | | |
| | | s chemicals, such as: | | | |
| | a) | Ensuring that they meet specifications when received at the facility? | L YES L NO L NA | | |
| | b) | Ensuring that they are stored in a manner that ensures | YES NO NA | | |
| | | that the material continues to meet specifications (i.e. | | | |
| | | temperature control, moisture control, inhibitor | | | |
| | | concentration, inerting, etc.) until it is ready to be | | | |
| | | used in the process? | | | |
| | c) | Ensuring that the materials are stored in designated | YES NO NA | | |
| | | locations so as to not create a hazard (i.e. limitations | | | |
| | | on quantities in containers, limitations on spacing or | | | |
| | 1) | density of containers, remote locations, etc.)? | TATES TO THE | | |
| | d) | Ensuring that these materials are only transferred into equipment that has been cleaned and prepared | LYES LNO LNA | | |
| | | appropriately? | | | |

| | Safety systems and their functions | | | | |
|----|------------------------------------|---|--------|---------|--|
| | | · · | | | |
| 1. | | e operating procedures adequately discuss the safety as that are used to protect against runaway reactions, s: | YES [| □NO □NA | |
| | a) | Pressure relief devices? | YES [| NO NA | |
| | b) | Automated vent systems? | YES | NO NA | |
| | c) | Automated quench systems? | YES [| NO NA | |
| | d) | Automated dump systems? | YES [| NO NA | |
| | e) | Automated systems that inject a reaction inhibitor or poison? | YES [| □NO □NA | |
| | f) | Inerting systems? | YES [| NO NA | |
| | g) | Recipe –based supervision (monitoring of material balance)? | YES [| □NO □NA | |
| | h) | Monitoring of heat balance? | YES [| NO NA | |
| | i) | Building or room temperature control systems? | YES [| NO NA | |
| | j) | Building or room humidity control systems? | YES [| NO NA | |
| | k) | Air and moisture exclusion systems? | YES | NO NA | |
| 2. | system | e operating procedures adequately discuss the safety ns that are used to mitigate the effects of a runaway on, such as: | YES [| □NO □NA | |
| | a) | Bunkers, blast walls and barricades? | YES [| NO NA | |
| | b) | Secondary containment? | YES [| NO NA | |
| | c) | Separation distances? | YES [| NO NA | |
| | d) | Excess flow valves? | YES [| NO NA | |
| | e) | Remotely actuated emergency block valves? | YES [| NO NA | |
| | f) | Fire-resistant/explosion/resistant construction? | YES [| NO NA | |
| | g) | Alarms to detect the heat and/or vapors generated as a | YES [| NO NA | |
| | 1) | result of the loss of containment? | Dvec 5 | | |
| | <u>h)</u> | Water curtains/deluge systems? | YES [| NO NA | |
| | i) | Automatic sprinkler systems? | YES [| □NO □NA | |

Training

| Initia | l Training | |
|--------|---|--------------|
| | | |
| 1. | Is there documentation to show that the operators have been trained ^{1, 3, 28, 29, 33, 37, 38, 45, 61, 62, 63, 114} and that they understood that training? | □YES □NO □NA |
| 2. | Is there documentation to show that employees involved in the operation of a HHRC process have been trained in, and understand the training received, in the operating limits of the process, such as: | □YES □NO □NA |
| | a) Does the training address the safe operating envelope (limits) for applicable process variables for each piece of equipment, such as | YES NO NA |
| | i) Temperature? | YES NO NA |
| | ii) Pressure? | YES NO NA |
| | iii) Level? | ☐YES ☐NO ☐NA |
| | iv) Flow rates? | YES NO NA |
| | v) Quantities? | YES NO NA |
| | vi) Concentrations of process chemicals? | YES NO NA |
| | vii) Concentrations of impurities? | YES NO NA |
| | viii) Concentrations of catalysts | YES NO NA |
| | ix) Concentrations of inhibitors? | YES NO NA |
| | b) Does the training address the normal operating range (i.e. the values in between the hi and lo alarm set points) for each piece of equipment for applicable process variables such as: | YES NO NA |
| | i) Temperature? | YES NO NA |
| | ii) Pressure? | YES NO NA |
| | iii) Level? | YES NO NA |
| | iv) Flow rates? | YES NO NA |
| | v) Quantities? | YES NO NA |
| | vi) Concentrations of process chemicals? | ☐YES ☐NO ☐NA |
| | vii) Concentrations of impurities? | □YES □NO □NA |
| | viii) Concentrations of catalysts | YES NO NA |
| | ix) Concentrations of inhibitors? | YES NO NA |
| | c) Does the training address the value of applicable process variables for each piece of equipment where operator actions are required (i.e. the hi and lo alarm | YES NO NA |
| | set points) for process variables, such as: | |
| | i) Temperature? | ☐YES ☐NO ☐NA |

| Initial Training | | |
|------------------|--|---------------------|
| | | |
| ii) | Pressure? | YES NO NA |
| iii) | Level? | YES NO NA |
| iv) | Flow rates? | YES NO NA |
| v) | Quantities? | YES NO NA |
| vi) | Concentrations of process chemicals? | YES NO NA |
| vii) | Concentrations of impurities? | YES NO NA |
| viii) | Concentrations of catalysts | YES NO NA |
| ix) | Concentrations of inhibitors? | YES NO NA |
| d) Does | s the training address the value of applicable | YES NO NA |
| | ess variables for each piece of equipment where | |
| | ns are automatically taken by the control system | |
| | ty system) (i.e. hi-hi and lo-lo alarm set points | |
| | activate a safety instrumented function | |
| | rlock), such as: | |
| i) | Temperature? | YES NO NA |
| | Pressure? | YES NO NA YES NO NA |
| iv) | Level? Flow rates? | YES NO NA YES NO NA |
| v) | Quantities? | YES NO NA |
| vi) | Concentrations of process chemicals? | YES NO NA |
| vii) | Concentrations of process enemears: Concentrations of impurities? | YES NO NA |
| viii) | Concentrations of catalysts | YES NO NA |
| ix) | Concentrations of inhibitors? | YES NO NA |
| , | s the training address the consequences of | YES NO NA |
| _ | ation for each piece of equipment for applicable | |
| | ess variables, such as: | |
| i) | Temperature? | □YES □NO □NA |
| ii) | Pressure? | ☐YES ☐NO ☐NA |
| iii) | Level? | YES NO NA |
| iv) | Flow rates? | YES NO NA |
| v) | Quantities? | ☐YES ☐NO ☐NA |
| vi) | Concentrations of process chemicals? | ☐YES ☐NO ☐NA |
| vii) | Concentrations of impurities? | ☐YES ☐NO ☐NA |
| viii) | Concentrations of catalysts | ☐YES ☐NO ☐NA |
| ix) | Concentrations of inhibitors? | □YES □NO □NA |

| Initial Trainir | Initial Training | | | | | |
|-----------------------|------------------|---|--------------|--|--|--|
| | -3 | | | | | |
| to | o avoi | he training address the steps needed to be taken d and to correct an applicable process variable on for each piece of equipment, such as: | YES NO NA | | | |
| i | .) | Temperature? | ☐YES ☐NO ☐NA | | | |
| i | i) | Pressure? | YES NO NA | | | |
| i | ii) | Level? | YES NO NA | | | |
| i | v) | Flow rates? | YES NO NA | | | |
| V | v) | Quantities? | YES NO NA | | | |
| V | vi) | Concentrations of process chemicals? | YES NO NA | | | |
| V | vii) | Concentrations of impurities? | YES NO NA | | | |
| V | viii) | Concentrations of catalysts | YES NO NA | | | |
| i | x) | Concentrations of inhibitors? | YES NO NA | | | |
| the opera understa | ation on the | nentation to show that employees involved in of a HHRC process have been trained in, and e training received, in the safety and health a for the process, such as | □YES □NO □NA | | | |
| a | and ha | he training adequately address the properties zards presented by the reactive chemicals in the s, such as: | □YES □NO □NA | | | |
| ij |) | Temperatures that could lead to a runaway reaction? | ☐YES ☐NO ☐NA | | | |
| 1 | i) | Concentrations of reactants that could lead to a runaway reaction? | YES NO NA | | | |
| 1 | ii) | Concentrations of impurities that could lead to a runaway reaction? | YES NO NA | | | |
| i | v) | The relationship between temperature and time to runaway reaction? | ☐YES ☐NO ☐NA | | | |
| V | v) | The interrelationship between temperatures, concentration of reactants and concentration of impurities that could lead to a runaway reaction? | □YES □NO □NA | | | |

| Initial Training | | | | |
|------------------|------------------------------|--|--------------|--|
| | | | | |
| | vi) | Inhibitor concentrations and conditions necessary to maintain effective inhibitor levels? | YES NO NA | |
| b | | the training adequately address the precautions sary to prevent exposure, such as: | ☐YES ☐NO ☐NA | |
| | i) | Engineering controls identified and listed as safeguards in the PHA? | ☐YES ☐NO ☐NA | |
| | ii) | Administrative controls identified and listed as safeguards in the PHA? | ☐YES ☐NO ☐NA | |
| | iii) | PPE identified and listed as safeguards in the PHA? | ☐YES ☐NO ☐NA | |
| c) | proce | the training adequately address quality control dures for raw materials, catalysts, solvents, and process chemicals, such as: | □YES □NO □NA | |
| | i) | Ensuring that they meet specifications when received at the facility? | YES NO NA | |
| | ii) | Ensuring that they are stored in a manner that ensures that the material continues to meet specifications (i.e. temperature control, moisture control, inhibitor concentration, inerting, etc.) until it is ready to be used in the process? | □YES □NO □NA | |
| | iii) | Ensuring that the materials are stored in designated locations so as to not create a hazard (i.e. limitations on quantities in containers, limitations on spacing or density of containers, remote locations, etc.)? | □YES □NO □NA | |
| | iv) | Ensuring that these materials are only transferred into equipment that has been cleaned and prepared appropriately? | □YES □NO □NA | |
| th u | ne operation nderstand th | mentation to show that employees involved in of a HHRC process have been trained in, and ne training received, in the engineering controls rocess, such as | □YES □NO □NA | |

| Initial 1 | Initial Training | | | | | |
|-----------|------------------------------|---|--------------|--|--|--|
| | | | | | | |
| a | system | he training adequately address the safety as that are used to protect against runaway ons, such as: | □YES □NO □NA | | | |
| | i) | Pressure relief devices? | ☐YES ☐NO ☐NA | | | |
| | ii) | Automated vent systems? | ☐YES ☐NO ☐NA | | | |
| | iii) | Automated quench systems? | ☐YES ☐NO ☐NA | | | |
| | iv) | Automated dump systems? | □YES □NO □NA | | | |
| | v) | Automated systems that inject a reaction inhibitor or poison? | ☐YES ☐NO ☐NA | | | |
| | vi) | Inerting systems? | ☐YES ☐NO ☐NA | | | |
| | vii) | Recipe –based supervision? | □YES □NO □NA | | | |
| | viii) | Monitoring of heat balance? | □YES □NO □NA | | | |
| | ix) | Building or room temperature control systems? | ☐YES ☐NO ☐NA | | | |
| | x) | Building or room humidity control systems? | ☐YES ☐NO ☐NA | | | |
| | xi) | Air and moisture exclusion systems? | ☐YES ☐NO ☐NA | | | |
| b | system | he training adequately address the safety as that are used to mitigate the effects of a ay reaction, such as: | YES NO NA | | | |
| | i) | Bunkers, blast walls and barricades? | ☐YES ☐NO ☐NA | | | |
| | ii) | Secondary containment? | ☐YES ☐NO ☐NA | | | |
| | iii) | Separation distances? | YES NO NA | | | |
| | iv) | Excess flow valves? | YES NO NA | | | |
| | v) | Remotely actuated emergency block valves? | ☐YES ☐NO ☐NA | | | |
| | vi) | Fire-resistant/explosion/resistant construction? | ☐YES ☐NO ☐NA | | | |
| | vii) | Alarms to detect the heat and/or vapors generated as a result of the loss of containment? | YES NO NA | | | |
| | viii) | Water curtains/deluge systems? | ☐YES ☐NO ☐NA | | | |
| | ix) | Automatic sprinkler systems? | ☐YES ☐NO ☐NA | | | |
| 5. E | Ooes the docu equirements | imentation show that the initial training met the of ANSI/ASSE Z490.1-2001 ¹¹⁴ ? | YES NO NA | | | |

| Refr | esher | trainir | ng | | | | |
|------|---|--|--|--------------|--|--|--|
| | | | | | | | |
| 1. | Is there documentation to show that the employees involved in the operation of a HHRC process have received refresher training at least every three years? Is there documentation to show that the employees involved TYES NO NA | | | | | | |
| 2. | Is there documentation to show that the employees involved in the operation of a HHRC process have assisted in establishing how frequently the refresher training should be given? | | | | | | |
| 3. | the op | eration ng in, ar | mentation to show that employees involved in of a HHRC process have received refresher and understand the training received, in the its of the process, such as: | □YES □NO □NA | | | |
| | a) | envel | the refresher training address the safe operating ope (limits) for applicable process variables for piece of equipment, such as | □YES □NO □NA | | | |
| | | i) | Temperature? | ☐YES ☐NO ☐NA | | | |
| | | ii) | Pressure? | YES NO NA | | | |
| | | iii) | Level? | ☐YES ☐NO ☐NA | | | |
| | | iv) | Flow rates? | ☐YES ☐NO ☐NA | | | |
| | | v) | Quantities? | YES NO NA | | | |
| | | vi) | Concentrations of process chemicals? | YES NO NA | | | |
| | | vii) | Concentrations of impurities? | YES NO NA | | | |
| | | viii) | Concentrations of catalysts | ☐YES ☐NO ☐NA | | | |
| | | ix) | Concentrations of inhibitors? | ☐YES ☐NO ☐NA | | | |
| | b) | operation of the local contract of the local | the refresher training address the normal ting range (i.e. the values in between the hi and rm set points) for each piece of equipment for eable process variables such as: | □YES □NO □NA | | | |
| | | i) | Temperature? | ☐YES ☐NO ☐NA | | | |
| | | ii) | Pressure? | ☐YES ☐NO ☐NA | | | |
| | | iii) | Level? | ☐YES ☐NO ☐NA | | | |
| | | iv) | Flow rates? | □YES □NO □NA | | | |

| | | | | _ |
|-----------|---|---|--------------|---|
| Refresher | trainin | g | | |
| | | | | |
| | v) | Quantities? | YES NO NA | |
| | vi) | Concentrations of process chemicals? | □YES □NO □NA | |
| | vii) | Concentrations of impurities? | YES NO NA | |
| | viii) | Concentrations of catalysts | YES NO NA | |
| | ix) | Concentrations of inhibitors? | YES NO NA | |
| c) | applica equipn | he refresher training address the value of able process variables for each piece of nent where operator actions are required (i.e. the lo alarm set points) for process variables, such | ☐YES ☐NO ☐NA | |
| | i) | Temperature? | ☐YES ☐NO ☐NA | |
| | ii) | Pressure? | YES NO NA | |
| | iii) | Level? | YES NO NA | |
| | iv) | Flow rates? | ☐YES ☐NO ☐NA | |
| | v) | Quantities? | ☐YES ☐NO ☐NA | |
| | vi) | Concentrations of process chemicals? | □YES □NO □NA | |
| | vii) | Concentrations of impurities? | □YES □NO □NA | |
| | viii) | Concentrations of catalysts | ☐YES ☐NO ☐NA | |
| | ix) | Concentrations of inhibitors? | ☐YES ☐NO ☐NA | |
| d) | proces actions (safety that ac | he training address the value of applicable s variables for each piece of equipment where s are automatically taken by the control system system) (i.e. hi-hi and lo-lo alarm set points tivate a safety instrumented function ock), such as: | YES NO NA | |
| | i) | Temperature? | ☐YES ☐NO ☐NA | |
| | ii) | Pressure? | ☐YES ☐NO ☐NA | |
| | iii) | Level? | ☐YES ☐NO ☐NA | |
| | iv) | Flow rates? | ☐YES ☐NO ☐NA | |
| | v) | Quantities? | ☐YES ☐NO ☐NA | |
| | vi) | Concentrations of process chemicals? | YES NO NA | |
| | vii) | Concentrations of impurities? | ☐YES ☐NO ☐NA | |

| Refresher training | | | | | | |
|--------------------|------------------------|--|--------------|--|--|--|
| | | | | | | |
| | viii) | Concentrations of catalysts | □YES □NO □NA | | | |
| | ix) | Concentrations of inhibitors? | □YES □NO □NA | | | |
| e) | deviat | the training address the consequences of tion for each piece of equipment for applicable ss variables, such as: | YES NO NA | | | |
| | i) | Temperature? | □YES □NO □NA | | | |
| | ii) | Pressure? | □YES □NO □NA | | | |
| | iii) | Level? | □YES □NO □NA | | | |
| | iv) | Flow rates? | □YES □NO □NA | | | |
| | v) | Quantities? | ☐YES ☐NO ☐NA | | | |
| | vi) | Concentrations of process chemicals? | YES NO NA | | | |
| | vii) | Concentrations of impurities? | YES NO NA | | | |
| | viii) | Concentrations of catalysts | YES NO NA | | | |
| | ix) | Concentrations of inhibitors? | YES NO NA | | | |
| f) | to avo | the training address the steps needed to be taken and to correct an applicable process variable tion for each piece of equipment, such as: | YES NO NA | | | |
| | i) | Temperature? | ☐YES ☐NO ☐NA | | | |
| | ii) | Pressure? | ☐YES ☐NO ☐NA | | | |
| | iii) | Level? | ☐YES ☐NO ☐NA | | | |
| | iv) | Flow rates? | YES NO NA | | | |
| | v) | Quantities? | YES NO NA | | | |
| | vi) | Concentrations of process chemicals? | YES NO NA | | | |
| | vii) | Concentrations of impurities? | YES NO NA | | | |
| | viii) | Concentrations of catalysts | YES NO NA | | | |
| | ix) | Concentrations of inhibitors? | YES NO NA | | | |
| the o | peration ing in, ar | mentation to show that employees involved in of a HHRC process have received refresher and understand the training received, in the safety nsiderations for the process, such as | □YES □NO □NA | | | |

| Refresher | trainin | ıg | |
|-----------|---------|---|--------------|
| | | | |
| a) | proper | the refresher training adequately address the rties and hazards presented by the reactive cals in the process, such as: | □YES □NO □NA |
| | i) | Temperatures that could lead to a runaway reaction? | □YES □NO □NA |
| | ii) | Concentrations of reactants that could lead to a runaway reaction? | □YES □NO □NA |
| | iii) | Concentrations of impurities that could lead to a runaway reaction? | □YES □NO □NA |
| | iv) | The relationship between temperature and time to runaway reaction? | □YES □NO □NA |
| | v) | The interrelationship between temperatures, concentration of reactants and concentration of impurities that could lead to a runaway reaction? | □YES □NO □NA |
| | vi) | Inhibitor concentrations and conditions necessary to maintain effective inhibitor levels? | □YES □NO □NA |
| b) | | the refresher training adequately address the ations necessary to prevent exposure, such as: | □YES □NO □NA |
| | i) | Engineering controls identified and listed as safeguards in the PHA? | □YES □NO □NA |
| | ii) | Administrative controls identified and listed as safeguards in the PHA? | YES NO NA |
| | iii) | PPE identified and listed as safeguards in the PHA? | YES NO NA |
| | iv) | Does the training adequately address quality control procedures for raw materials, catalysts, solvents, and other process chemicals, such as: | □YES □NO □NA |
| | | (a) Ensuring that they meet specifications when received at the facility? | ☐YES ☐NO ☐NA |

| Refresher trainin | g | | | |
|-------------------------------|---------|--|--------------|--|
| | (b) | Ensuring that they are stored in a manner that ensures that the material continues to meet specifications (i.e. temperature control, moisture control, inhibitor concentration, inerting, etc.) until it is ready to be used in the process? | YES NO NA | |
| | (c) | Ensuring that the materials are stored in designated locations so as to not create a hazard (i.e. limitations on quantities in containers, limitations on spacing or density of containers, remote locations, etc.)? | □YES □NO □NA | |
| | (d) | Ensuring that these materials are only transferred into equipment that has been cleaned and prepared appropriately? | □YES □NO □NA | |
| the operation training in, an | of a HE | on to show that employees involved in IRC process have received refresher estand the training received, in the used in the process, such as | □YES □NO □NA | |
| safety | system | esher training adequately address the s that are used to protect against tions, such as: | □YES □NO □NA | |
| i) | Pressu | re relief devices? | □YES □NO □NA | |
| ii) | Auton | nated vent systems? | □YES □NO □NA | |
| iii) | Auton | nated quench systems? | ☐YES ☐NO ☐NA | |
| iv) | Auton | nated dump systems? | ☐YES ☐NO ☐NA | |
| v) | | nated systems that inject a reaction for or poison? | ☐YES ☐NO ☐NA | |
| vi) | Inertin | ng systems? | ☐YES ☐NO ☐NA | |
| vii) | Recipo | e –based supervision? | ☐YES ☐NO ☐NA | |
| viii) | Monit | oring of heat balance? | ☐YES ☐NO ☐NA | |
| ix) | Buildi | ng or room temperature control systems? | □YES □NO □NA | |
| x) | Buildi | ng or room humidity control systems? | □YES □NO □NA | |

| Refre | esher t | rainin | a | | |
|-------|--------------|-------------------|---|--------------|--|
| | | | | | |
| | | xi) | Air and moisture exclusion systems? | ☐YES ☐NO ☐NA | |
| | b) | safety | he refresher training adequately address the systems that are used to mitigate the effects of a ay reaction, such as: | ☐YES ☐NO ☐NA | |
| | | i) | Bunkers, blast walls and barricades? | YES NO NA | |
| | | ii) | Secondary containment? | ☐YES ☐NO ☐NA | |
| | | iii) | Separation distances? | YES NO NA | |
| | | iv) | Excess flow valves? | ☐YES ☐NO ☐NA | |
| | | v) | Remotely actuated emergency block valves? | ☐YES ☐NO ☐NA | |
| | | vi) | Fire-resistant/explosion/resistant construction? | ☐YES ☐NO ☐NA | |
| | | vii) | Alarms to detect the heat and/or vapors generated as a result of the loss of containment? | YES NO NA | |
| | | viii) | Water curtains/deluge systems? | ☐YES ☐NO ☐NA | |
| | | ix) | Automatic sprinkler systems? | ☐YES ☐NO ☐NA | |
| 6. | Does the req | he docu uireme | imentation show that the refresher training met nts of ANSI/ASSE Z490.1-2001 ¹¹⁴ ? | YES NO NA | |

Contractors

| | | | | | _ |
|------|--|---|---|--------------|---|
| Appl | icatior | า | | | |
| 1. | require | ements | nentation to show that the employer has met the of this paragraph for contractors ⁴⁵ that perform an impact on process safety, such as: | YES NO NA | |
| | a) | Operat | tion of the process? | □YES □NO □NA | |
| | b) | unload | ming packaging, blending, loading, or ling of the raw materials, intermediates, ets or wastes from the process? | ☐YES ☐NO ☐NA | |
| | c) | Toll m | anufacturing? | □YES □NO □NA | |
| | d) | Mainte | enance or construction on or near the process? | □YES □NO □NA | |
| | | | | | _ |
| Emp | loyer r | espor | nsibilities | | |
| | | | | | |
| 1. | notifie packag materi manuf proces | ed contraging, blocals or in a care | nentation to show that the employer ⁴⁵ has actors that operate the process, perform ending, loading or unloading of the raw atermediates, products or wastes, toll and maintenance or construction on or near the potential fire, explosion, or toxic chemical as of the process by providing such information | YES NO NA | |
| | a) | Inform | nation about the chemicals in the process? | □YES □NO □NA | |
| | b) | | nation about the technology of the process? not apply to maintenance and construction) | ☐YES ☐NO ☐NA | |
| | c) | | nation about the equipment in the process? (May ply to maintenance and construction) | YES NO NA | |
| | d) | equipn | nation about the design and design basis of the nent and the applicable RAGAGEP? (May not to maintenance and construction) | YES NO NA | |
| | e) | assessi | ost recent process hazards analysis and risk ment? (May not apply to maintenance and uction) | YES NO NA | |
| | | i) | The status of all recommendations made as a result of the most recent PHA? | ☐YES ☐NO ☐NA | |

| | ii) Are the contractor's responsibilities for participation in, or conducting a PHA adequately defined? | ☐YES ☐NO ☐NA |
|----|---|--------------|
| f) | Operating procedures, or the information necessary to prepare operating procedures? (May not apply to maintenance and construction) | ☐YES ☐NO ☐NA |
| | i) Are the responsibilities of the contractor for operating procedures adequately defined? | □YES □NO □NA |
| | ii) Are the contractor's responsibilities for safe work practices, such as LOTO, confined space entry and line breaking and equipment opening adequately defined? | □YES □NO □NA |
| g) | The information necessary to provide training to their employees? (May not apply to maintenance and construction) | □YES □NO □NA |
| | i) Are the contractor's responsibilities for training adequately defined? | YES NO NA |
| h) | The information necessary to participate in or perform pre-startup safety reviews? (May not apply to maintenance and construction) | YES NO NA |
| | i) Are the contractor's responsibilities for pre- startup safety reviews adequately defined? | □YES □NO □NA |
| i) | The information necessary to participate in the mechanical integrity program? | □YES □NO □NA |
| | i) Are the contractor's responsibilities for the mechanical integrity program adequately defined? | □YES □NO □NA |
| j) | The employer's hot work permit program or the information necessary to develop a hot work permit program? | □YES □NO □NA |
| | i) Are the contractor's responsibilities for the hot work permit program adequately defined? | □YES □NO □NA |
| k) | The employer's management of change procedures, or the information needed to develop and use a management of change program? | □YES □NO □NA |
| | i) Are the contractor's responsibilities for management of change adequately defined? | □YES □NO □NA |
| 1) | Incident investigation reports, including near misses? | □YES □NO □NA |

| | | i) | Are the contractor's responsibilities for incident investigation adequately defined? | YES NO NA | |
|----|--------|-----------|---|--------------|---|
| | m) | The en | nergency response plan? | □YES □NO □NA | |
| | | i) | Are the contractor's responsibilities for emergency response adequately defined? | □YES □NO □NA | |
| | n) | | nost recent audit that evaluated the compliance his recommended practice | YES NO NA | |
| | | i) | The status of all recommendations made as a result of the previous audit? | YES NO NA | |
| | | ii) | The contractor's responsibilities for participating in, or performing audits? | YES NO NA | |
| | o) | | ontractor's responsibility for reporting to the yer any hazards that had not previously been fied? | YES NO NA | |
| 2. | evacua | ation of | loyer have procedures in place that require fall non-essential personnel from the area of the g startup, shutdown and periods of unstable | □YES □NO □NA | |
| | a) | | ese procedures include sounding of an ation alarm? | YES NO NA | |
| 3. | analys | sis be pe | loyer have procedures that require that a siting erformed prior to contractors placing temporary or near the process area? Does it include: | □YES □NO □NA | |
| | a) | Office | trailers? | YES NO NA | |
| | b) | Work | trailers? | YES NO NA | |
| | c) | Tool 7 | Frailers? | YES NO NA | |
| | d) | Mater | ials storage trailers? | YES NO NA | |
| | e) | Portab | ole toilets? | YES NO NA | |
| | f) | Lunch | areas? | YES NO NA | |
| | g) | Wash- | -up and Locker facilities? | YES NO NA | _ |

| Cont | ractor | respo | onsibilities | |
|------|--------------------------------------|---|--|--------------|
| | | | | |
| 1. | a HHR unload wastes on or i | RC procling of to the state of | nentation to show that contractors ⁴⁵ that operate ess, perform packaging, blending, loading or the raw materials or intermediates, products or anufacturers and maintenance or construction process have provided the training necessary oyees to safely perform their job, such as ning in: | □YES □NO □NA |
| | a) | Inform | nation about the chemicals in the process? | YES NO NA |
| | b) | | nation about the technology of the process? not apply to maintenance or construction) | □YES □NO □NA |
| | c) | | nation about the equipment in the process? (May ply to maintenance or construction) | ☐YES ☐NO ☐NA |
| | d) | assessi | ost recent process hazards analysis and risk ment? (May not apply to maintenance or uction) | □YES □NO □NA |
| | | i) | The status of all recommendations made as a result of the most recent PHA? | ☐YES ☐NO ☐NA |
| | | ii) | The employee's responsibilities for participation in, or conducting PHA adequately defined? | □YES □NO □NA |
| | e) | Opera | ting procedures? | □YES □NO □NA |
| | | i) | The responsibilities of the employee's for operating procedures? (May not apply to maintenance or construction) | □YES □NO □NA |
| | | ii) | The safe work practices, such as LOTO, confined space entry and line breaking and equipment opening adequately defined? | □YES □NO □NA |
| | f) | | enance or construction) | □YES □NO □NA |
| | | i) | The employee's responsibilities for pre-startup safety reviews? | □YES □NO □NA |
| | g) | The m | echanical integrity program? | □YES □NO □NA |
| | | i) | The employee's responsibilities for the mechanical integrity program? | □YES □NO □NA |
| | h) | The ho | ot work permit program? | ☐YES ☐NO ☐NA |

| | | i) | The employee's responsibilities for the hot work permit program? | ☐YES ☐NO ☐NA | |
|----|--|--|---|--------------|--|
| | i) | Manag | gement of change procedures? | ☐YES ☐NO ☐NA | |
| | | i) | The employee's responsibilities for management of change? | ☐YES ☐NO ☐NA | |
| | j) | Incide | nt investigation reports, including near misses? | ☐YES ☐NO ☐NA | |
| | | i) | The employee's responsibilities for incident investigation, including near misses? | ☐YES ☐NO ☐NA | |
| | k) | The en | mergency response plan? | ☐YES ☐NO ☐NA | |
| | | i) | The employee's responsibilities for emergency response to a condition or event caused by the process? | YES NO NA | |
| | | ii) | The employee's responsibilities for emergency notification and response for a condition caused by their work? | YES NO NA | |
| | 1) | | ost recent audit that evaluated the compliance nis recommended practice? | ☐YES ☐NO ☐NA | |
| | | i) | The status of all recommendations made as a result of the previous audit? | ☐YES ☐NO ☐NA | |
| | | ii) | The employee's responsibilities for participating in, audits? | ☐YES ☐NO ☐NA | |
| | m) | hazard | mployee's responsibility for reporting any als presented by the process that were not usly identified? | YES NO NA | |
| 2. | | es the documentation show that the contractor's employees erstood the training received? | | ☐YES ☐NO ☐NA | |
| 3. | the req | tes the documentation show that the training provided met requirements of ANSI/ASSE Z490-2001 ¹¹⁴ ? | | YES NO NA | |
| 4. | Does the audit of safe practice permits, such as: LOTO permits, line breaking permits, confined space entry permits, hot work permits, and safe to work permits, show that the contractor's employees are following these safe work practices? | | | YES NO NA | |

Mechanical Integrity

| App | Application | | | | | |
|-----|---|---|--------------|--|--|--|
| | | | | | | |
| 1. | HHI are p | s the equipment included in the mechanical integrity ram ^{1, 29, 37, 46, 61, 62} include all equipment that contains RC and other equipment which contains non-HHRC, but part of the covered process because they can potentially et a HHRC release? | □YES □NO □NA | | | |
| | | | | | | |
| | | | | | | |
| Ap | plicati | on – Controls | | | | |
| | | | | | | |
| 1. | | the following control systems ^{1, 3, 6, 7, 16, 26, 27, 28, 46, 62, 63, 94} | ☐YES ☐NO ☐NA | | | |
| | | could reduce the probability of a runaway reaction | | | | |
| | a) | Automated vent systems that open on high pressure: | YES NO NA | | | |
| | <u>a)</u> b) | Automated quench systems that actuate on high | YES NO NA | | | |
| | 0) | temperature; | | | | |
| | c) | Automated dump systems that actuate on high | ☐YES ☐NO ☐NA | | | |
| | | temperature or pressure? | | | | |
| | d) | Automated systems that inject a reaction inhibitor or | ☐YES ☐NO ☐NA | | | |
| | | poison on high temperature or pressure? | | | | |
| | <u>e)</u> | Explosion suppression systems? | YES NO NA | | | |
| | f) | Inerting systems? Equipment insulation used to prevent heat induced | YES NO NA | | | |
| | g) | runaway reactions? | | | | |
| | h) | Purge and flush systems, and chemical seals used to ensure that instruments used to identify potential runaway reaction conditions receive an accurate input? | □YES □NO □NA | | | |
| | i) | All of the equipment in each instrument loop in each | ☐YES ☐NO ☐NA | | | |
| | | layer of protection that is used as a safeguard against | | | | |
| | • | runaway reactions? | | | | |
| | j) | The functionality of each instrument loop in each layer of protection that is used as a safeguard against | ☐YES ☐NO ☐NA | | | |
| | | runaway reactions? | | | | |
| | k) | Building, or room, temperature control systems for | YES NO NA | | | |
| |) | thermally sensitive materials? | | | | |
| | 1) | Building, or room, humidity control systems for | ☐YES ☐NO ☐NA | | | |
| | | moisture sensitive materials? | | | | |

| Application – Controls | | | | |
|------------------------|---|----------------------------|--|--|
| | | | | |
| | tes the mechanical integrity program include control stems ^{1, 3, 6, 7, 16, 26, 27, 28, 46, 62, 63, 94} that can be used to | YES NO NA | | |
| | tigate the effects of a runaway reaction, such as: | | | |
| <u>a)</u> | Bunkers, blast walls and barricades? | YESNONA | | |
| b) | Traffic barriers that are used to protect process equipment from vehicles? | YES NO NA | | |
| c) | Secondary containment? | ☐YES ☐NO ☐NA | | |
| d) | Excess flow valves? | □YES □NO □NA | | |
| e) | Remotely actuated emergency block valves? | ☐YES ☐NO ☐NA | | |
| f) | Fire-resistant/explosion/resistant construction? | □YES □NO □NA | | |
| g) | Alarms to detect the heat and/or vapors generated as a result of the loss of containment? | □YES □NO □NA | | |
| h) | Fire protection systems that would be expected to be called upon as the result of a runaway reaction, such as: | ☐YES ☐NO ☐NA | | |
| | i) Firewater pumps, jockey pumps, and controls? | YES NO NA | | |
| | ii) Firewater headers? | YES NO NA | | |
| | iii) Firewater monitors? | YES NO NA | | |
| | iv) Fire hoses and fog nozzles | YES NO NA | | |
| | v) Fire sprinkler systems? | YES NO NA | | |
| i) | Emission control systems? | YES NO NA | | |
| -) | i) Flares and thermal oxidizers? | YES NO NA | | |
| | ii) Cyclones? | YES NO NA | | |
| | iii) Catch tanks? | YES NO NA | | |
| | iv) Knockout drums? | YES NO NA | | |
| | v) Water curtains/deluge systems? | YES NO NA | | |
| | vi) Scrubber systems? | YES NO NA | | |
| | vii) Blowdown stacks (It is recommended that all existing blowdown stacks be taken out of service. They have unacceptable safety hazards.) | □YES □NO □NA | | |
| j) | Buildings, such as control rooms ^{14, 15, 26} and other occupied process buildings, which provide shelter to employs from the affects of runaway reactions such as explosions and the release of toxic materials? | □YES □NO □NA | | |
| k) | HVAC systems ^{14, 15, 26} that control the atmosphere in control rooms and other buildings where employees take shelter following a runaway reaction that could result in the release of toxic vapors, including such items as: i) The air handling unit? | ☐YES ☐NO ☐NA ☐YES ☐NO ☐NA | | |

| cation – Co | ontrols | |
|-------------------------------------|--|--------------|
| | , | |
| ii) | The ductwork? | YES NO NA |
| iii) | Air purification systems such as adsorbents, absorbents and scrubbers? | ☐YES ☐NO ☐NA |
| iv) | Monitors located in the ductwork and control room or building that are used to detect the presence of hazardous gases and vapors? | □YES □NO □NA |
| v) | Interlock systems that are used to prevent or minimize the entry of hazardous materials into the control room or building? | YES NO NA |
| vi) | Clean air intake stacks? | YES NO NA |
| to red | gency power supplies ¹⁸ for the equipment used uce the probability of a runaway reaction or to ate the effects of a runaway reaction, such as:: | YES NO NA |
| i) | Telephones? | YES NO NA |
| ii) | Alarm systems? | YES NO NA |
| iii) | Instrumentation? | YES NO NA |
| iv) | The HVAC air handling system? | YES NO NA |
| v) | Pumps for scrubber systems? | YES NO NA |
| vi) | Instrument air compressors? | YES NO NA |
| vii) | Agitators for reactors and other vessels that require agitation to prevent a potential runaway reaction? | YES NO NA |
| viii) | Ventilation systems? | YES NO NA |
| ix) | Emergency cooling systems? | YES NO NA |
| x) | Emission control systems? | YES NO NA |
| Were inspect | Test Procedures ion and tests performed based on procedures that | YES NO NA |
| follow manu 6, 7, 16, 26, 27, 28 | facturer's recommendations and RAGAGEP ^{1, 3,} ^{46, 62, 63, 94} for all covered equipment, such as: | |
| equip the co | quipment that contains HHRC and other ment which contains non-HHRC, but are part of overed process because they can potentially a HHRC release? | ∐YES ∐NO ∐NA |
| | ressure relief systems? | YES NO NA |
| runav | ol systems that could reduce the probability of a vay reaction occurring, included in the anical integrity program: | YES NO NA |

| Inspection and | Test Procedures | | |
|----------------|---|--------------|--|
| | | | |
| i) | Automated vent systems that open on high pressure: | □YES □NO □NA | |
| ii) | Automated quench systems that actuate on high temperature; | □YES □NO □NA | |
| iii) | Automated dump systems that actuate on high temperature or pressure? | □YES □NO □NA | |
| iv) | Automated systems that inject a reaction inhibitor or poison on high temperature or pressure? | □YES □NO □NA | |
| v) | Explosion suppression systems? | ☐YES ☐NO ☐NA | |
| vi) | Inerting systems? | YES NO NA | |
| vii) | Equipment insulation used to prevent heat induced runaway reactions? | YES NO NA | |
| viii | used to ensure that instruments used to identify potential runaway reaction conditions receive an accurate input? | □YES □NO □NA | |
| ix) | All of the equipment in each instrument loop in each layer of protection that is used as a safeguard against runaway reactions? | ☐YES ☐NO ☐NA | |
| x) | The functionality of each instrument loop in each layer of protection that is used as a safeguard against runaway reactions? | ☐YES ☐NO ☐NA | |
| xi) | Building, or room, temperature control systems for thermally sensitive materials? | □YES □NO □NA | |
| xii) | Building, or room, humidity control systems for moisture sensitive materials? | □YES □NO □NA | |
| xiii | Control systems that can be used to mitigate the effects of a runaway reaction, such as: | □YES □NO □NA | |
| xiv | Bunkers, blast walls and barricades? | YES NO NA | |
| xv) | Traffic barriers that are used to protect process equipment from vehicles? | □YES □NO □NA | |
| xvi | | ☐YES ☐NO ☐NA | |
| xvi | | YES NO NA | |
| xvi | i) Remotely actuated emergency block valves? | YES NO NA | |
| xix | | YES NO NA | |
| xx) | Alarms to detect the heat and/or vapors generated as a result of the loss of containment? | YES NO NA | |
| | e protection systems that would be expected to be ed upon as the result of a runaway reaction, such | YES NO NA | |

| Inspection | and T | est Procedures | |
|------------|-----------|---|---------------------|
| - | | | |
| | i) | Firewater pumps, jockey pumps, and controls? | YES NO NA |
| | ii) | Firewater headers? | YES NO NA |
| | iii) | Firewater monitors? | YES NO NA |
| | iv) | Fire hoses and fog nozzles | YES NO NA |
| | v) | Fire sprinkler systems? | YES NO NA |
| m) | , | ion control systems? | YES NO NA |
| | i) | Flares and thermal oxidizers? | YES NO NA |
| | ii) | Vent headers and sub-headers, including | YES NO NA |
| | / | accumulation of solids within these systems? | |
| | iii) | Cyclones? | TYES NO NA |
| | iv) | Catch tanks? | YES NO NA |
| | v) | Knockout drums? | YES NO NA |
| | vi) | Water curtains/deluge systems? | YES NO NA |
| | vii) | Scrubber systems? | YES NO NA |
| | viii) | Blowdown stacks (It is recommended that all | YES NO NA |
| | | existing blowdown stacks be taken out of | |
| | | service. They have unacceptable safety | |
| | | hazards.) | |
| n) | | ngs, such as control rooms ^{14, 15, 26} and other | │ □YES □NO □NA │ |
| | | ied process buildings, which provide shelter to | |
| | emplo | ys from the affects of runaway reactions such as | |
| | explos | sions and the release of toxic materials? C systems 14, 15, 26 that control the atmosphere in | |
| 0) | HVAC | Systems 14, 15, 26 that control the atmosphere in | LYES LNO LNA |
| | | l rooms and other buildings where employees | |
| | | nelter following a runaway reaction that could | |
| | | in the release of toxic vapors, including such | |
| | items | as: The air handling unit? | YES NO NA |
| | i) ii) | The ductwork? | YES NO NA YES NO NA |
| | iii) | Air purification systems such as adsorbents, | YES NO NA |
| | 111) | absorbents and scrubbers? | |
| | iv) | Monitors located in the ductwork and control | YES NO NA |
| | 11) | room or building that are used to detect the | |
| | | presence of hazardous gases and vapors? | |
| | v) | Interlock systems that are used to prevent or | YES NO NA |
| | • , | minimize the entry of hazardous materials into | |
| | | the control room or building? | |
| | vi) | Clean air intake stacks? | □YES □NO □NA |
| | vi) | Agitators for reactors and other vessels that | YES NO NA |
| | | require agitation to prevent a potential | |
| | | runaway reaction? | |

| Inspection | and Test Procedures | |
|------------|---|--------------|
| | | |
| | vii) Ventilation systems? | YES NO NA |
| | viii) Emergency cooling systems? | YES NO NA |
| 2. Did th | the inspections and tests methods follow RAGAGEP, | |
| such a | <u> </u> | |
| a) | Control systems (safety systems) in compliance with ANSI/ISA-84.00.01-2004 Part 1 ⁹² (IEC 61511-1-Mod) and API 551 ¹⁰⁸ and 554 ¹⁰⁹ | □YES □NO □NA |
| b) | Pressure vessels in compliance with the ASME BPVC ⁸⁴ and API 510 ⁹⁵ 572 ⁸⁶ , 579 ⁹⁷ and 581 ⁴⁷ ? | YES NO NA |
| c) | Above ground atmospheric pressure storage tanks in compliance with API 653 ⁹⁸ , 579 ⁹⁷ and 581 ⁴⁷ ? | □YES □NO □NA |
| d) | Low pressure storage tanks in compliance with API 575 ⁹⁹ , 579 ⁹⁷ and 581 ⁴⁷ ? | □YES □NO □NA |
| e) | Piping, including vent headers, in compliance with API 570 ¹⁰⁰ , 579 ⁹⁷ and 581 ⁴⁷ ? | □YES □NO □NA |
| f) | Pressure relief devices in compliance with API 576 ¹⁰¹ and 581 ⁴⁷ ? | □YES □NO □NA |
| g) | Materials of construction of alloy piping systems is verified in compliance with API 578 ¹⁰² | □YES □NO □NA |
| h) | Centrifugal compressors in compliance with API 617 ¹⁰³ ? | □YES □NO □NA |
| i) | Reciprocating compressors in compliance with API 618 ¹⁰⁴ ? | □YES □NO □NA |
| j) | Steam turbines in compliance with API 611 ¹⁰⁵ and 612 ¹⁰⁶ ? | □YES □NO □NA |
| k) | Gas turbines in compliance with API 616 ¹⁰⁷ ? | YES NO NA |
| 1) | Process control in compliance with API 551 ¹⁰⁸ and 554 ¹⁰⁹ ? | □YES □NO □NA |
| m) | Electrical equipment, such as that shown below, in compliance with NFPA 70B ¹¹⁰ : | YES NO NA |
| | i) Substations and switchgear assemblies? | ☐YES ☐NO ☐NA |
| | ii) Power and Distribution Transformers? | YES NO NA |
| | iii) Power cables? | YES NO NA |
| | iv) Motor control equipment? | YES NO NA |
| | v) Molded case circuit breaker power panels | YES NO NA |
| | vi) Ground fault protection? | YES NO NA |
| | vii) Fuses? | YES NO NA |
| | viii) Rotating equipment (motors, generators, alternators, etc.) | YES NO NA |
| | ix) Lighting? | ☐YES ☐NO ☐NA |

| Inchastic | n and Tast Procedures | |
|-----------|--|--------------|
| mspecho | n and Test Procedures | |
| | x) Wiring devices (i.e. connectors, plugs and receptacles, switches, etc.)? | YES NO NA |
| | xi) Portable electric tools and equipment? | YES NO NA |
| | xii) Hazardous location electrical equipment? | YES NO NA |
| | xiii) De-energizing and grounding equipment? | YES NO NA |
| | xiv) Cable tray and busway? | YES NO NA |
| n) | Uninterruptible power supply systems in compliance with NFPA 70B ¹¹⁰ and NFPA 111 ¹¹¹ ? | □YES □NO □NA |
| 0) | Does the PSI show that emergency power generators, switchgear, and ancillary equipment are inspected, tested and maintained in compliance with NFPA 70B ¹¹⁰ and 110 ¹¹² , and IEEE Standard 446-1995 ¹⁸ ? | □YES □NO □NA |

| Freq | Frequency of inspections - Relief and vent systems and devices | | | | | | |
|------|--|--------------|--|--|--|--|--|
| | | | | | | | |
| 1. | Does the frequency of inspection and testing ^{3, 6, 12, 26, 28, 46, 47, 84} of relief and vent devices take into consideration the difference in pressure between the pressure when the relief device pops when taken out of service before any cleaning or disassembly has occurred, and the set pressure (use of a precleaning pop test)? | ☐YES ☐NO ☐NA | | | | | |
| 2. | Does the frequency of inspection of relief and vent devices take into consideration the accumulation of materials in the piping leading to the device, on the surface of rupture disks and in the nozzle and on the disk of pressure relief devices? | YES NO NA | | | | | |
| 3. | Does the frequency of inspection of relief and vent systems take into consideration the tendency for reaction products to plug the nozzles leading to these devices? | YES NO NA | | | | | |
| 4. | Does the inspection include systems that are used to minimize the plugging of nozzles with reaction products, such as nitrogen purges, liquid purges and chemical seals? | ☐YES ☐NO ☐NA | | | | | |
| | Note: When this type of equipment is installed, it is considered part of the relief and vent system and is required to be inspected. | | | | | | |
| 5. | Are vent headers and effluent handling systems that service equipment containing reactive materials included in the mechanical integrity program? | YES NO NA | | | | | |

Management of Change

| Written procedures for changes to a facility that affect a covered process | | | | |
|---|--------------|--|--|--|
| | | | | |
| 6. Are there written procedures for managing organizational changes ^{1, 29, 33, 48, 61, 62} such as changes in staffing and work schedules in an HHRC covered process? | □YES □NO □NA | | | |
| a) Do the procedures require that the proposed change is reviewed and approved by appropriate personnel before the change is actually made? | □YES □NO □NA | | | |
| b) Do the procedures require an analysis to be performed to determine the impact of the change on safety and health? | □YES □NO □NA | | | |
| c) Does the procedure define which jobs are covered by the procedure, such as: | ☐YES ☐NO ☐NA | | | |
| i) Employees, including supervisors and managers which have an involvement in the operation of the process, including: | □YES □NO □NA | | | |
| (a) Department managers? | ☐YES ☐NO ☐NA | | | |
| (b) Process unit managers | YES NO NA | | | |
| (c) Process improvement engineers? | YES NO NA | | | |
| (d) Operations engineers? | YES NO NA | | | |
| (e) Shift supervisors | YES NO NA | | | |
| (f) Lead operators? | YES NO NA | | | |
| (g) Operators? | YES NO NA | | | |
| ii) Employees, including supervisors and managers which support the safe operation of the process, such as: | YES NO NA | | | |
| (a) Safety and health groups? | ☐YES ☐NO ☐NA | | | |
| (b) Groups responsible for providing utilities, such as steam, electric, water, instrument air? | YES NO NA | | | |
| (c) Maintenance groups? | □YES □NO □NA | | | |
| (d) Purchasing groups? | YES NO NA | | | |
| (e) Engineering groups? | YES NO NA | | | |
| (f) Fire Brigade? | YES NO NA | | | |
| (g) Plant security? | YES NO NA | | | |
| d) Does the procedure apply at all hours of operation to permanent or temporary staffing changes, such as: | □YES □NO □NA | | | |
| i) Hiring of employees new to the plant? | YES NO NA | | | |
| ii) Transfers of personnel from other departments, workgroups, or facilities? | YES NO NA | | | |

| en proc | edu | res for changes to a facility that affect | a covered process |
|---------|-------|--|-------------------|
| ii | ii) | Promotions from within, or outside the department? | YES NO NA |
| iv | v) | Retirements of experienced personnel? | YES NO NA |
| V | | Layoff of experienced personnel? | YES NO NA |
| | vi) | Changes in job responsibilities even though there is no change in job title? | YES NO NA |
| V | rii) | Changes in the needs of the process due to: | YES NO NA |
| | | (a) Changes in production rates? | YES NO NA |
| | | (b) Changes in equipment? | YES NO NA |
| | | (c) Changes in technology? | YES NO NA |
| | | (d) Maintenance outages? | YES NO NA |
| | | (e) Working hours? | YES NO NA |
| | | (f) Unforeseen events? | YES NO NA |
| v | riii) | Changes in the work schedule? | YES NO NA |
| e) [| Ooes | the program apply to temporary or minor ges such as: | YES NO NA |
| i) | | Summer interns? | YES NO NA |
| | | Temporary workers? | YES NO NA |
| | ii) | Contractors? | YES NO NA |
| | v) | Consultants? | YES NO NA |
| v | | National Guard or Military Reserve call up for active duty, or training? | YES NO NA |
| c | onsi | the procedure describe when changes are dered to be replacements in kind for which the dure does not apply, such as: | YES NO NA |
| i) |) | Replacement by a worker that is qualified by training and experience to perform the work (i.e. trading shifts)? AND | YES NO NA |
| ii | i) | There is no change in this recommended practice compliance responsibilities for either individual (i.e. trading shifts)? | □YES □NO □NA |
| g) [| Ooes | the procedure require that an analysis be | YES NO NA |
| | | rmed to ensure that the change will not have an se affect on: | |
| i) | | The safety and health of the employees? | YES NO NA |
| ii | i) | The ability to comply with the requirements of this recommended practice? | YES NO NA |
| ii | ii) | Operability of the process? | YES NO NA |
| a | nd u | the procedure require that accurate, complete p-to-date personnel records be maintained and for the review, including: | YES NO NA |

| Written pro | ocedui | res for changes to a facility that affect a | a covered process |
|-------------|-----------------------|--|-------------------|
| | | | |
| | i) | Education? | YES NO NA |
| | ii) | Training? | YES NO NA |
| | iii) | Certifications? | YES NO NA |
| | iv) | Current job responsibilities (i.e. job description)? | ☐YES ☐NO ☐NA |
| i) | performerspondare ide | the procedure require that an analysis be med to ensure that all recommended practice is ibilities associated with the change in staffing entified and appropriate resources are assigned form that work, such as: | □YES □NO □NA |
| | i) | Development and use of employee participation programs? | YES NO NA |
| | ii) | Preparation, use of, and evaluation of process safety information, including information about the technology, chemicals, and equipment used in the process? | YES NO NA |
| | iii) | Design of the equipment in the process? | YES NO NA |
| | iv) | Evaluation and selection of RAGAGEP to be used? | □YES □NO □NA |
| | v) | Planning, organizing, leading, and participating in process hazards analyses? | □YES □NO □NA |
| | vi) | Operation of the process? | ☐YES ☐NO ☐NA |
| | vii) | Preparation and updating of operating procedures? | YES NO NA |
| | viii) | Performing training? | YES NO NA |
| | ix) | Performing maintenance on the process including preventative maintenance and testing and inspections? | □YES □NO □NA |
| | x) | Preparation, use, evaluation, and participation in mechanical integrity programs, including preventative maintenance, quality control, and testing and inspection? | YES NO NA |
| | xi) | Development, evaluation, and use of safe work practices such as LOTO, confined space, equipment opening and safe work permit programs? | □YES □NO □NA |
| | xii) | Evaluation and use of contractor safety programs? | □YES □NO □NA |
| | xiii) | Planning, organizing, leading, and participation in pre-startup safety reviews? | YES NO NA |

| Written pro | ocedui | es for changes to a facility that affect a | a covered process |
|-------------|-------------------------|---|-------------------|
| | xiv) | Initiation, evaluation, review, and authorization of changes covered by this recommended practice? | YES NO NA |
| | xv) | Planning, organizing, leading, and participating in emergency response procedures, including fire brigade? | ☐YES ☐NO ☐NA |
| | xvi) | Planning, organizing, leading, and participating in safety and recommended practice compliance audits? | ☐YES ☐NO ☐NA |
| j) | that in have the job in | he procedure require a training review to ensure dividuals moving into a new or changed job he training and skills needed to perform their a safe and responsible manner, before they e new responsibilities? | YES NO NA |
| k) | trainin topics | he procedure require that comprehensive g be performed, completed, and understood, for such as that shown below, prior to performance j job duties? | ☐YES ☐NO ☐NA |
| | i) | Corporate safety policies and procedures? | YES NO NA |
| | ii) | Plant safety policies and procedures? | ☐YES ☐NO ☐NA |
| | iii) | Department, or unit safety policies and procedures? | □YES □NO □NA |
| | iv) | Employee participation program? | YES NO NA |
| | v) | Information about the chemicals in the process? | YES NO NA |
| | vi) | Information about the technology of the process? | YES NO NA |
| | vii) | Information about the equipment in the process, including the design and design basis? | ∐YES ∐NO ∐NA |
| | viii) | Information about the hazards of the process and the equipment in it? | YES NO NA |
| | ix) | Personal protective equipment used in the process? | □YES □NO □NA |
| | x) | The PHA procedures and review of previous process hazards analysis? | □YES □NO □NA |
| | xi) | Operating procedures? | ☐YES ☐NO ☐NA |
| | xii) | Training procedures? | ☐YES ☐NO ☐NA |
| | xiii) | Contracting procedures? | YES NO NA |
| | xiv) | Purchasing procedures? | YES NO NA |
| | xv) | Pre-startup safety review procedures? | YES NO NA |

| Written procedures for changes to a facility that affect a covered process | | | | | |
|--|--------|--|-------------------|--|--|
| written pro | Cedui | es for changes to a facility that affect of | a covered process | | |
| | xvi) | Maintenance procedures, including preventative maintenance and testing and inspection? | □YES □NO □NA | | |
| | xvii) | Safe work practices such as LOTO, confined space entry, equipment and line opening and safe to work permit procedures? | YES NO NA | | |
| | xviii) | Management of change procedures? | YES NO NA | | |
| | xix) | Incident investigation procedures and review of previous incidents? | ☐YES ☐NO ☐NA | | |
| | xx) | Emergency operation procedures? | YES NO NA | | |
| | xxi) | Emergency response plan? | YES NO NA | | |
| | xxii) | Trade secrets policy? | ☐YES ☐NO ☐NA | | |
| | xxiii) | Procedures for auditing compliance with this recommended practice and review of previous audits? | □YES □NO □NA | | |
| 1) | | he procedure identify who has the authority to ye the change? | YES NO NA | | |
| m) | | he procedure require reauthorization if any es are made after the initial approval? | □YES □NO □NA | | |
| n) | | he procedure require documentation of the e including all analyses, reviews, training, and vals? | YES NO NA | | |

Emergency Planning and Response

| Emer | gency | / Planning and Response | | | | | | |
|------|--|--|------------------|--|--|--|--|--|
| | | | | | | | | |
| 7. | Does the emergency action plan ⁶⁰ include preplanning for HHRC events, such as: | | | | | | | |
| | a) | Identification of reactive chemicals potentially present in the process, and adjacent processes that might be affected? | □YES □NO □ NA | | | | | |
| | b) | Identification of the hazards presented by the reactive chemicals potentially present in the process, and adjacent processes that might be affected? | □YES □NO □ NA | | | | | |
| | c) | Identification of scenarios that could result in loss of containment due to reactive chemical incidents? | ☐YES ☐NO ☐ NA | | | | | |
| | d) | Preparation of a pre-plan for responders for all scenarios that could result in a loss of containment due to reactive chemicals? | □YES □NO □ NA | | | | | |
| | e) | Training of all responders in the pre-plan developed for all scenarios that could result in a loss of containment due to reactive chemicals? | □YES □NO □ NA | | | | | |
| 8. | | the emergency action plan include training all emergency aders in the hazards associated with the HHRC in the self-self-self-self-self-self-self-self- | ☐YES ☐NO ☐ NA | | | | | |

| C ₄ H ₆ 1,3- Butadiene | Flammable; peroxidizes; polymerizes; decomposes | | | | | | |
|--|---|--|---|---|--------------------------------|---------------------------------------|---------------------|
| Cl ₂ Chlorine | Fire, toxic gas generation; violent polymerization | Oxidizer, toxic vapor, Cryogenic liquid spill | | | | | |
| HF Anhydrous hydrogen fluoride | Heat generation, violent polymerization | Heat generation, liberating toxic vapors; | Strong acid; corrosive ³ ; toxic vapor and liquid | | | | |
| NH ₃ Anhydrous ammonia | Heat generation, violent polymerization | Explosive NCl ₃ formed with excess chlorine or heat | Heat generation, liberation of toxic vapors ⁴ | Combustible; toxic vapor; cryogenic liquid spill | | | |
| Fe Iron, carbon steel | None Predicted ⁶ | Iron/chlorine fire if above 250°C ² | Hydrogen blistering between laminations; formation of hydrogen | None predicted | Material of construction | | |
| H ₂ O 150 psig steam | Inhibitor consumed, leading to polymerization | None predicted | Heat generation, liberating toxic vapors | Heat generation, liberating toxic vapors | None predicted | Elevated temperature, pressure | |
| Air - Oxygen | Formation of explosive compound; polymerization catalyst ¹ | Accelerates or may initiate combustion of materials | None predicted | None predicted | None predicted | None predicted | Supports combustion |
| Combined with | C ₄ H ₆ 1,3- Butadiene | Cl ₂ Chlorine | HF Anhydrous hydrogen fluoride | NH ₃ Anhydrous ammonia | Fe Iron, carbon steel | H ₂ O 150 psig steam | Air - Oxygen |

Table 15 Typical Reactivity Matrix

Notes:

- 1) BD reacts with oxygen from rust, water, or ambient air to form butadiene polyperoxide, a very unstable explosive material. The polyperoxide also acts as a catalyst for the formation of rubber polymer and polybutadiene popcorn, both of which can be formed at explosive rates.
- 2) If there are contaminants present, or if the iron is finely divided, the fire can occur at 100°C or less
- 3) Dissolves glass to form toxic silicon tetrafluoride gas.
- 4) Explosive NF₃ may be formed from the reaction products.
- 5) Ammonia will react explosively with the reaction products of chlorine and 1,3-butadiene.
- 6) Forms explosive compounds on contact with copper and its alloys.

Adapted from Figure 4.2 CCPS 1995³

Table 16 Typical SIL Determination Matrix

Typical SIL Requirement Determination Matrix

| Number of IPL | SIL Level Required | | | | | | | | | | |
|------------------------------------|---------------------------------|-----|------|--|---------|------|---------|--|-----------|---------|---------|
| 3 | | | | | | | | | c) | 1 | 1 |
| 2 | c) | c) | 1 | | c) | 1 | 2 | | 1 | 2 | 3 b) |
| 1 | c) | 1 | 2 | | 1 | 2 | 3 b) | | 3 b) | 3 b) | 3 a) |
| Hazardous Event Likelihood. | Low | Med | High | | Low | Med. | High | | Low | Med. | High |
| Assumes all IPL are out of service | Minor | | | | Serious | | | | Extensive | | |
| | Hazardous Event Severity Rating | | | | | | | | | | |

The likelihood and severity of a potential incident are used to determine the Number of IPLs needed and the SIL of the SIS.

- a) One level 3 safety instrumented system does not provide sufficient risk reduction at this risk level. Additional IPL are required.
- b) One level 3 safety instrumented function may not provide sufficient risk reduction at this risk level. Consider additional IPL.
- c) SIS IPL may not be needed.

Table 17 Typical Risk Matrix

| | | Severity | | | | | | | |
|------------|---|--|--------------------------|------------------|--|--------------------------|-------------------------|--|--|
| | | 1 | 2 | 3 | | 4 | 5 | | |
| þ | 5 | Е | Е | D | | С | С | | |
| Likelihood | 4 | Е | D | С | | В | В | | |
| keli | 3 | D | С | С | | В | В | | |
| Li | 2 | С | С | В | | В | A | | |
| | 1 | С | С | В | | A | A | | |
| | | Severity - potential fo | or: | | Likeli | hood – potential frequ | iency | | |
| 1 | Injury requ | uiring medical treatmer | nt; recordable case | 1 | Expected to occur annually (1/year) | | | | |
| 2 | Severe inju | evere injury requiring hospitalization; lost work case | | | May occur a couple of times during the facility l (1/25 years) | | | | |
| 3 | Immediate | ediate impairment; permanent health effects | | | Unlikely to occur during the facility life (1/250 year | | | | |
| 4 | Fatality; so organ dam | - | ve burns, loss of limbs, | 4 | Very unlyears) | ikely to occur during th | e facility life (1/2500 | | |
| 5 | Multiple fa | atalities | 5 | Extreme (1/25,00 | ly unlikely to occur duri 0 years) | ing the facility life | | | |
| | | | Corrective A | Action Leve | ls | | | | |
| A | Eminent hazard; Shutdown process until corrections are made | | | D | Acceptable with controls; verify that engineering and administrative controls are in place | | | | |
| В | | ble; Mitigate hazards vag controls to level D w | | E | No furth | er actions required | | | |
| С | | ole; Mitigate hazards woo level D within 12 mo | | | | | | | |

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